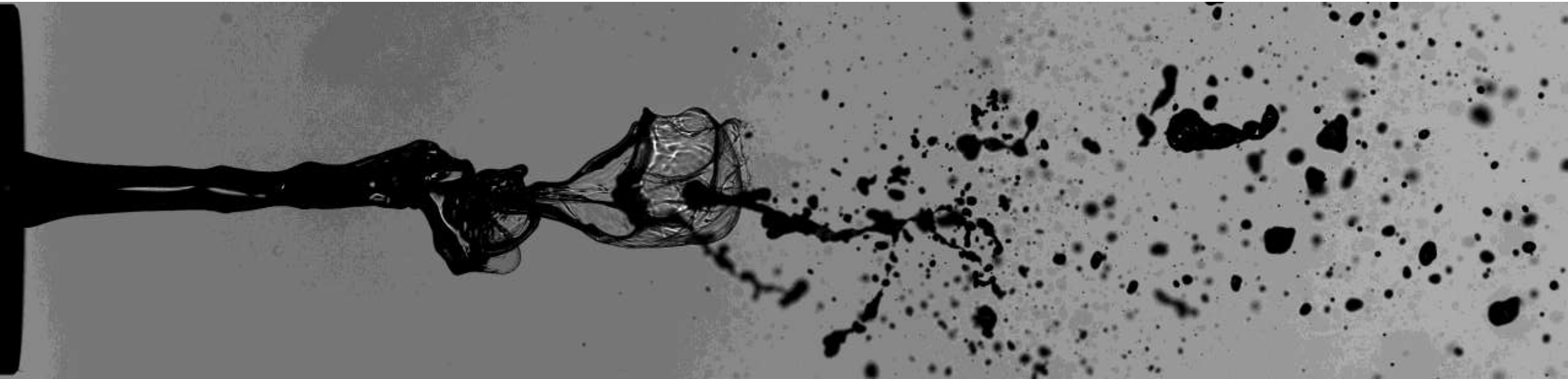


# High-speed spray formation probed by Synchrotron X-ray

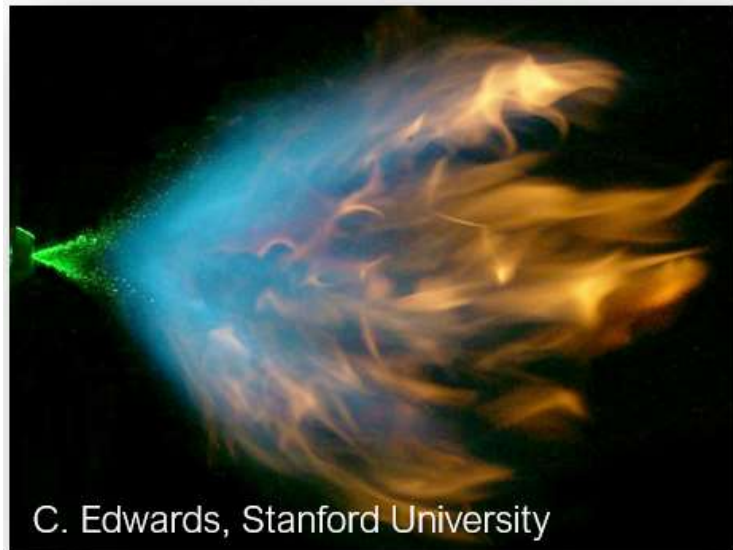
Nathanaël Machicoane<sup>1</sup>, Santanu K. Sahoo<sup>1</sup>, Oliver Tolfts<sup>1</sup>, and Alexander Rack<sup>2</sup>

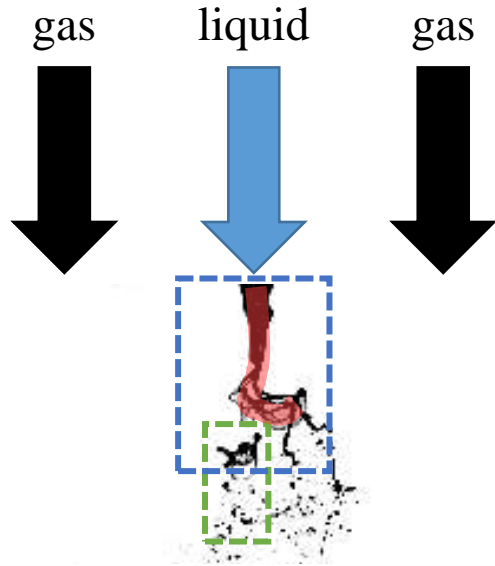
<sup>1</sup>*Univ. Grenoble Alpes, CNRS, Grenoble INP, LEGI, 38000 Grenoble, France*

<sup>2</sup>*ESRF - The European Synchrotron, 38000 Grenoble, France*



- Liquid-gas flows are critical in engineering process innovation and intensification
- Liquid sprays are critical for combustion systems, manufacturing, heat management, chemical processing, painting, e. g.:
  - Liquid fuel sprays
  - Liquid metal atomization
  - Spray cooling and coating
  - Pharmaceutical, food, consumer products
  - Fire safety
  - Ship wake and sea spray





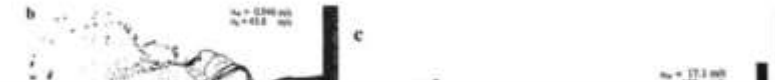
Gas-assisted atomization: breaking of a liquid jet into a spray (droplet cloud) by a gas co-flow

### Spray formation:

- Interfacial instabilities
- Primary break-up

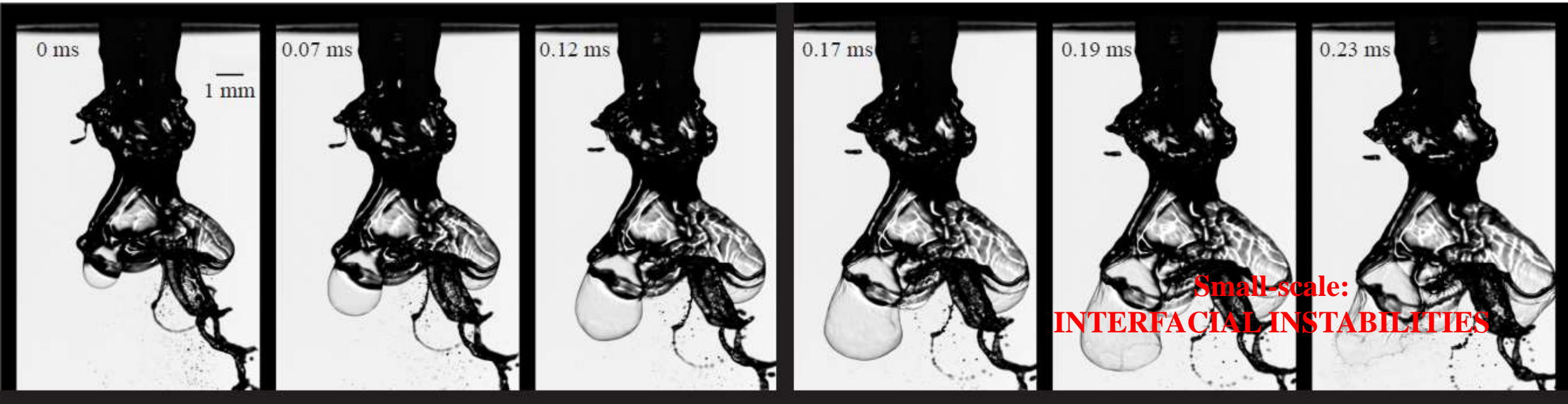
**Large-scale:  
FLAPPING**

*Farago & Chigier, 1992*



### Multiscale process

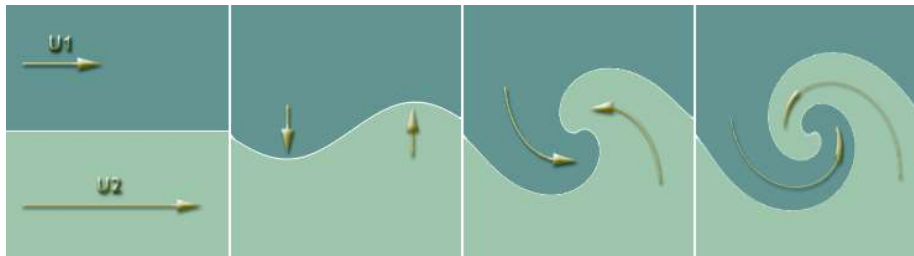
Near field



## Interface destabilized by surface tension

Rayleigh–Plateau instability

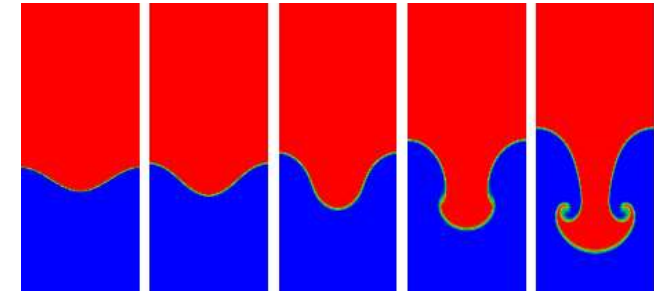
## Interface aligned with shear



Shear or Kelvin–Helmholtz instability



## Accelerated interface (transverse to shear)

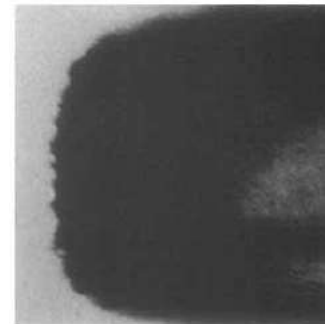
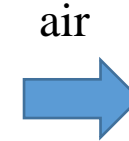


Rayleigh–Taylor instability

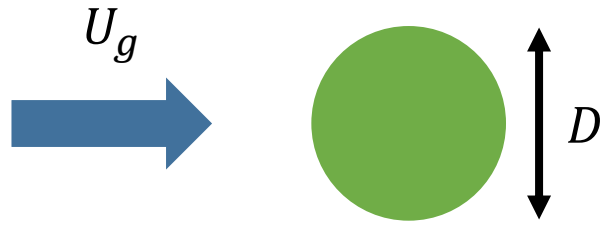
Drop under  
strong air flow



*Gravity-driven*



*Aero-driven*



Low to moderate Weber numbers



$$We = \frac{\text{gas - induced stresses}}{\text{surface tension}}$$

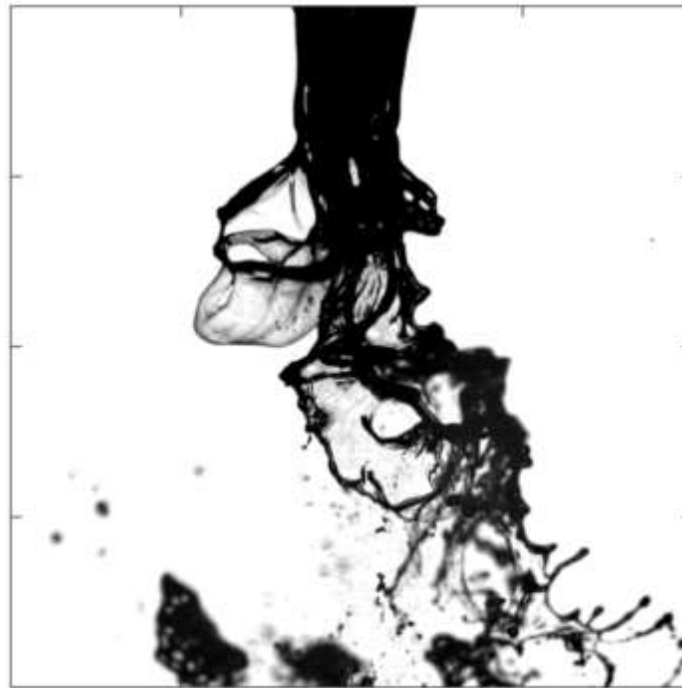
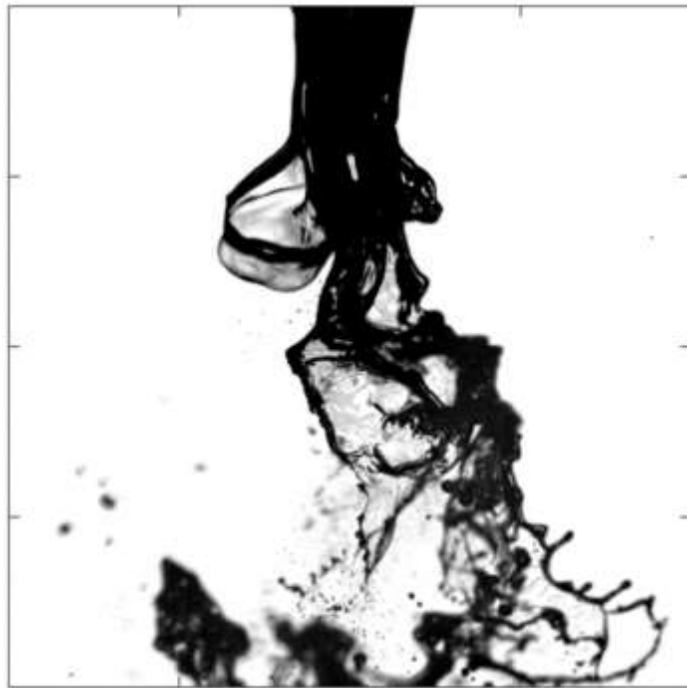
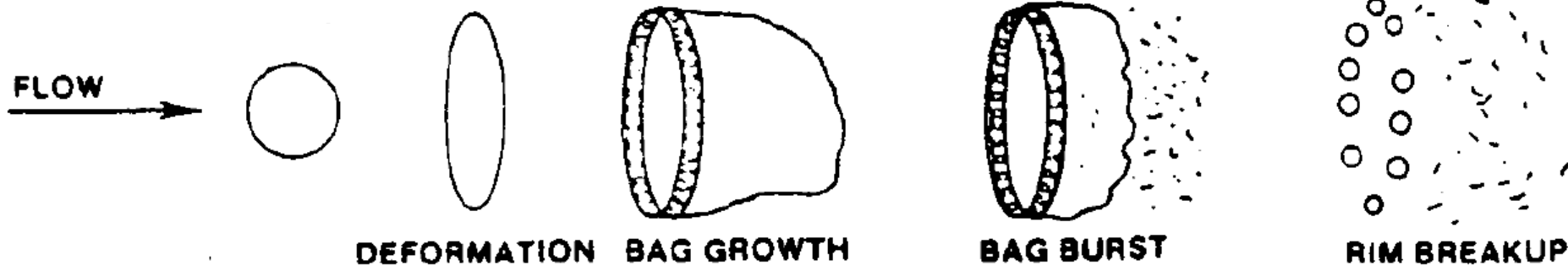
$$We = \frac{\rho_g U_g^2 D}{\sigma}$$

High Weber numbers

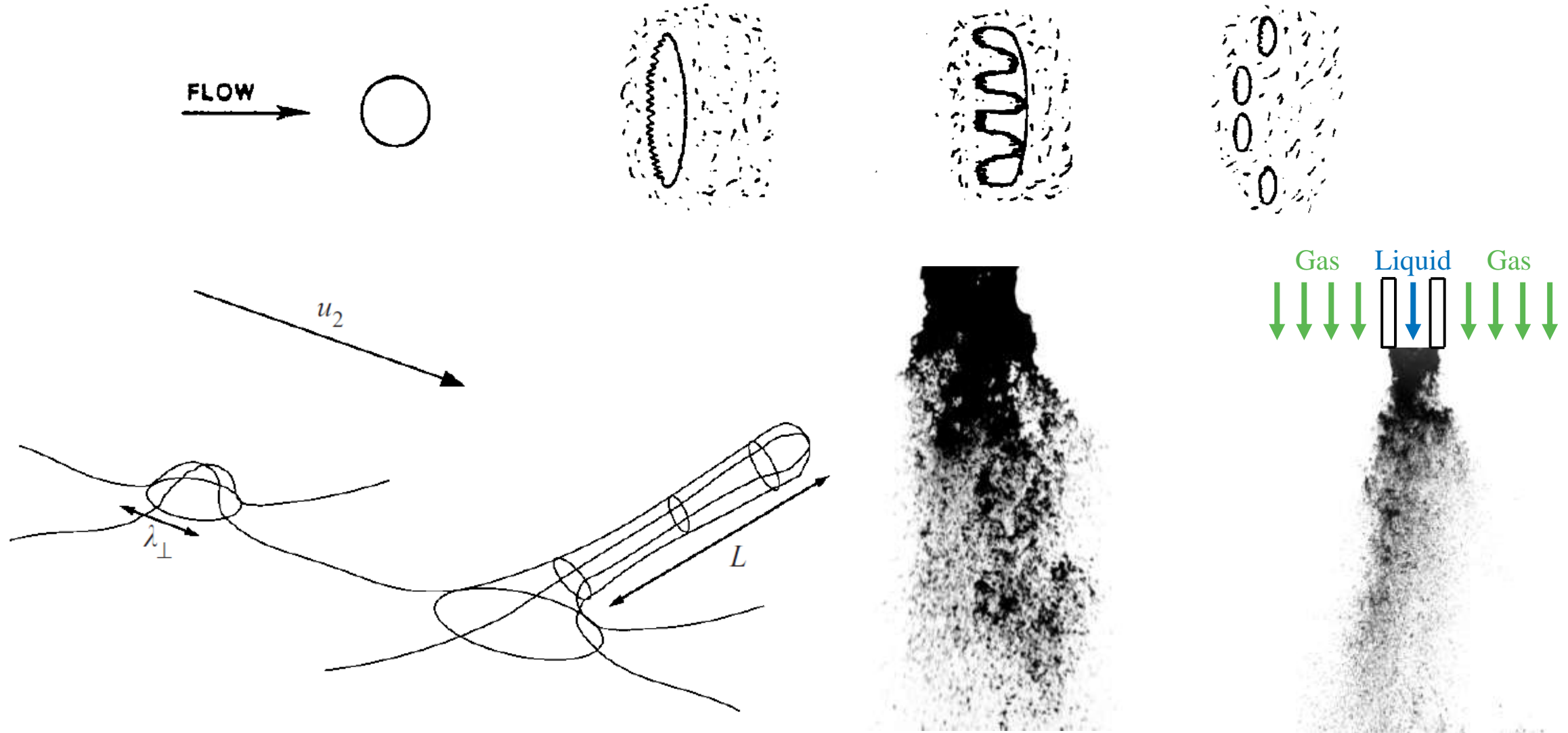


*Pilch and Erdman, IJMF 1987*

## b) BAG BREAKUP



## c) CATASTROPHIC BREAKUP



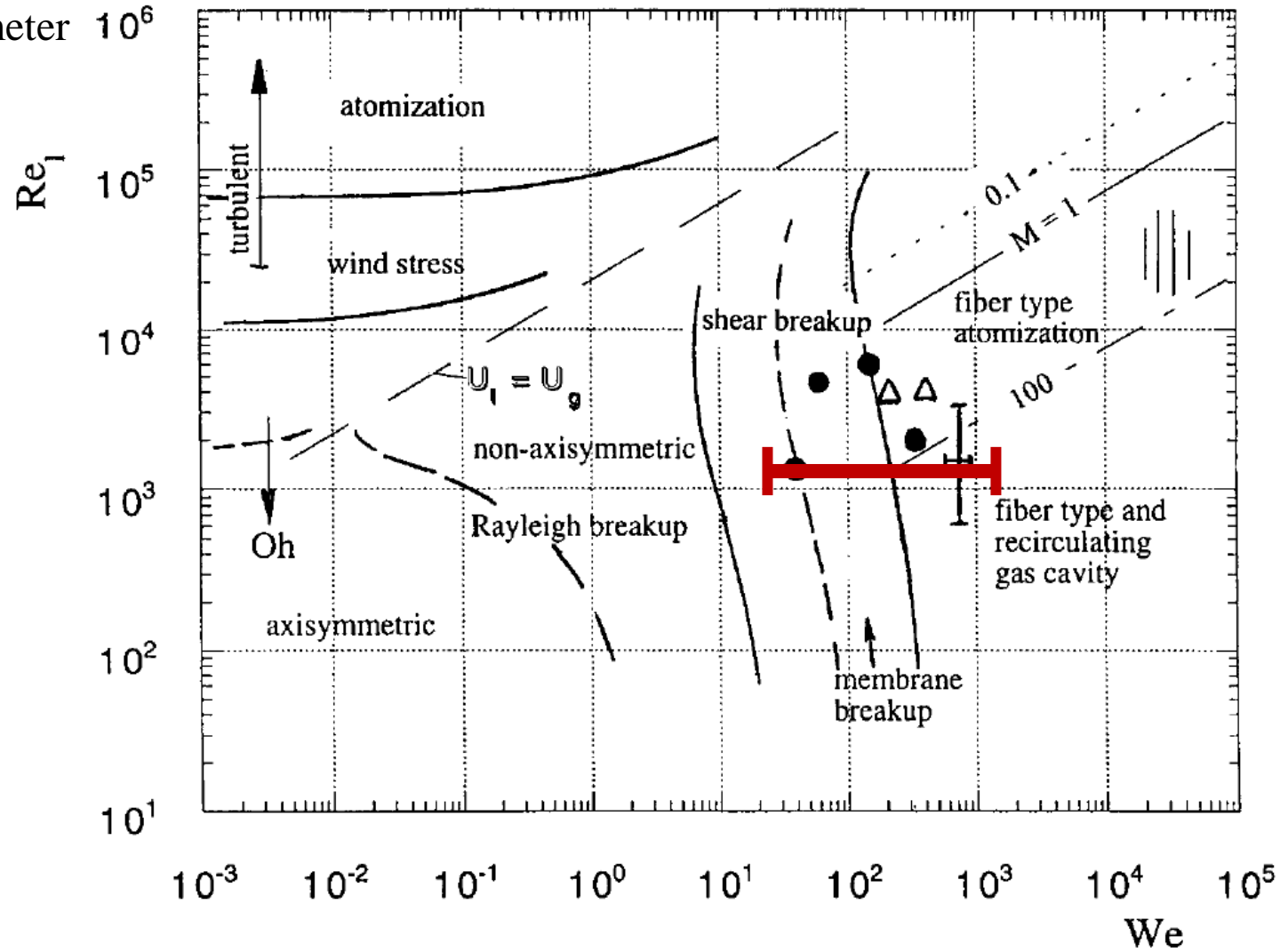
*P. Marmottant and E. Villermaux, JFM 2004*

Reynolds and Weber numbers  
based on the liquid jet diameter

*Lasheras & Hopfinger, ARFM 2000*



Rims produce large drops that contain a large portion of the liquid volume  
→ incomplete combustion/pollutants



**Need for quantitative arguments for change between regimes**



$700 < Re_l < 20\,000$   
 $10^4 < Re_g < 10^5$

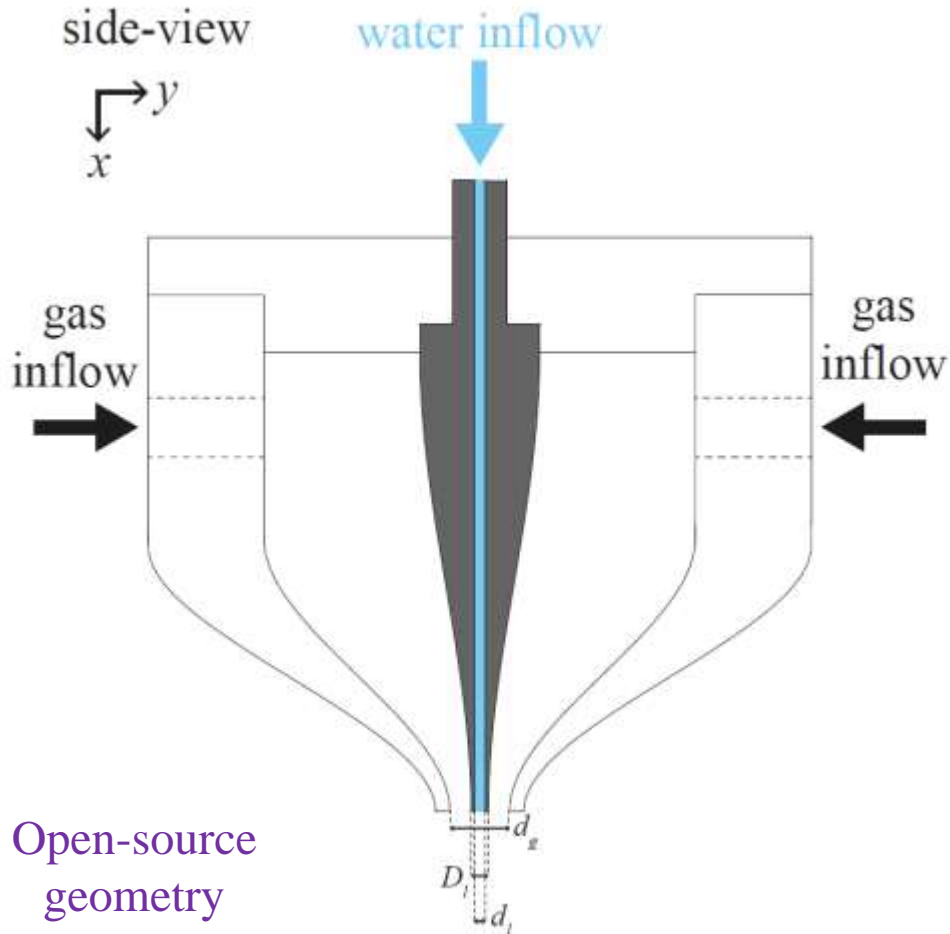
By varying the gas and liquid flow rates

Weber number

$$We_g = \frac{\rho_g u_g^2 d_l}{\sigma}$$

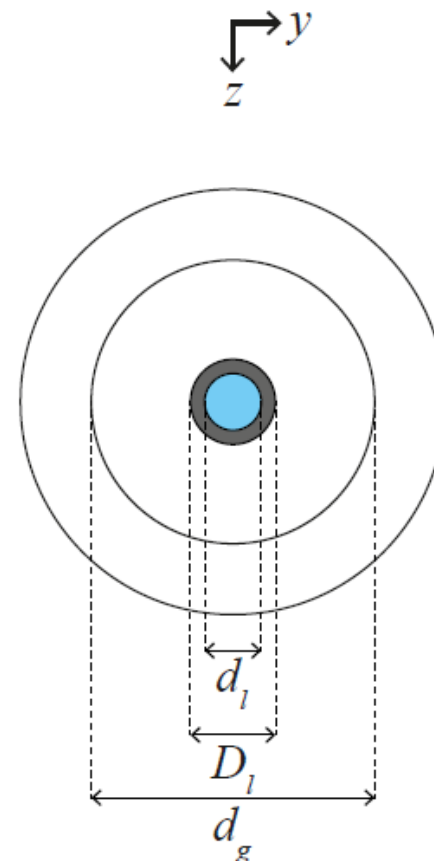
Gas-to-liquid dynamic pressure ratio

$$M = \frac{\rho_g u_g^2}{\rho_l u_l^2}$$

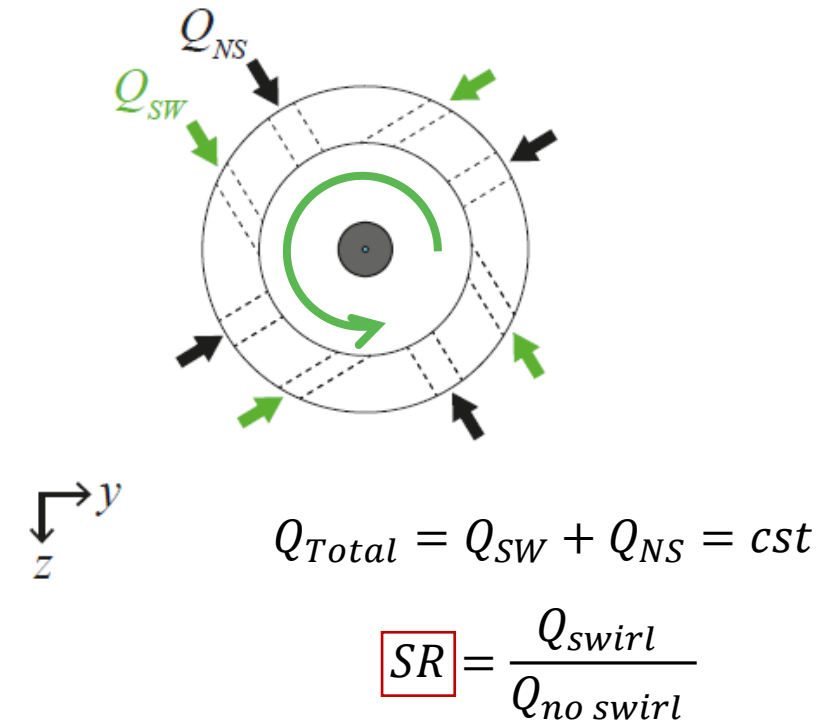


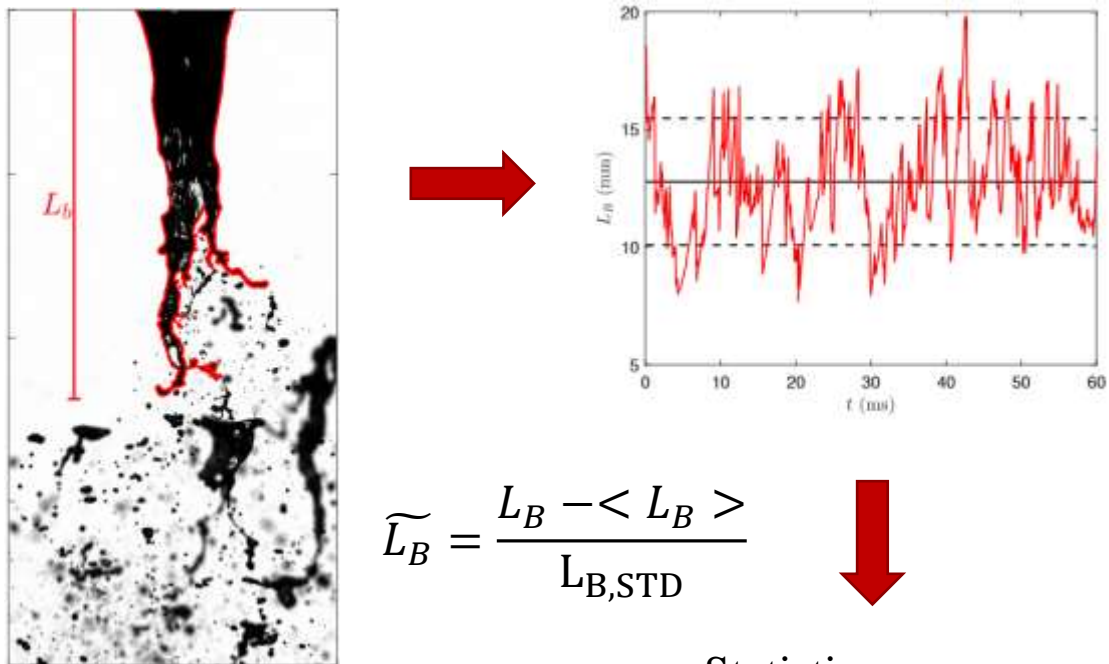
Open-source geometry

exit plane



top-view

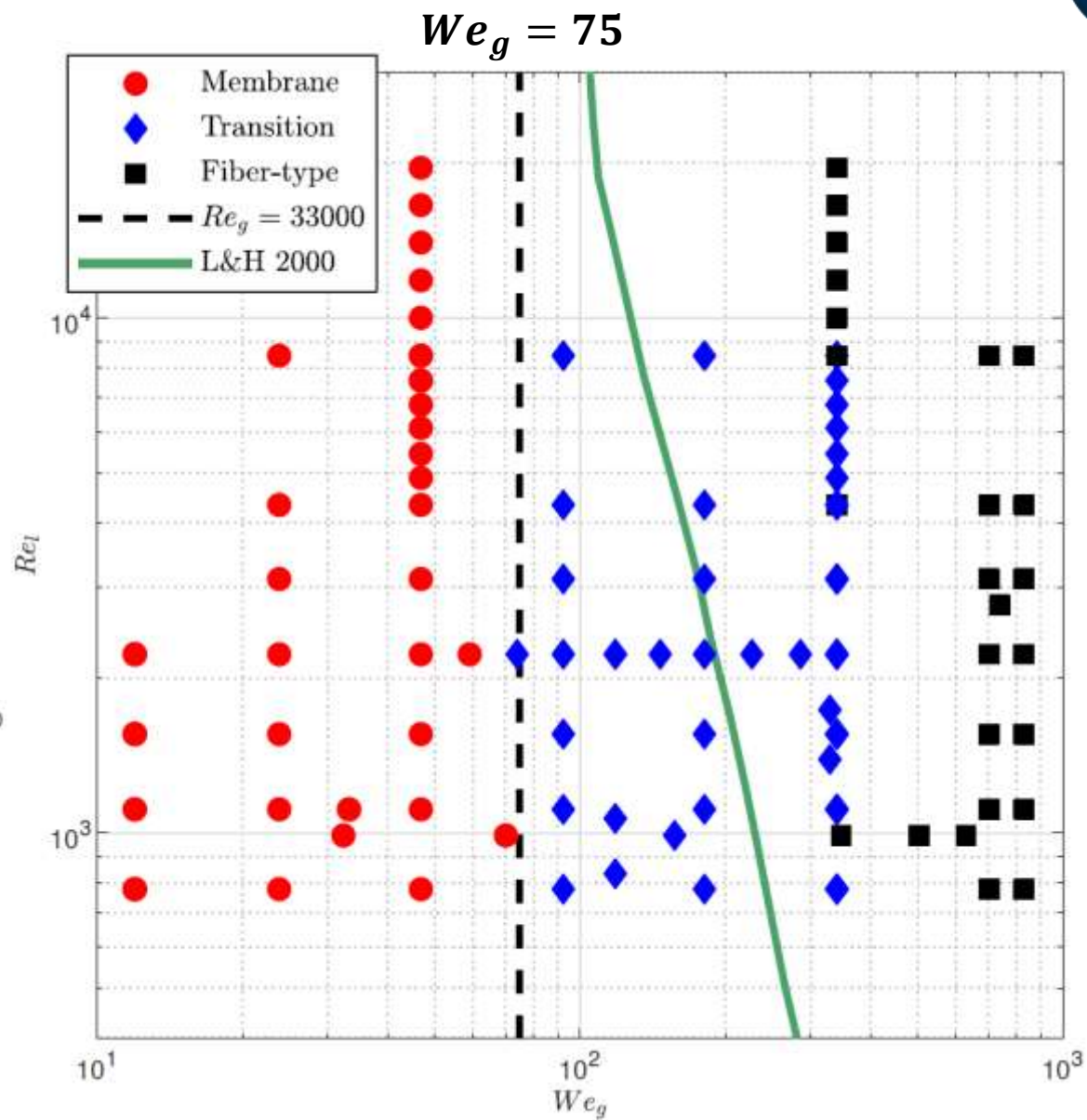
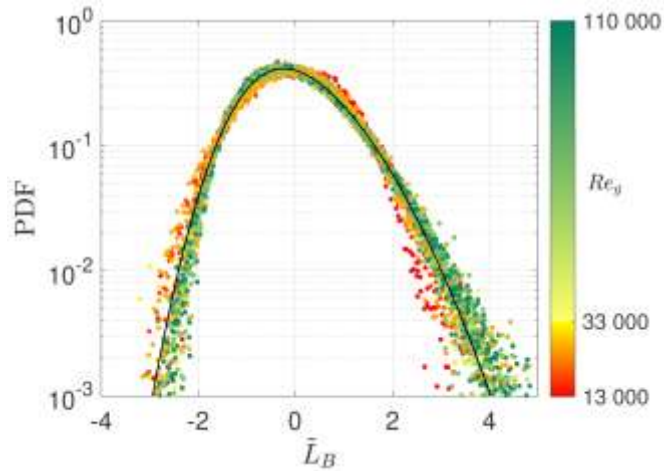
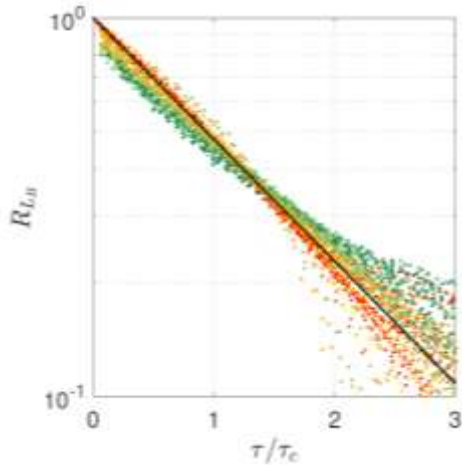


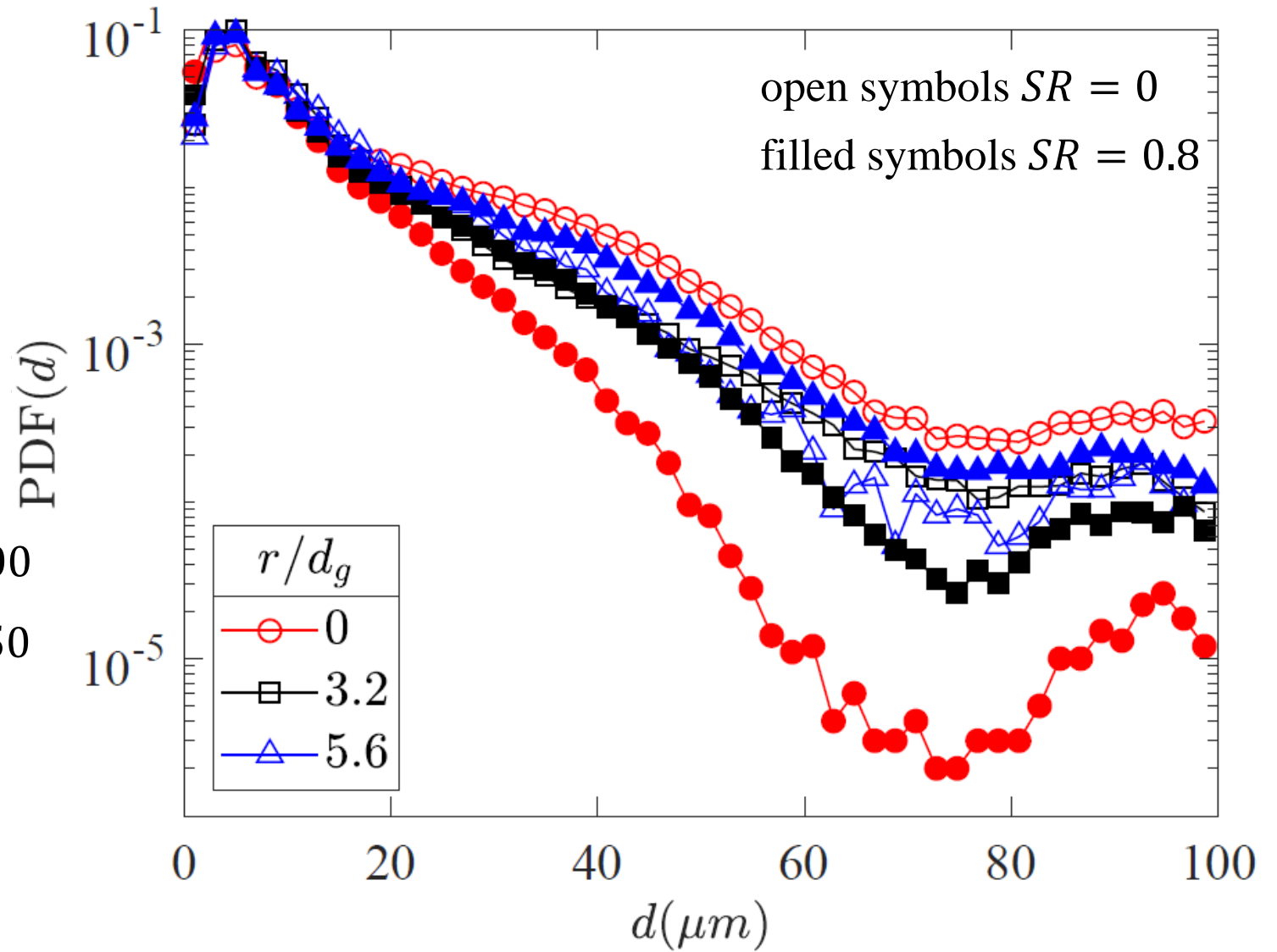
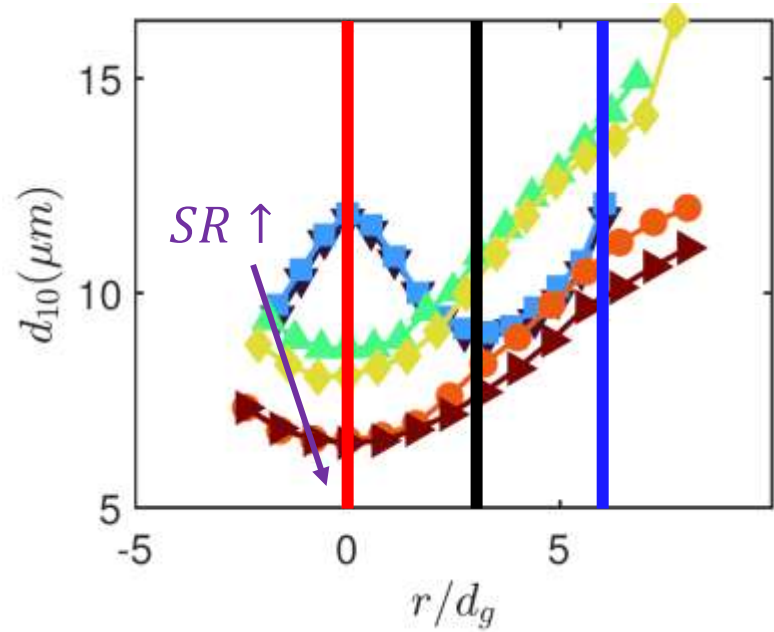


$$\tilde{L}_B = \frac{L_B - \langle L_B \rangle}{L_{B,STD}}$$

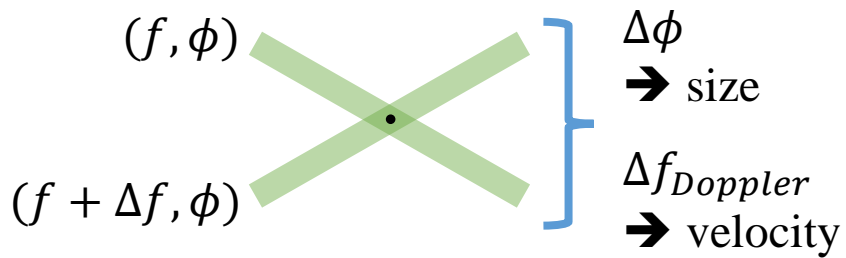
- Statistics
- Temporal dynamic

$$R_{L_B}(\tau) = \frac{\langle \tilde{L}_B(t) \tilde{L}_B(t + \tau) \rangle}{\langle \tilde{L}_B^2 \rangle}$$





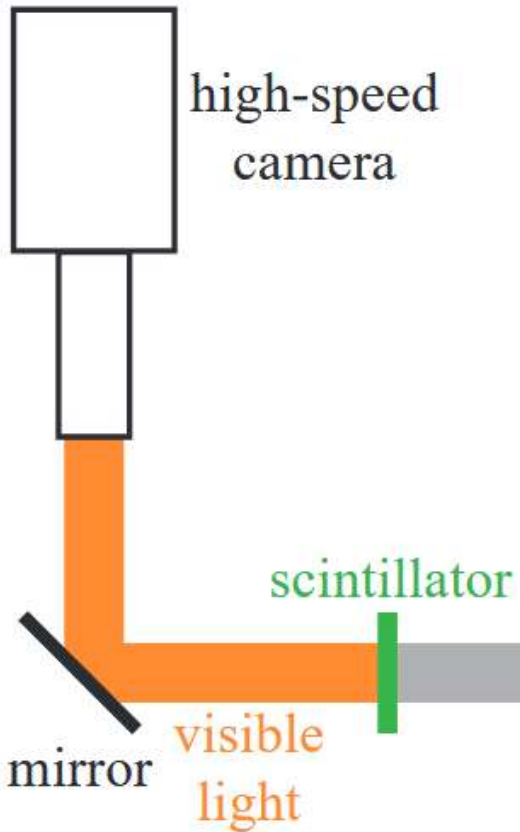
$Re_l = 1100$   
 $We_g = 850$



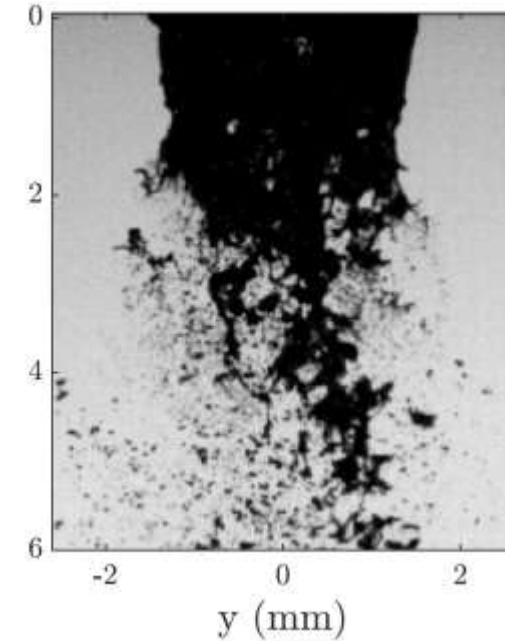
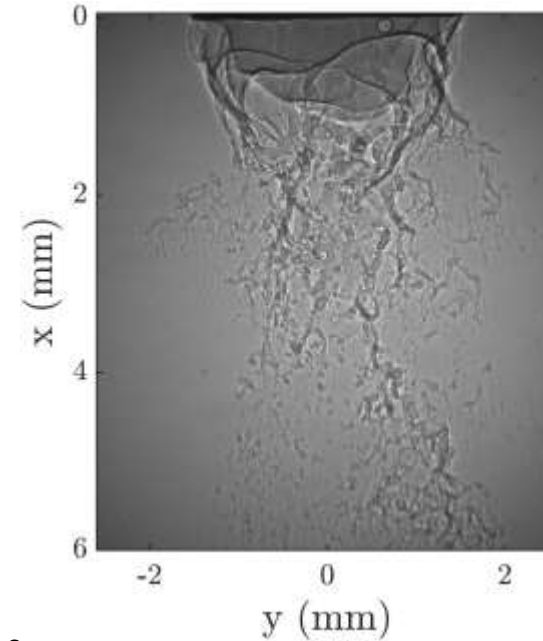
**Can we understand the shape of the PDF( $d$ ) and how they vary in high-speed spray conditions?**



A. Rack  
ID19



1 s acquisitions  
30 – 100 kHz  
7  $\mu\text{m}$  per px  
Field of view 7x7 mm<sup>2</sup>



$$800 < Re_l < 5000$$

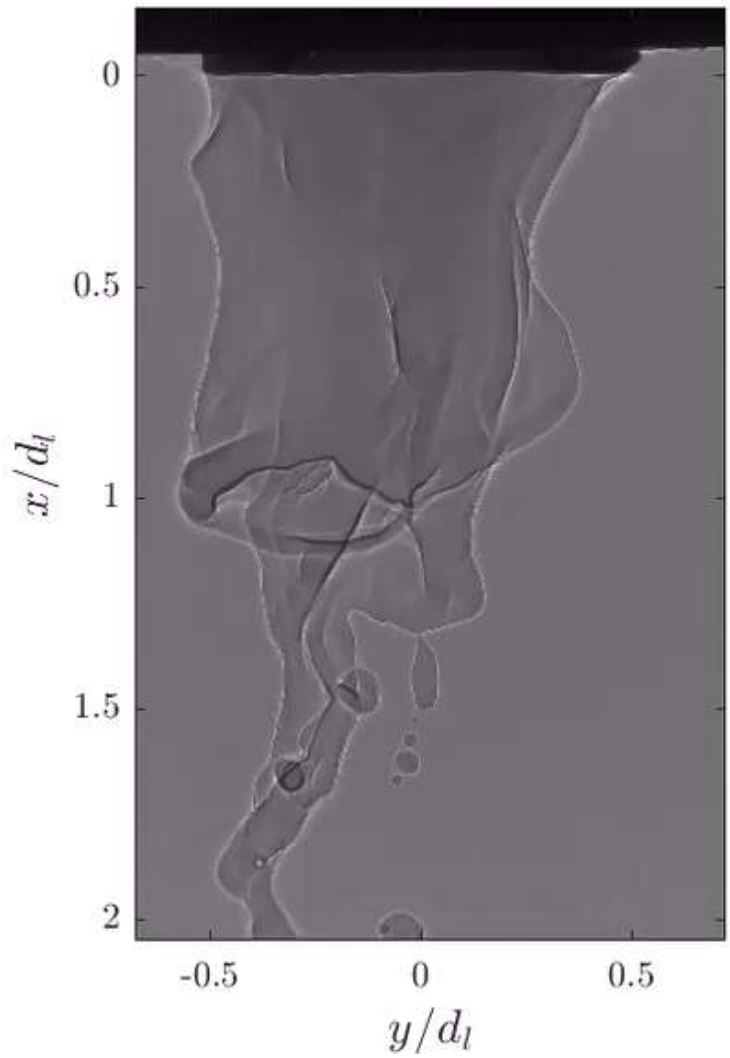
$$2 \cdot 10^4 < Re_g < 2 \cdot 10^5$$

$$30 < We_g < 3200$$

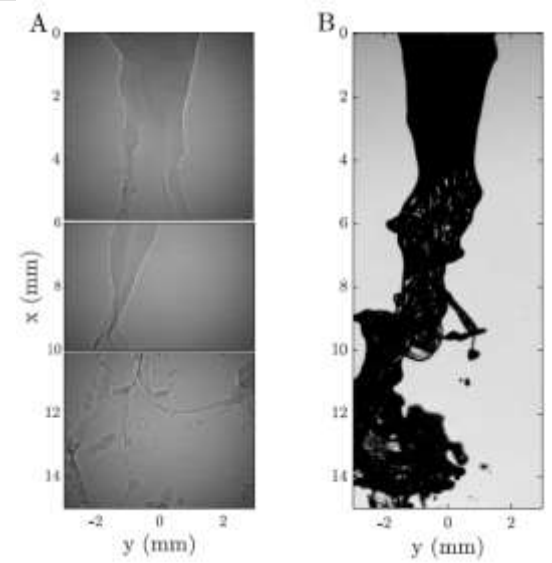
$$5 < M < 700$$

## Synchrotron X-ray high-speed imaging

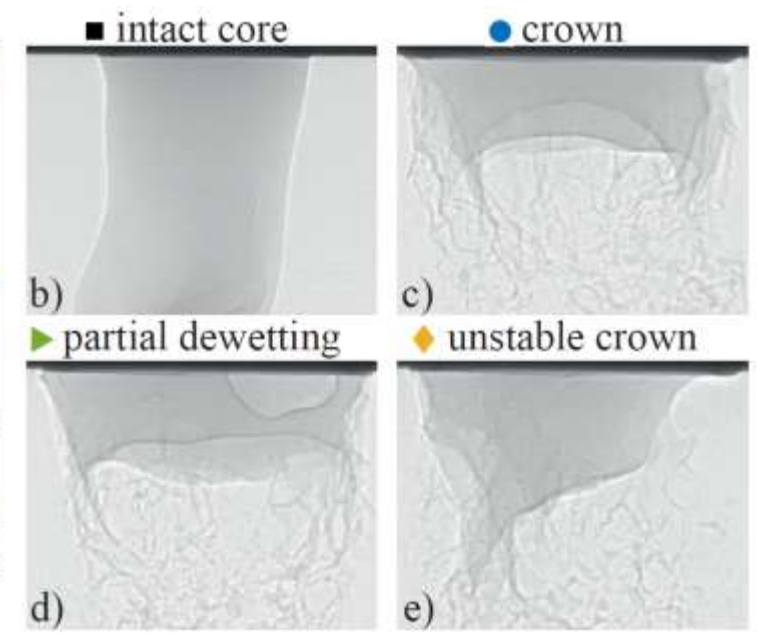
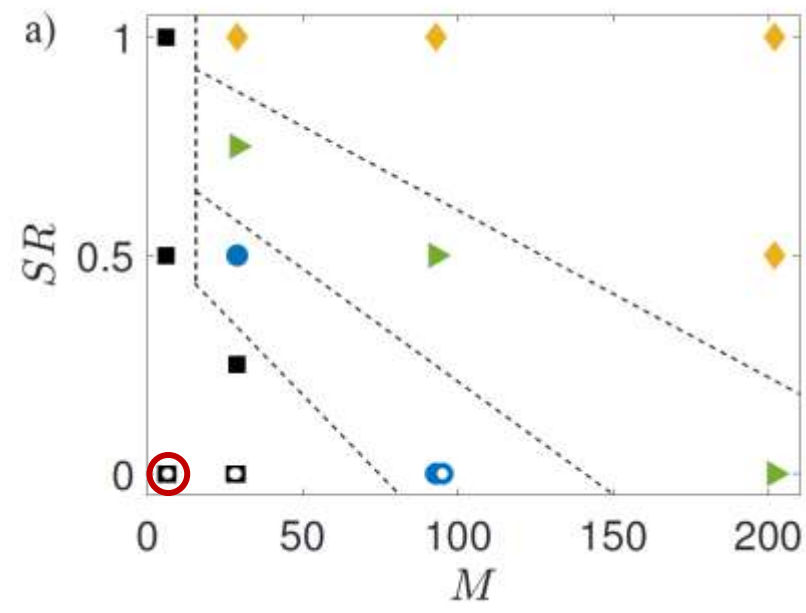
$Re_l = 800$        $We_g = 45$   
 0.00 ms      500  $\mu$ m



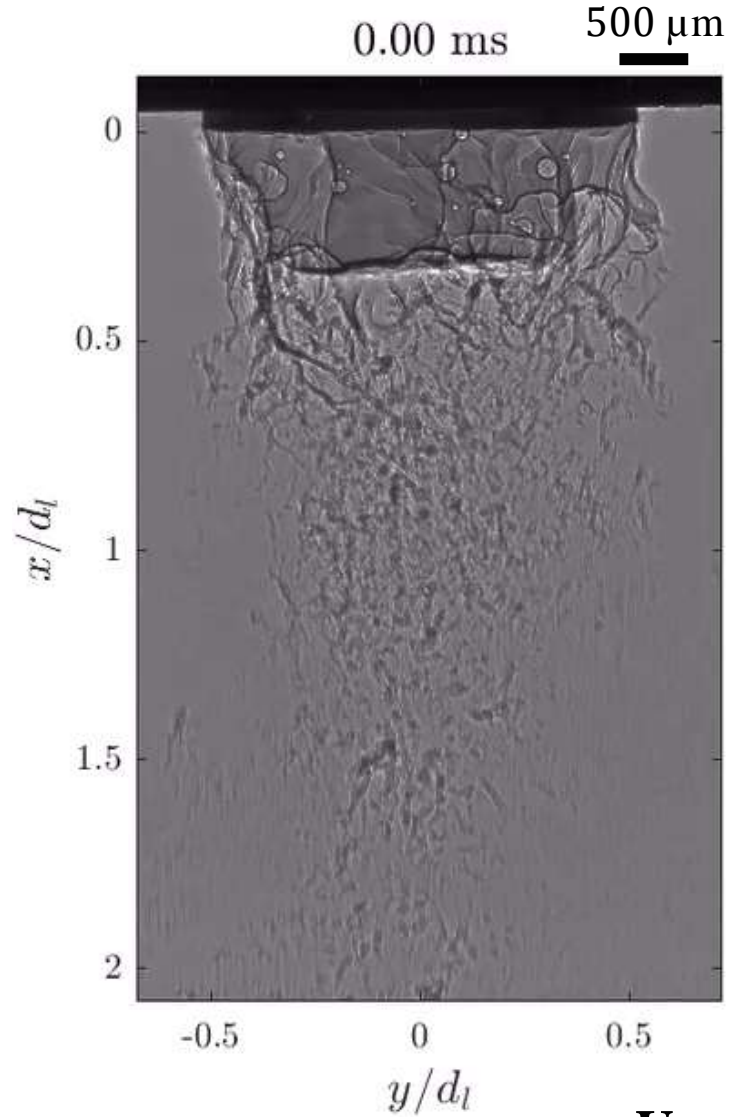
- No gas penetrated within the liquid jet's core
- Strong signature of flapping
- Formation of bags
- Localized Kelvin-Helmholtz perturbations
- Liquid structure reattachments encapsulate large air pockets
- Full wetting of the liquid nozzle with high curvature as the liquid jet is accelerated



*Machicoane et al., IJMF 2019*

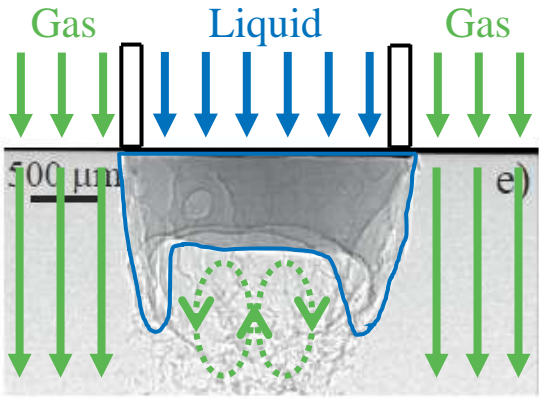


$Re_l = 1100$     $We_g = 800$



*Machicoane et al., IJMF 2019*

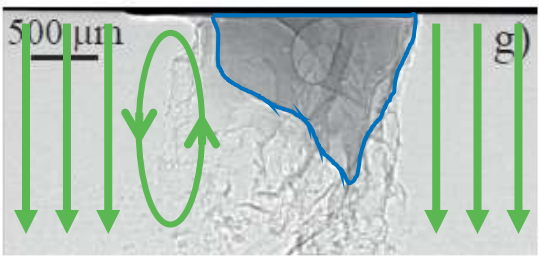
$Re_l = 1100, We_g = 1350$



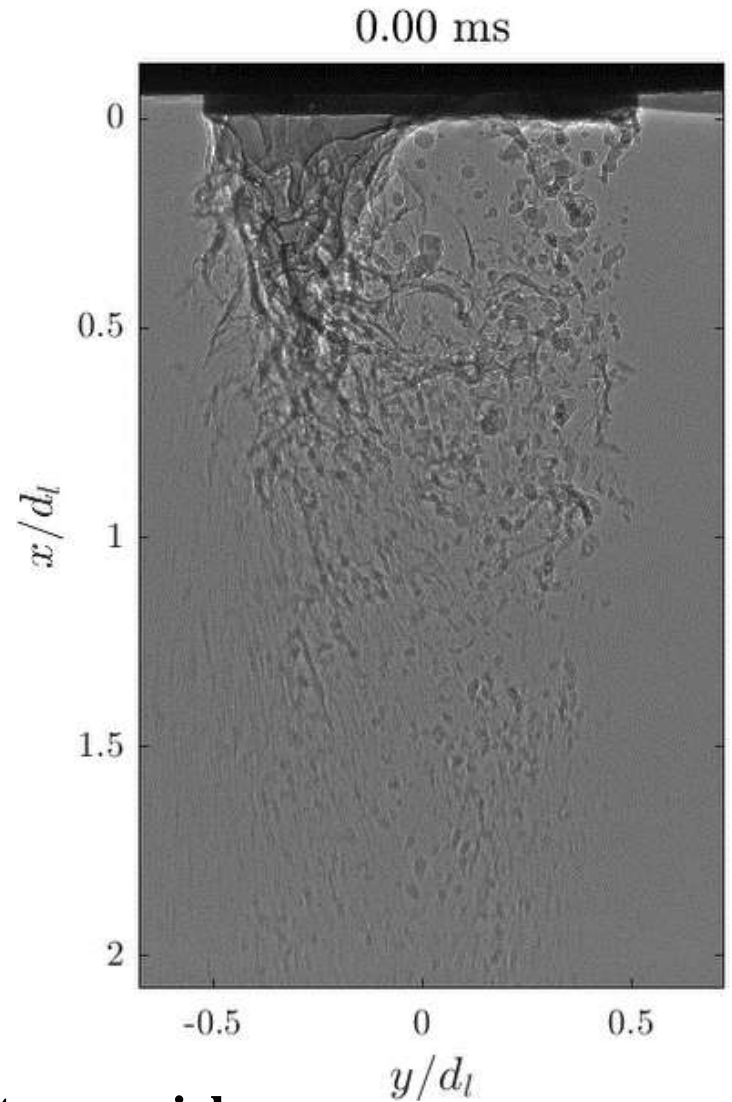
Crown

with gas swirl

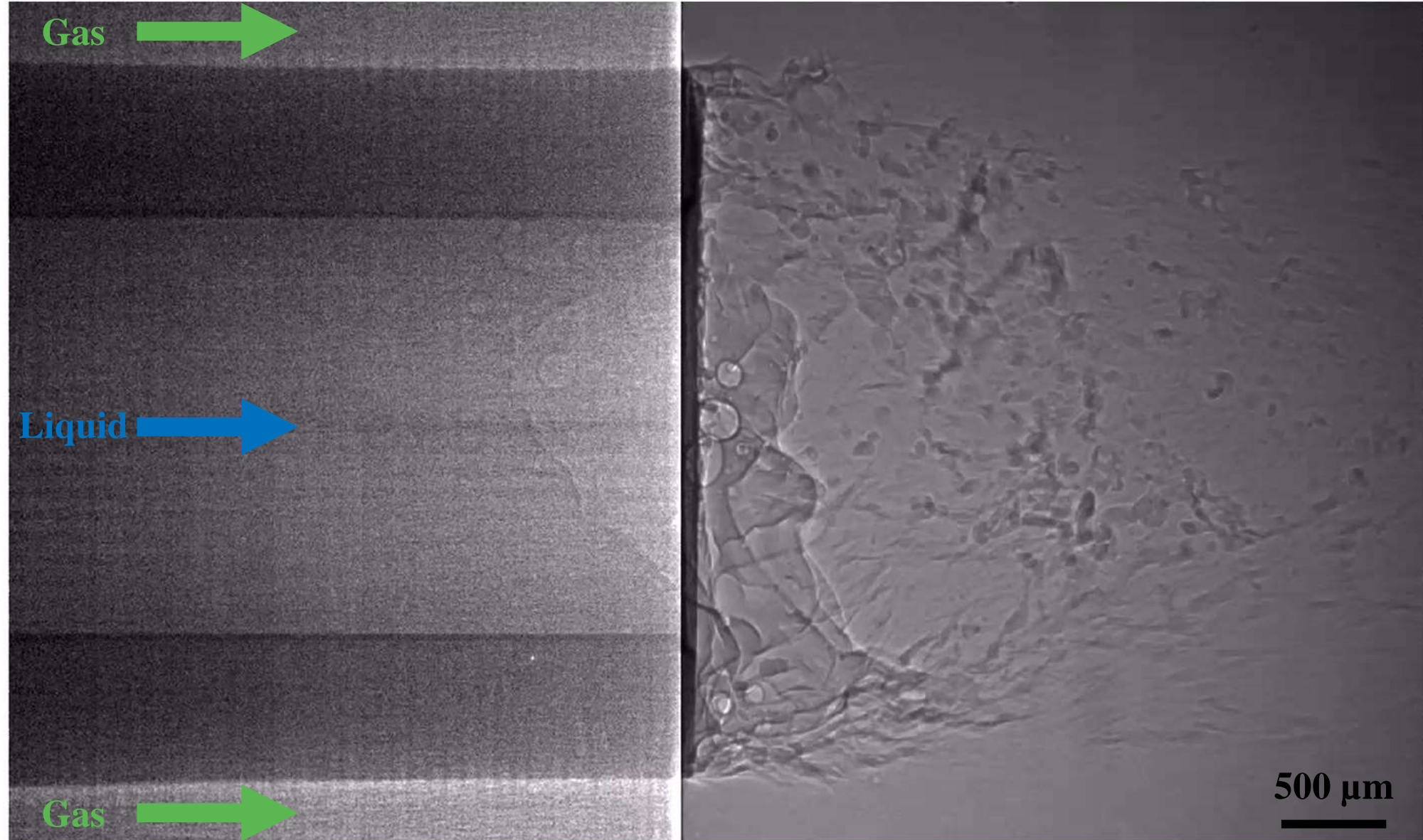
→ Unstable crown



$Re_l = 800$     $We_g = 1100$

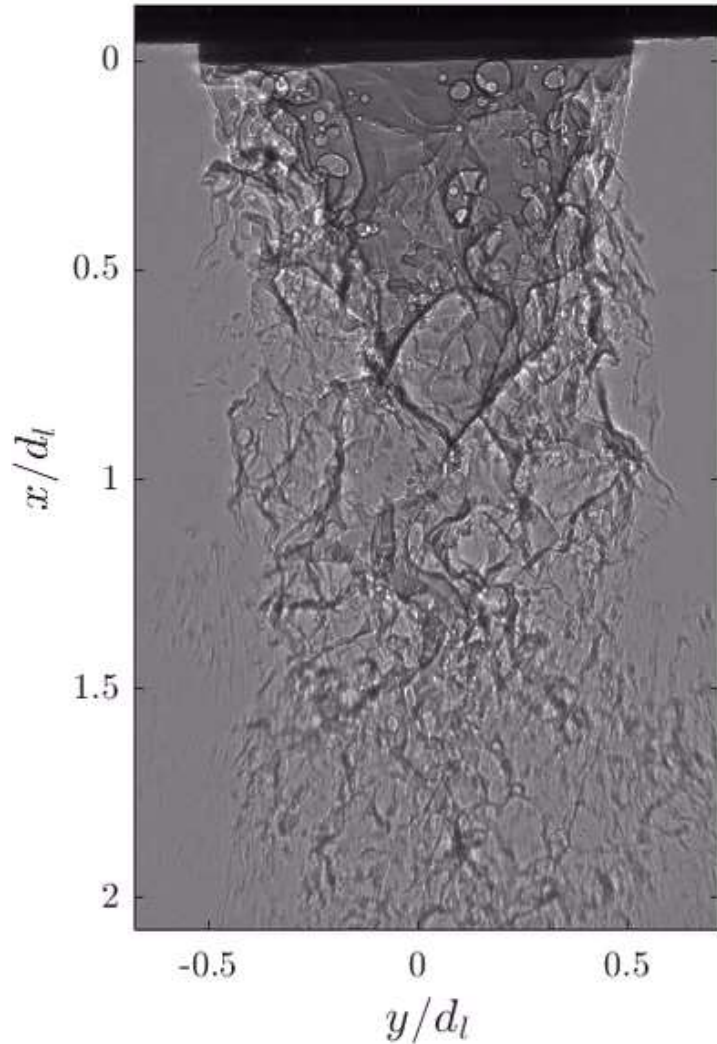


**Unstable crown at extreme  $M$  values, without gas swirl**



$Re_l = 3100$     $We_g = 800$

0.00 ms   500  $\mu$ m

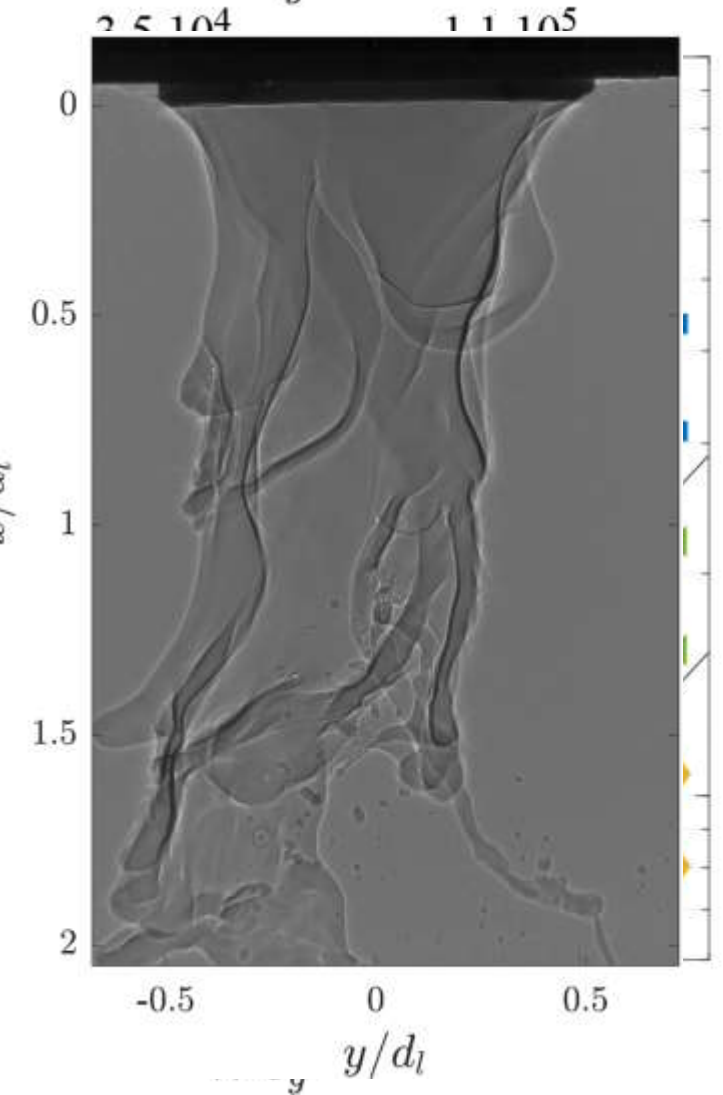


- Many overlapping interfaces
- Many smaller-scale gas recirculations
- « Perforated core » transition between intact core and crown

$$M = \frac{\rho_g u_g^2}{\rho_l u_l^2}$$

**Kinetic energy arguments seem in good agreement for transition to crown and unstable crown**

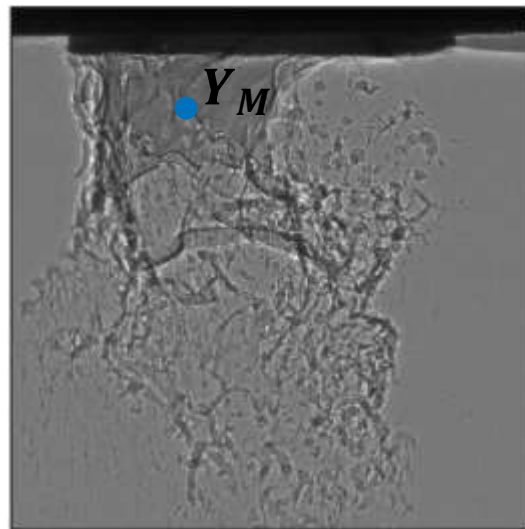
Intact core at  $Re_l = 800$     $We_g = 45$





# Quantitative identification of unstable crown and role of swirl

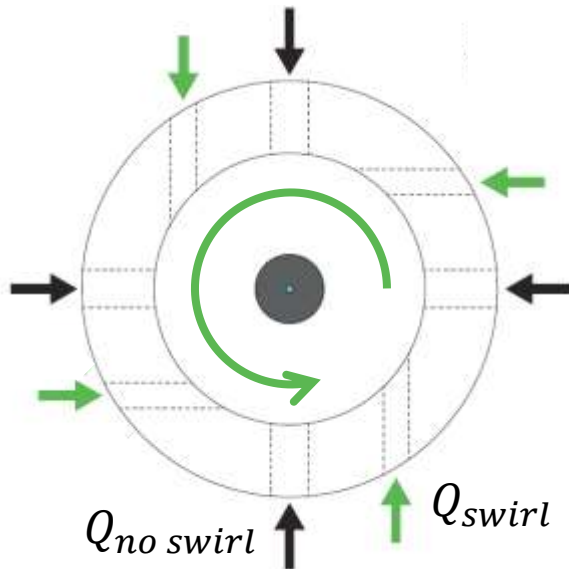
X-ray absorption by the liquid jet follows Beer-Lambert's law



Center of mass along y

→ Equivalent path length

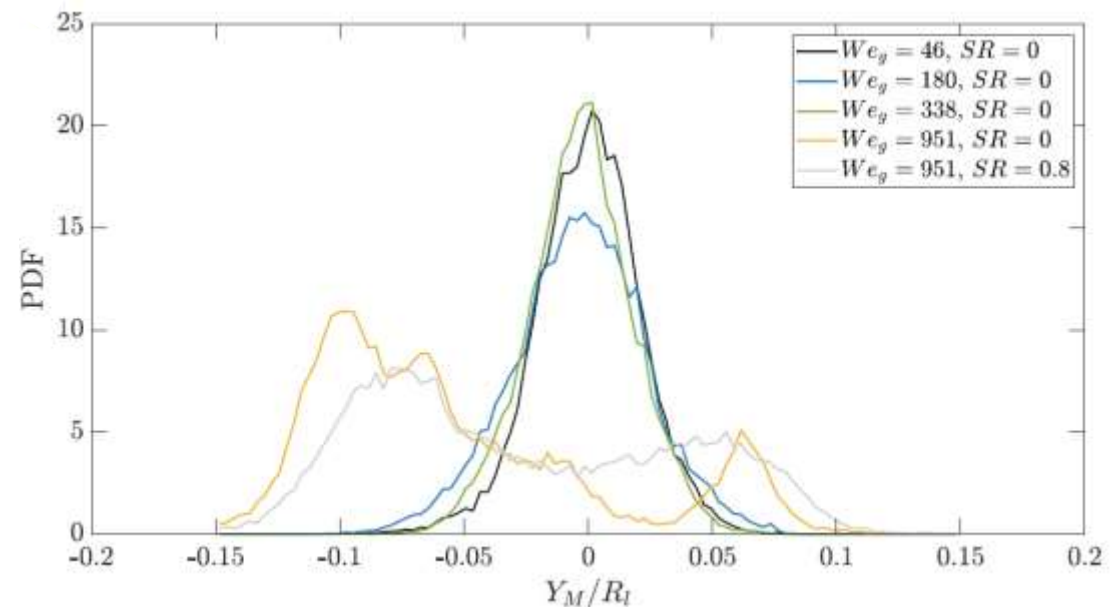
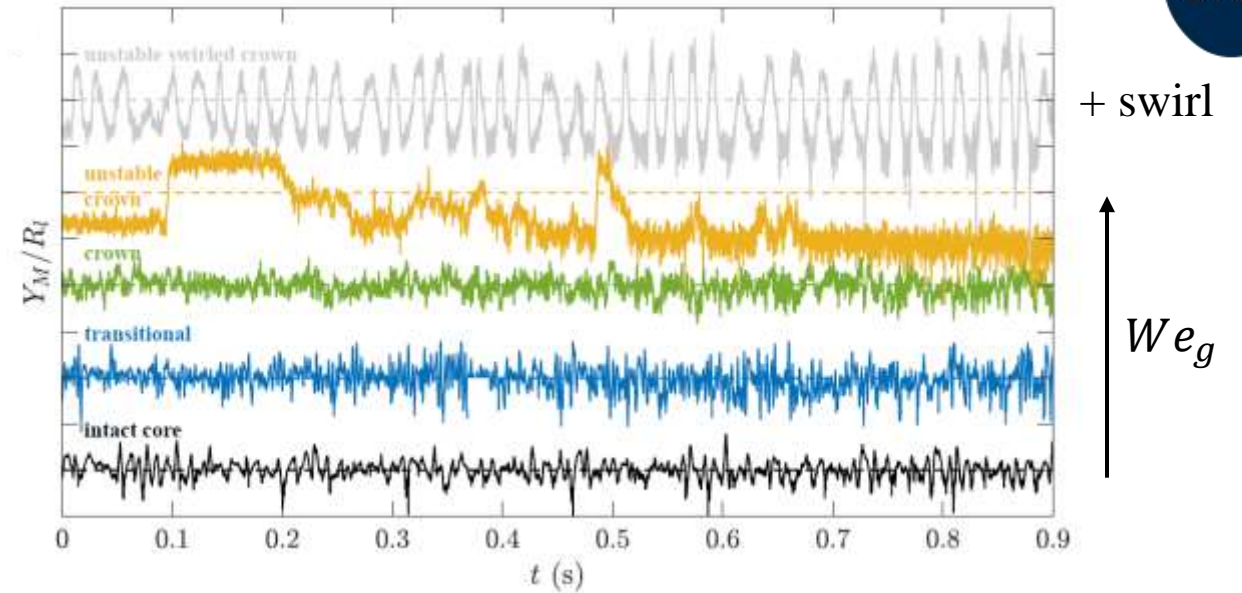
using ANKA Phase  
Weitkamp et al.  
*J. of Synchrotron  
Radiation 2011*



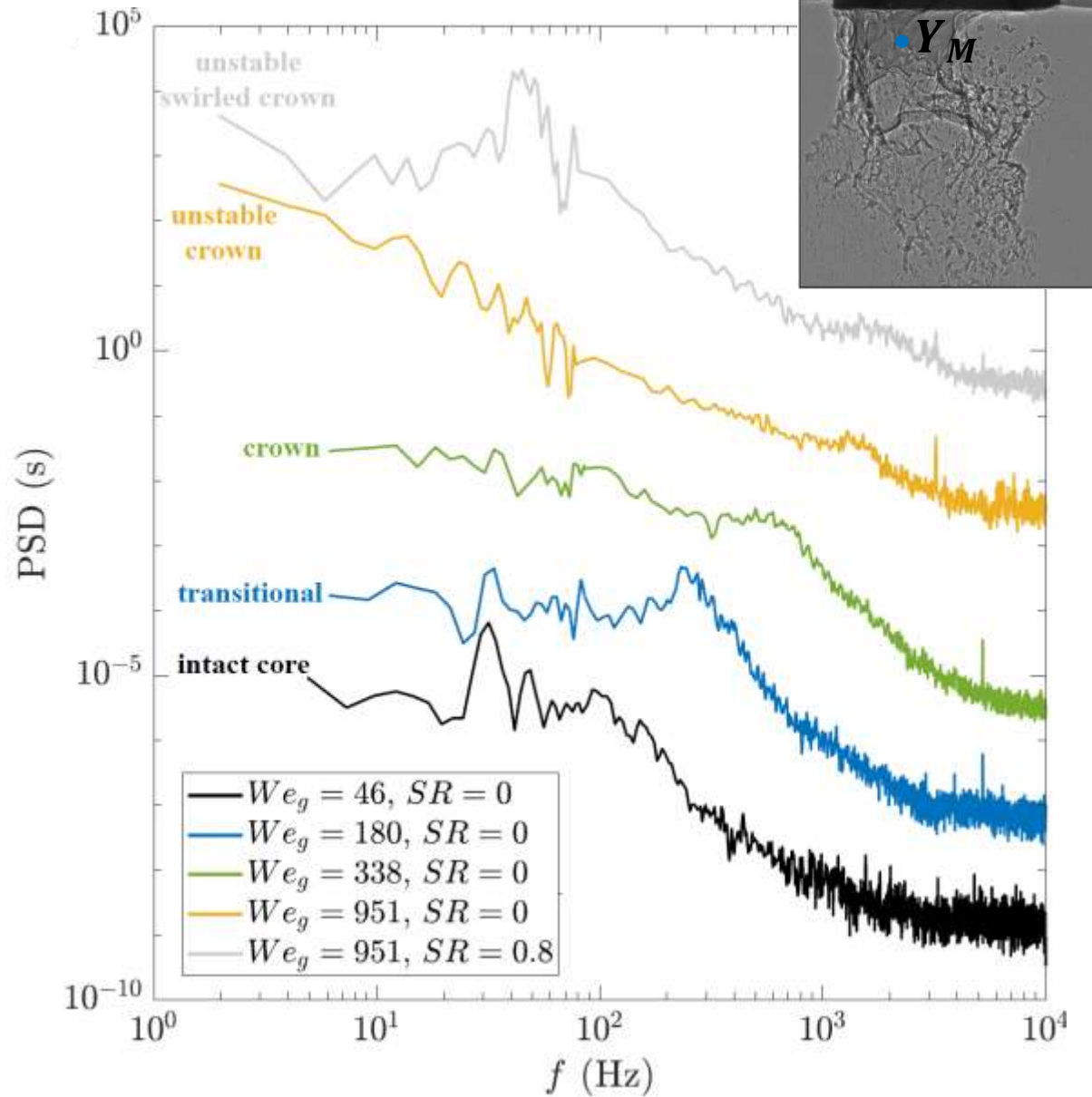
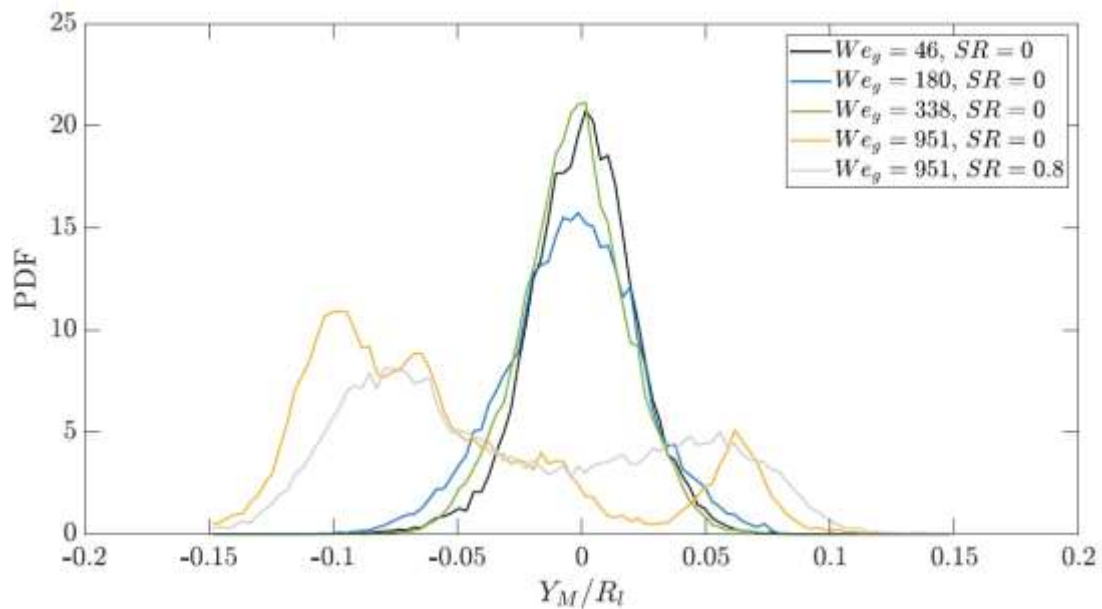
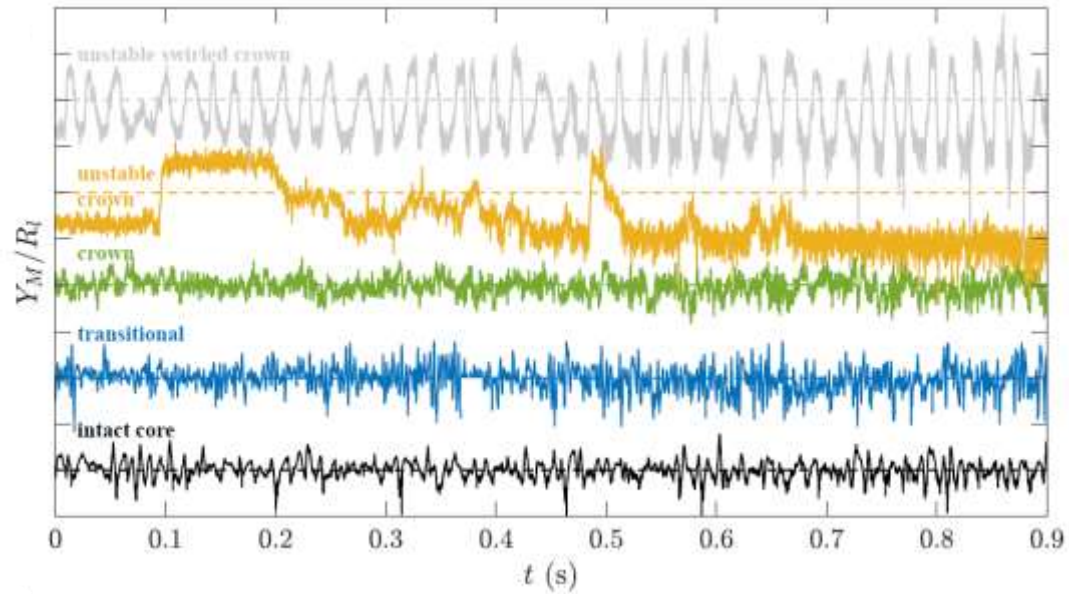
$$Q_{Total} = Q_{SW} + Q_{NS} = cst$$

$$SR = \frac{Q_{swirl}}{Q_{no\ swirl}}$$

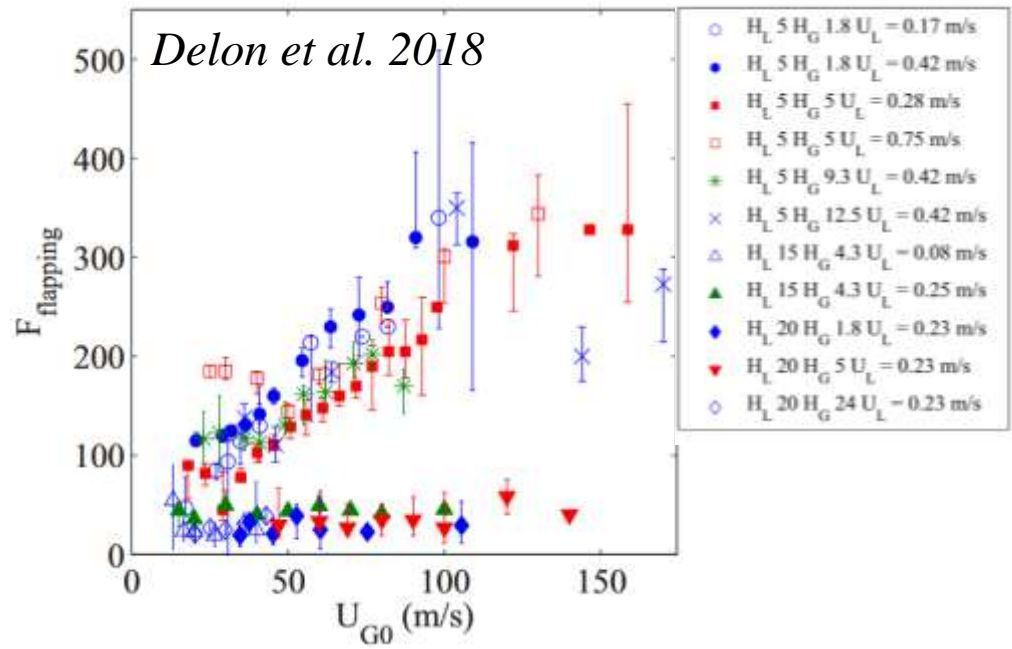
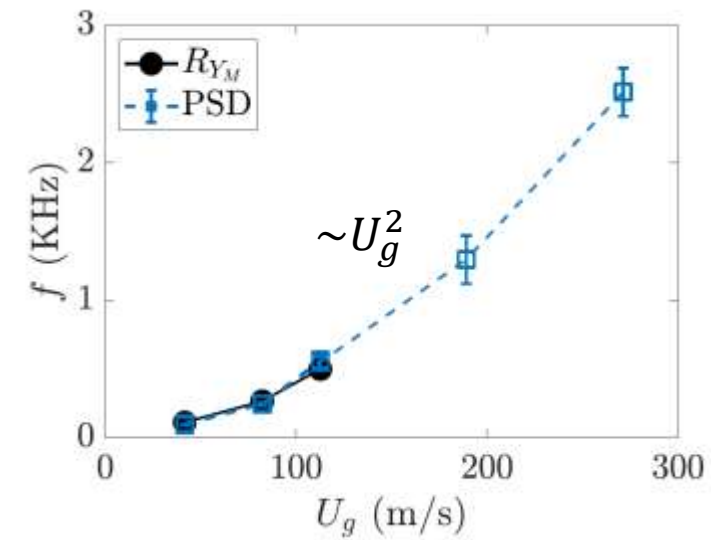
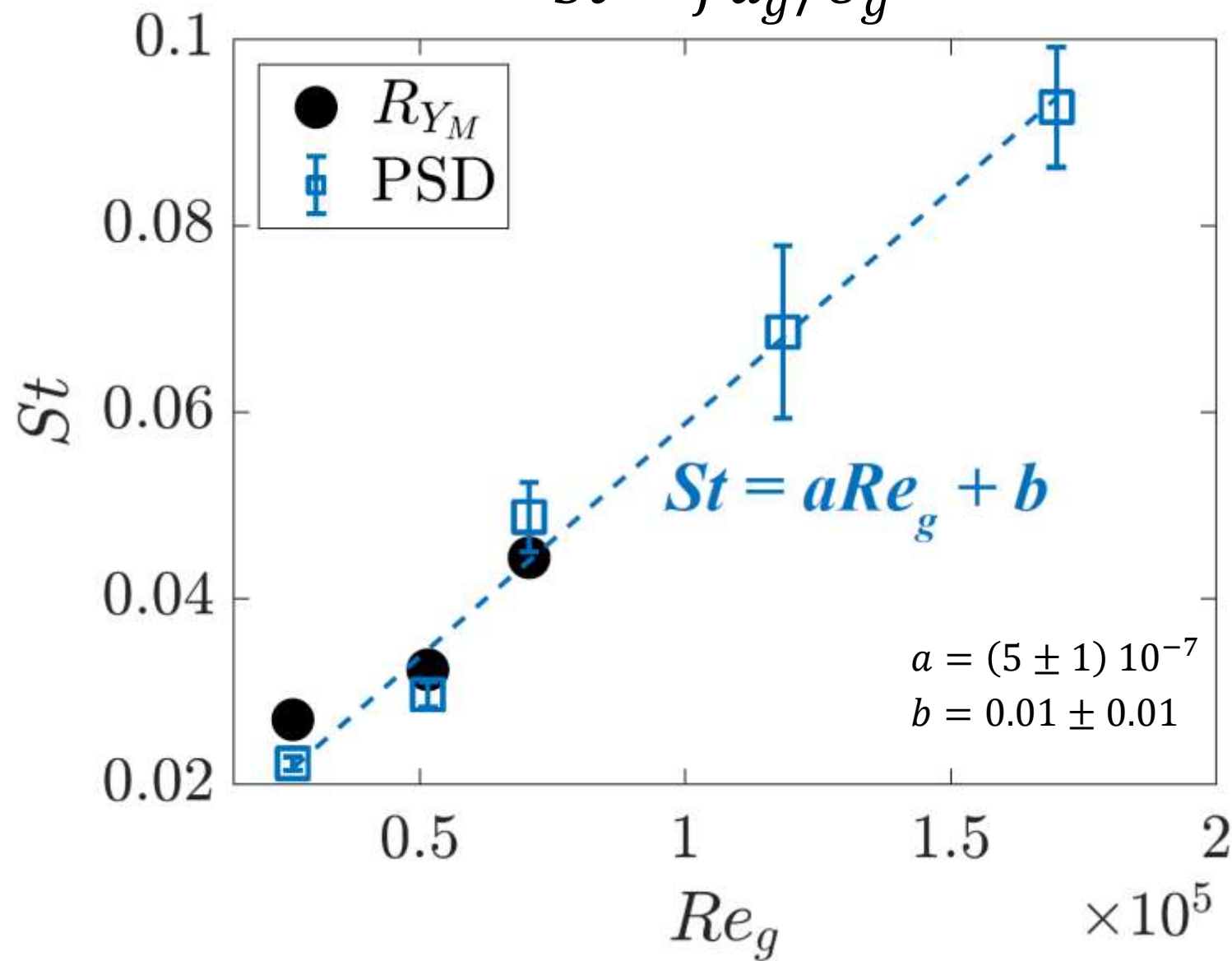
$$Re_l = 800$$



# Quantitative identification of unstable crown and role of swirl

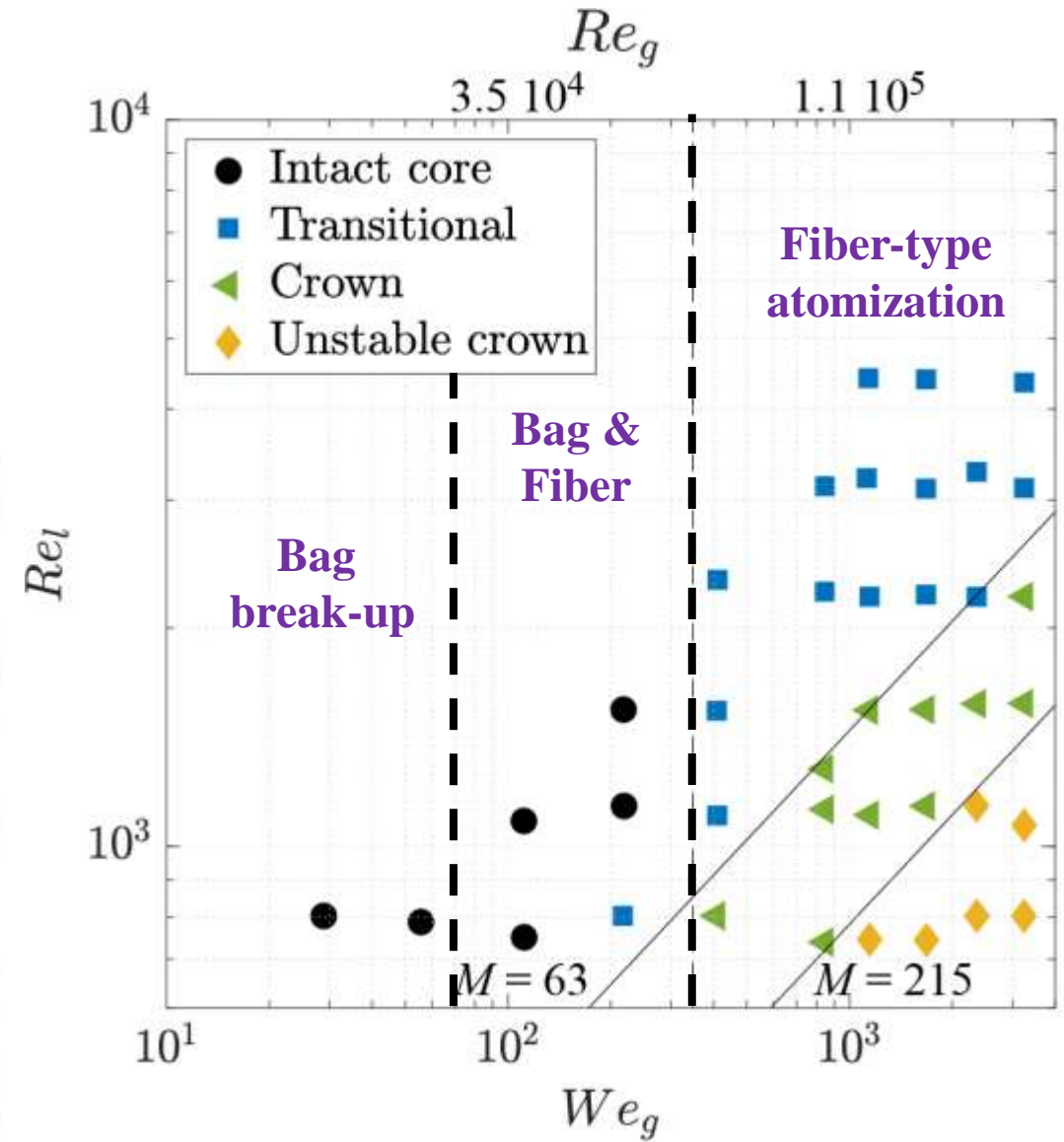
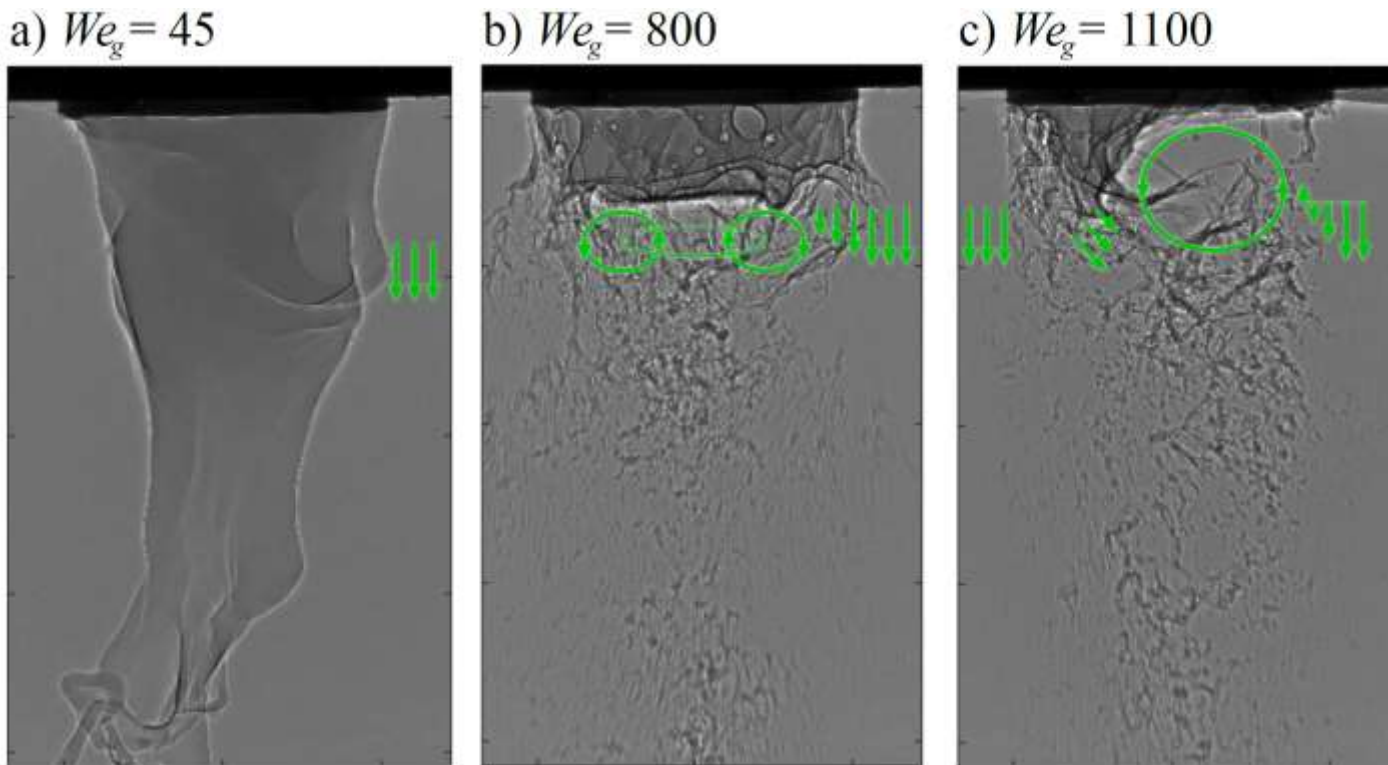


$$St = f d_g / U_g$$



# General conclusion

- At higher  $We_g$ , liquid core undergoes transitions, up to unstable crown, even without gas swirl
- Changes in atomization regimes and liquid core morphologies are entangled
- Gas swirl leads to earlier onset of unstable crown and much more frequent motions of the gas recirculation
- Study other mechanisms (e.g., flapping and instabilities) with swirl to try and relate to droplet size distributions



# Thank you for your attention

**February 10-14, 2025**

Winter school NCTR VII

New Challenges in Turbulence Research

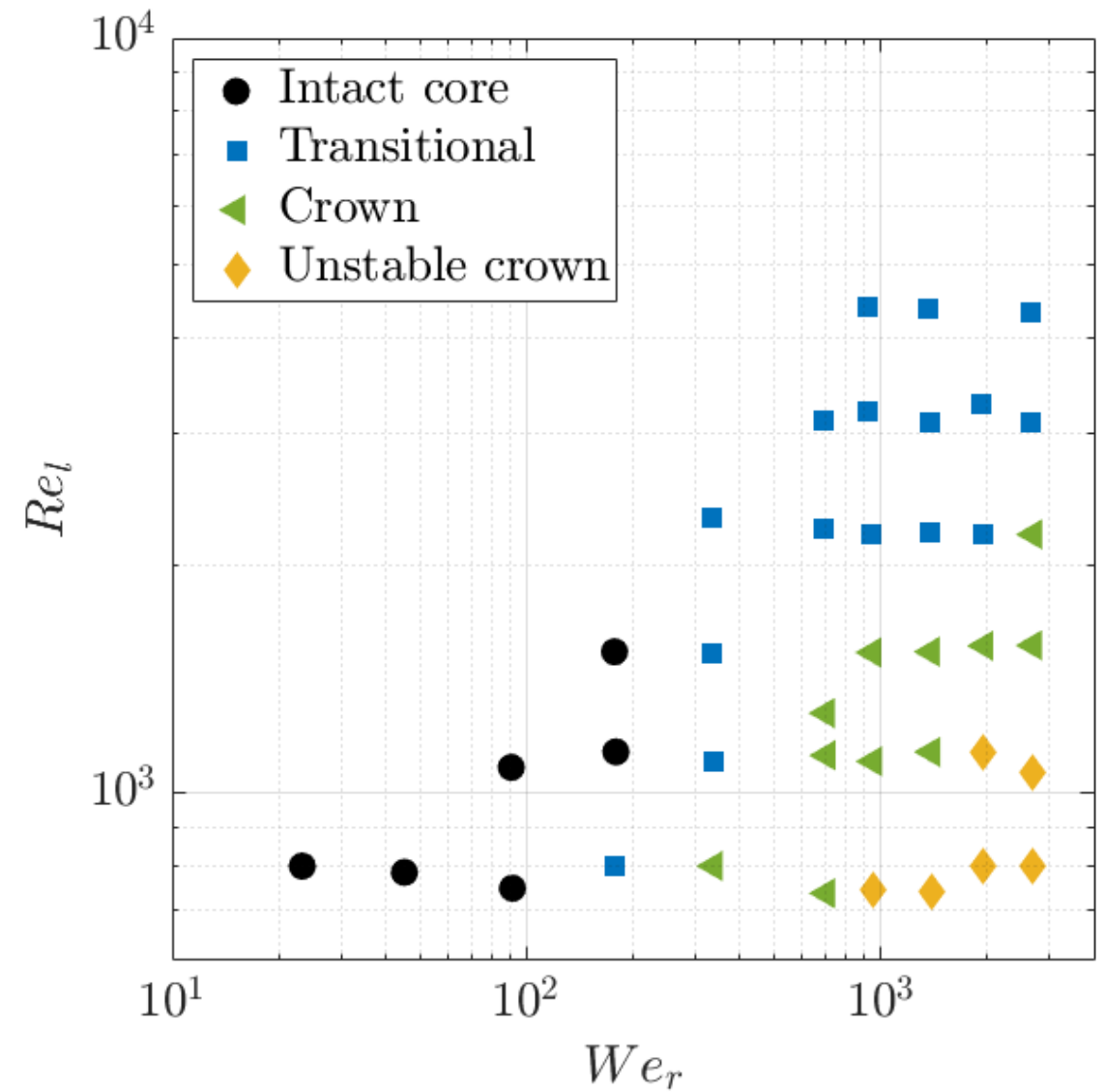
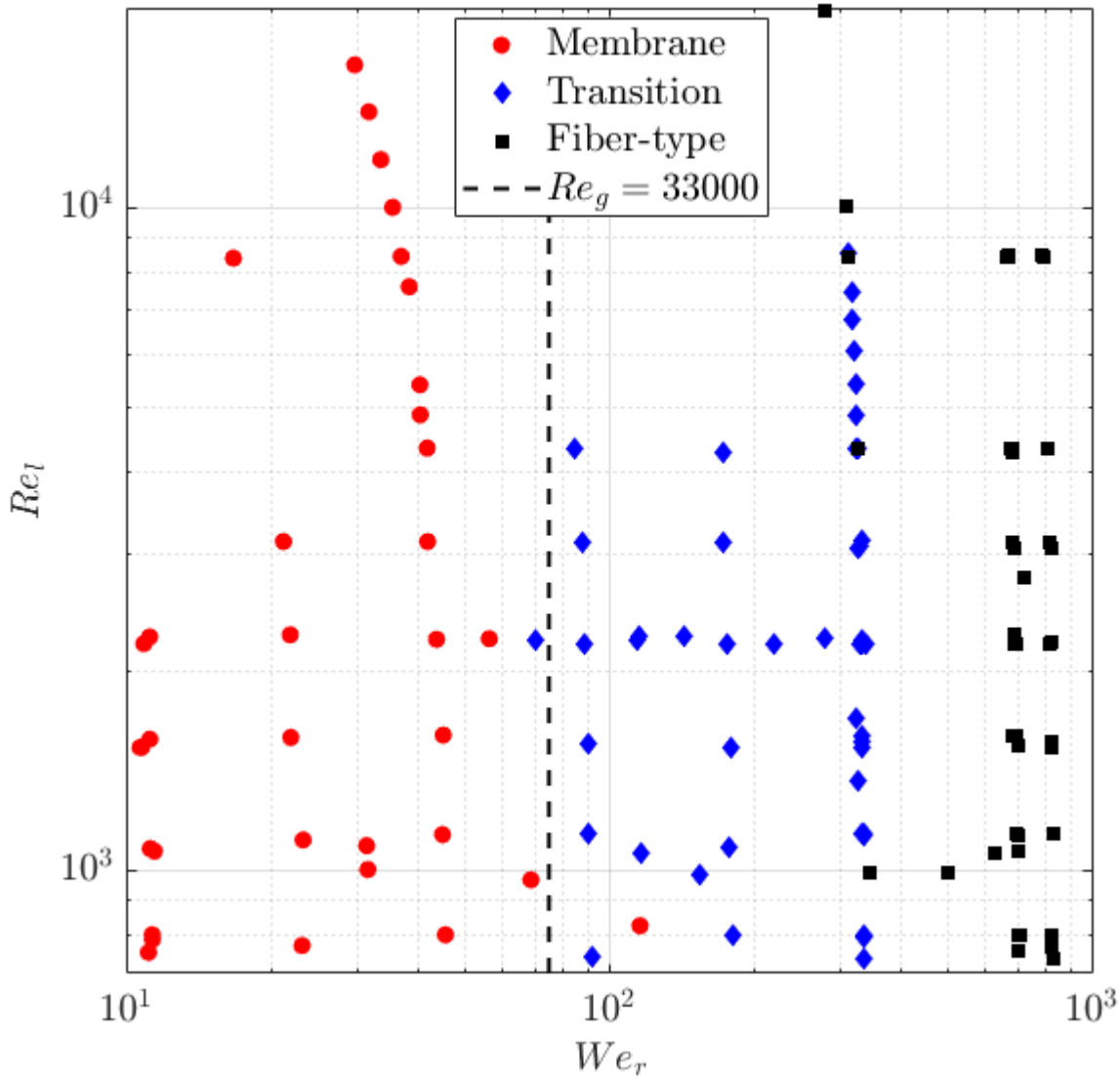


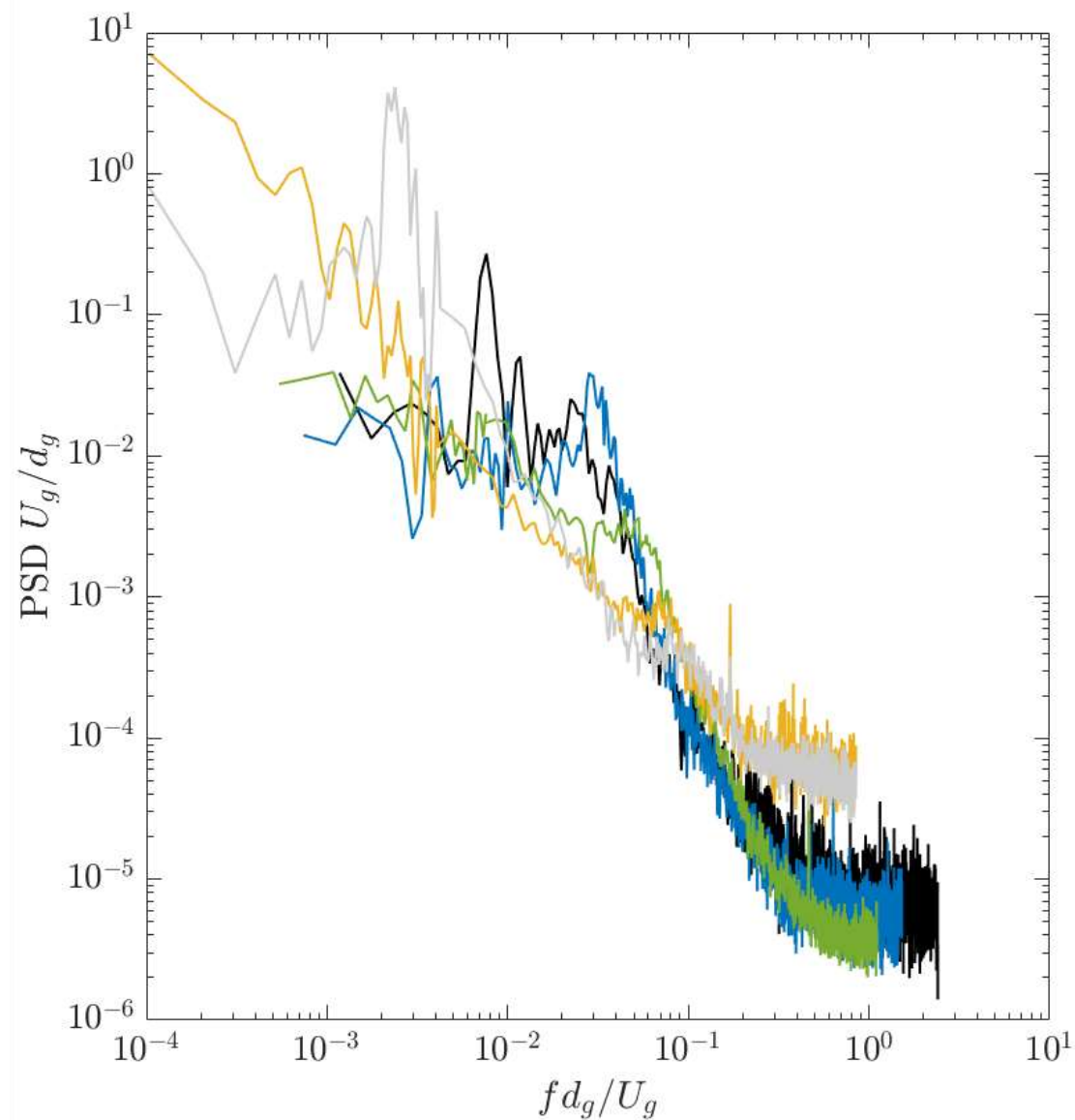
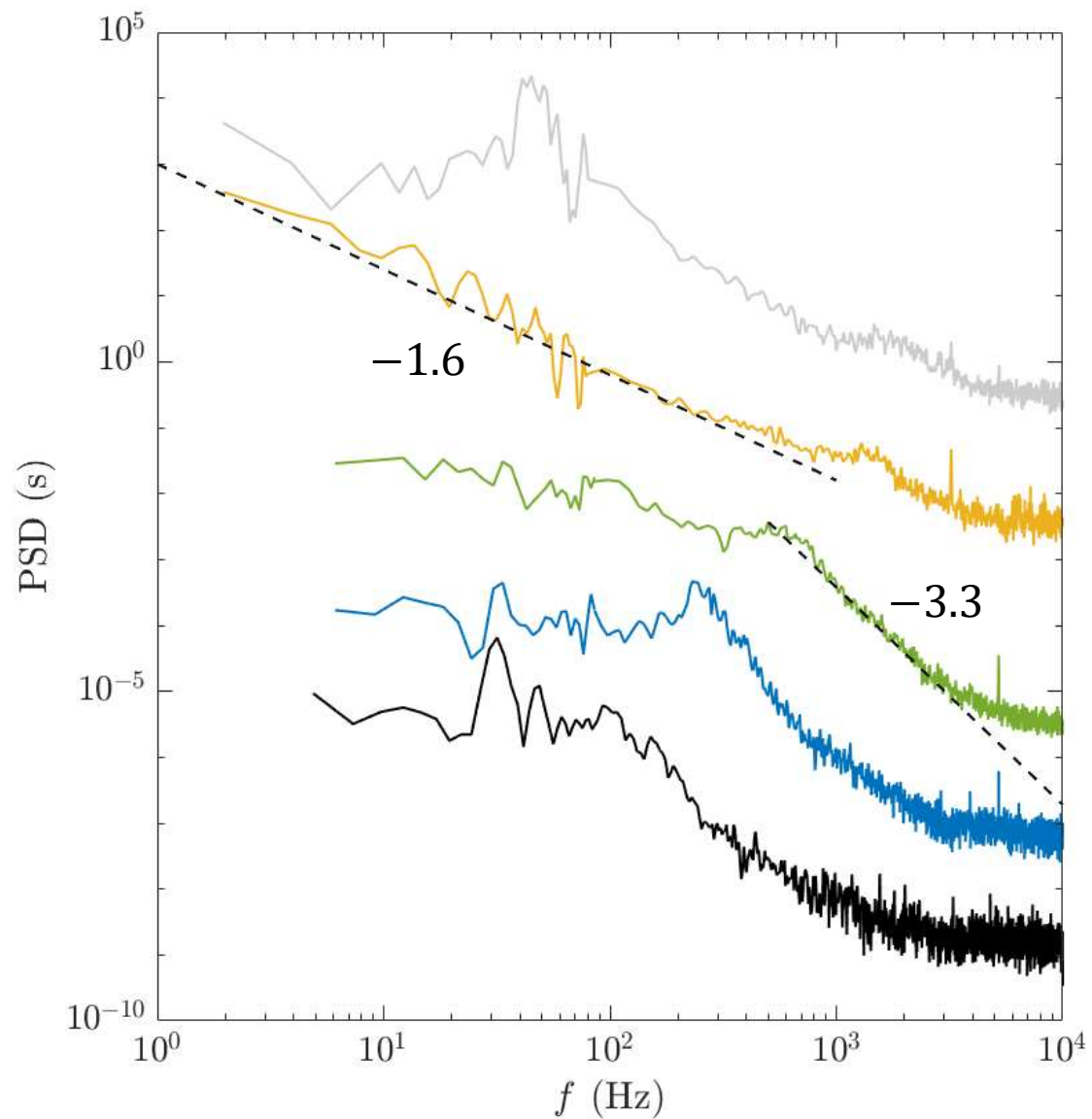
ÉCOLE DE  
**PHYSIQUE**  
**DES HOUCHES**



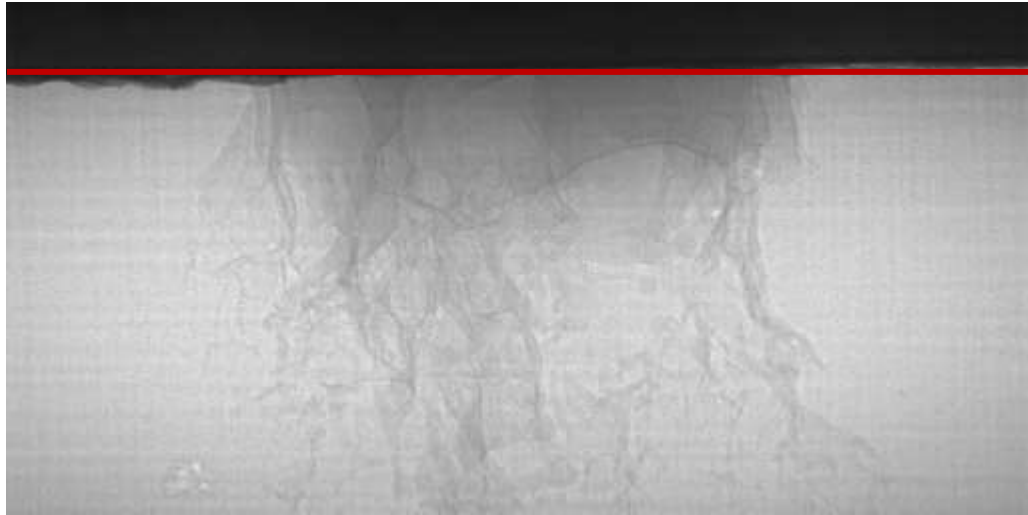


Based on slip velocity  $We_r = \frac{\rho_g(u_g - u_l)^2 d_l}{\sigma}$









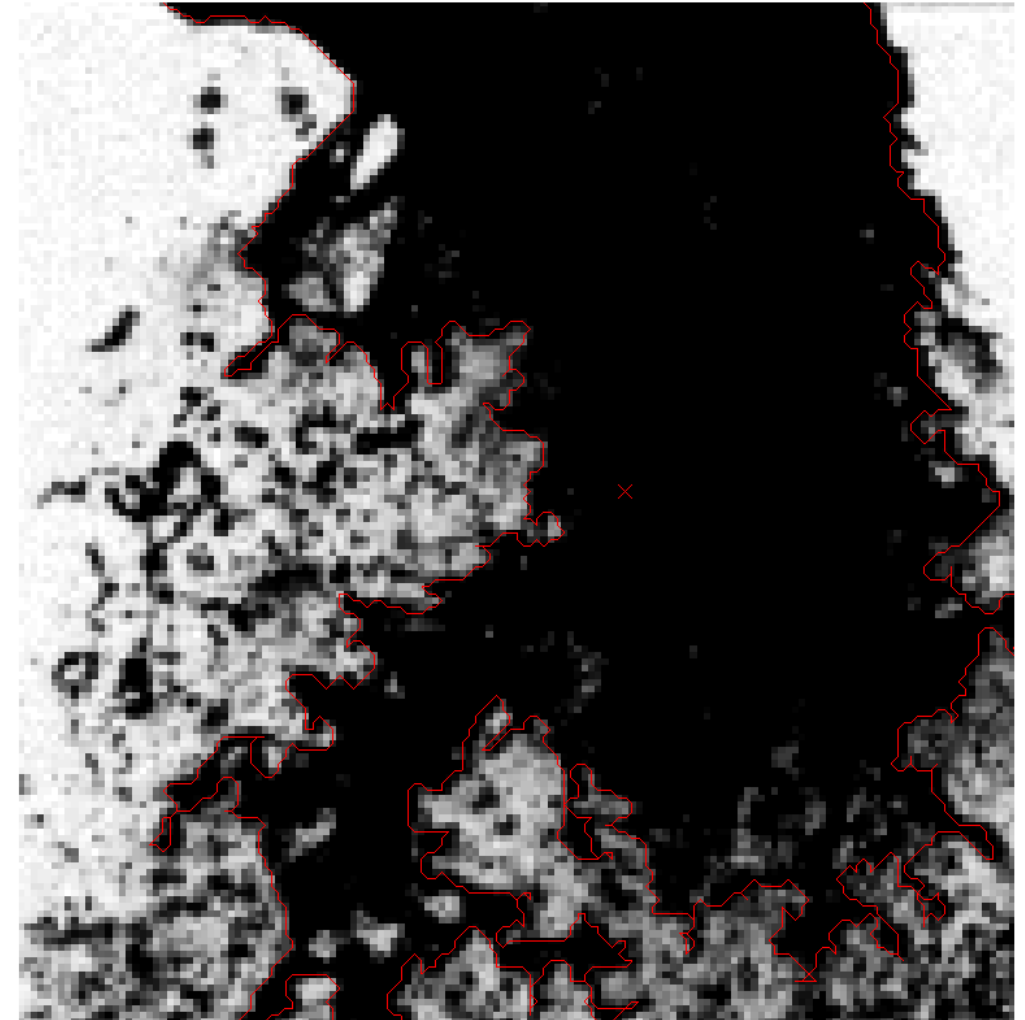
$x = 0$

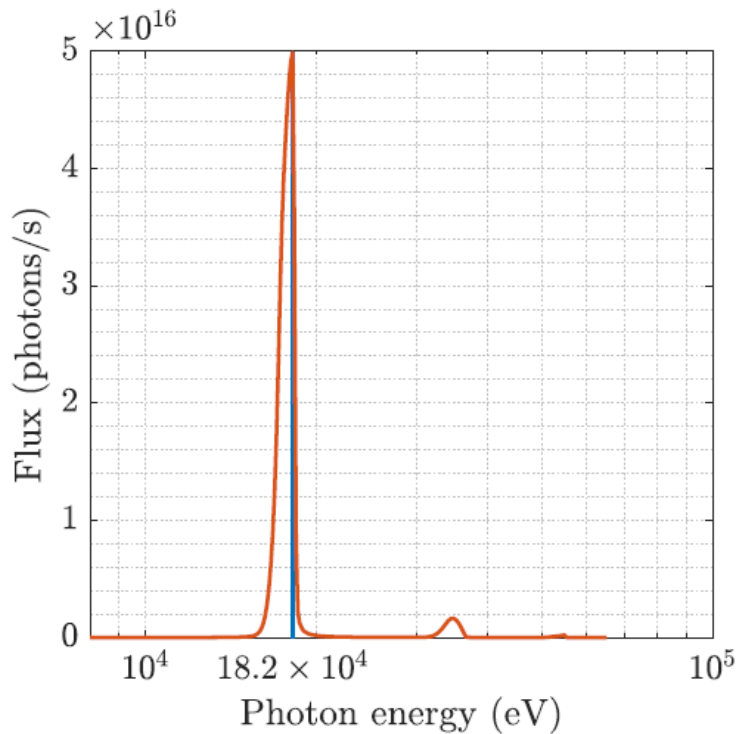


$x = 0.21d_g$

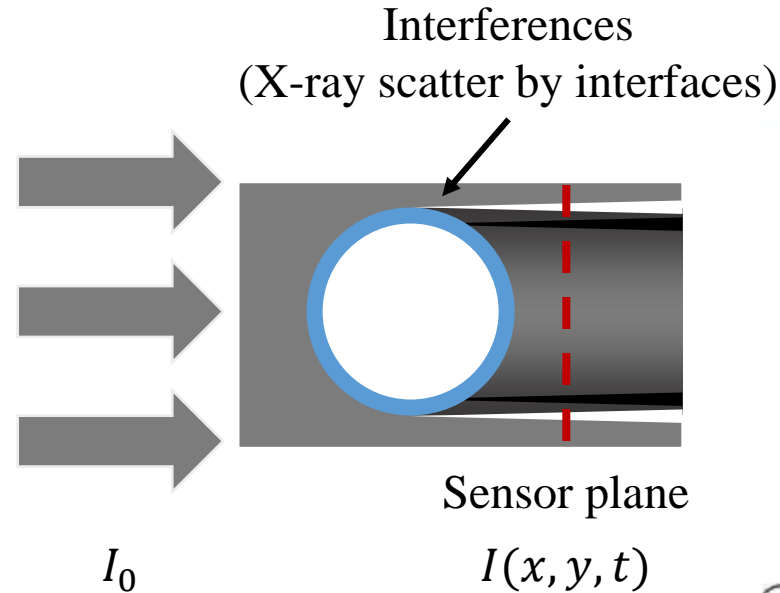
$x = 0.17d_g$

$x = 0.41d_g$





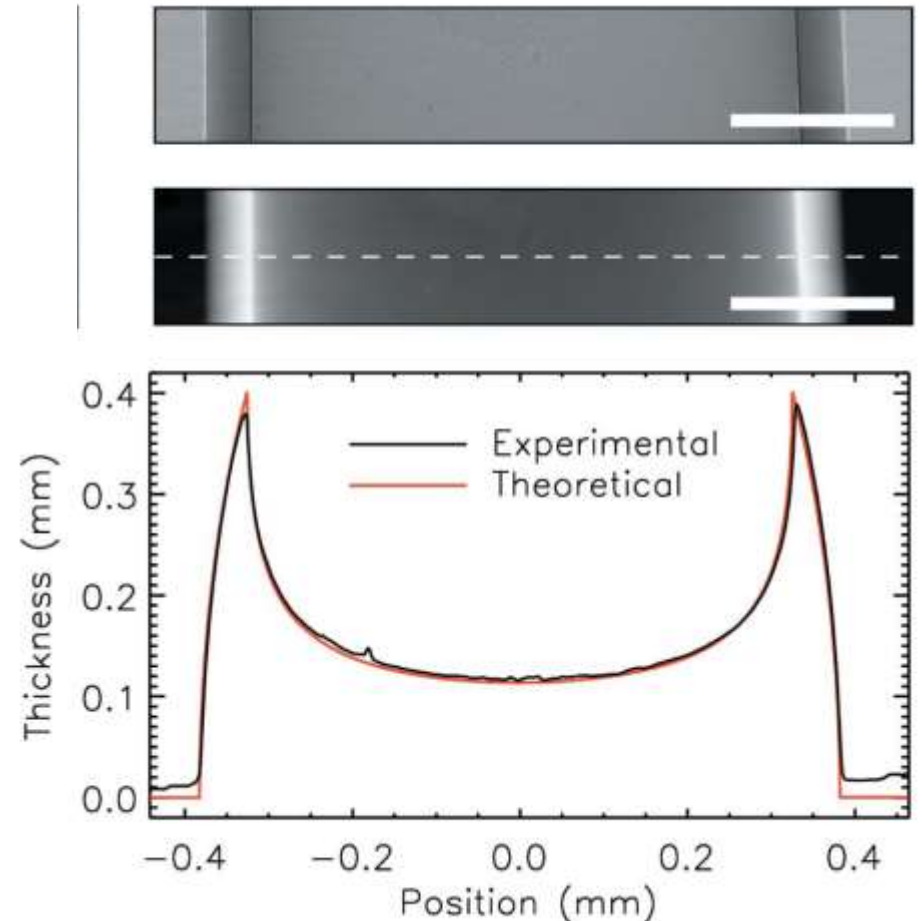
Incoming X-ray beam energy spectrum



$$\frac{I(x, y, t)}{I_0(x, y)} = \int e^{-\mu(\lambda)h(x,y,t)} d\lambda$$

- Remove interferences  $f(x, y, \lambda)$
- Retrieve phase map  $\phi$
- Convert into EPL map

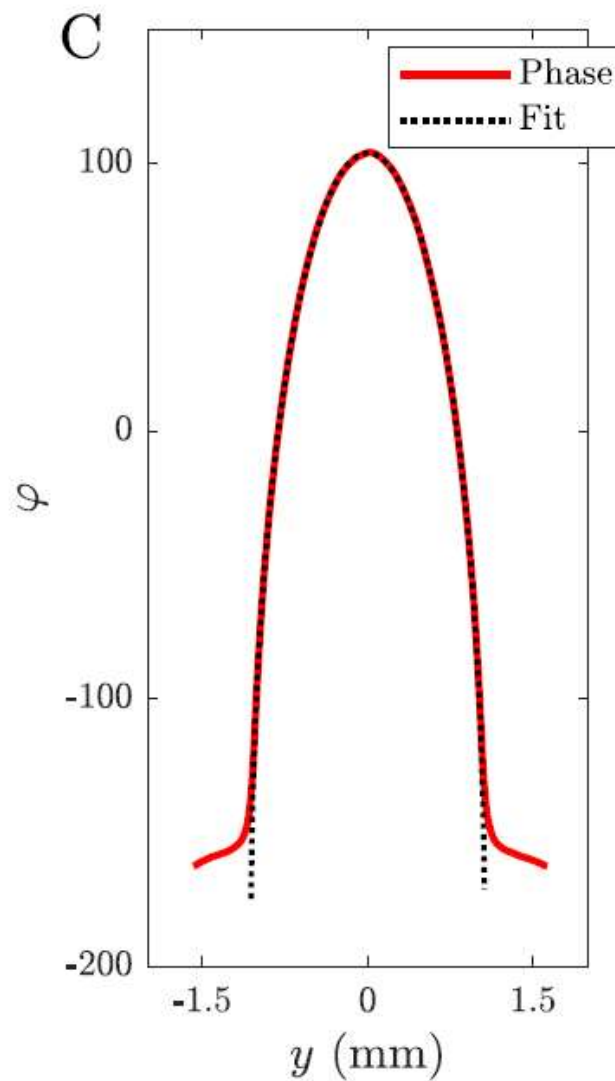
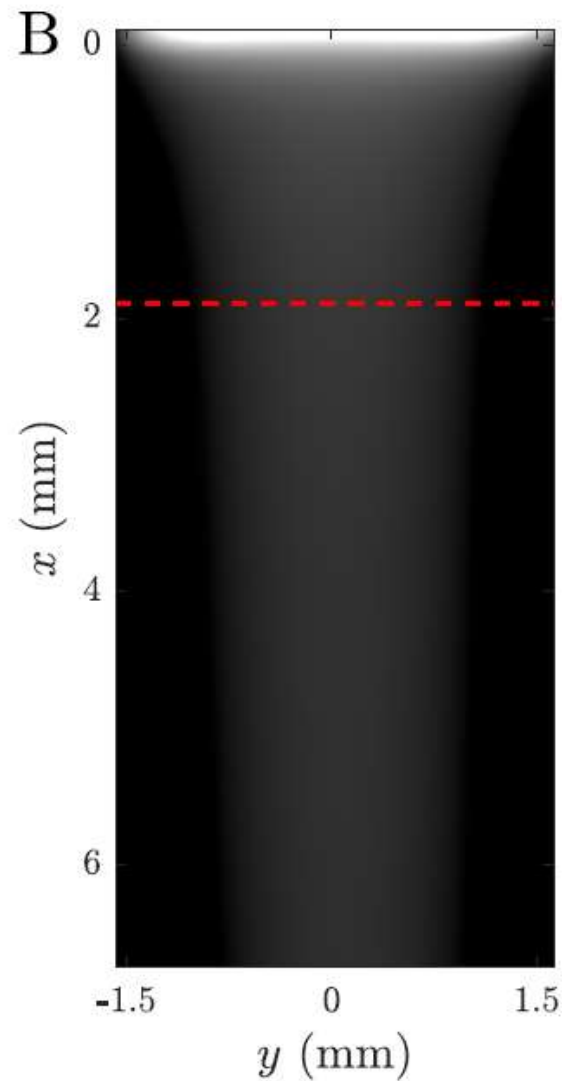
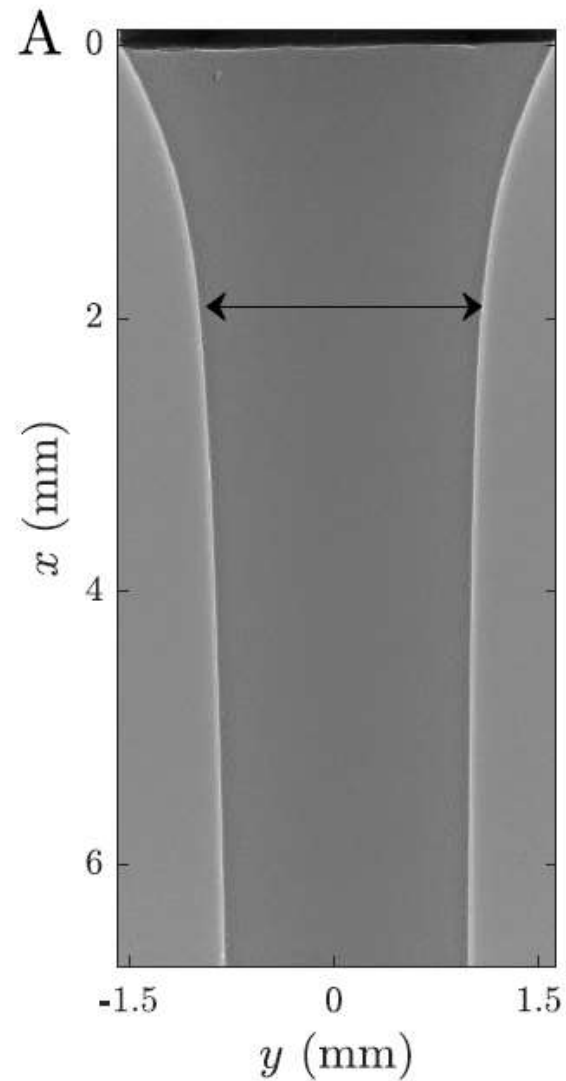
Weitkamp et al.  
*J. of Synchrotron Radiation* 2011



Normalized radiograph  
Phase map  
EPL

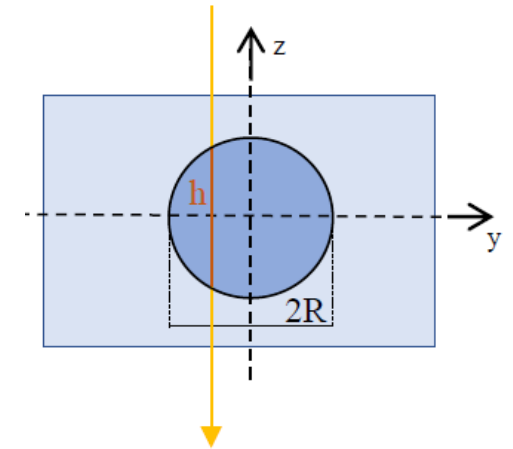
X-ray absorption by the liquid jet follows Beer-Lambert's law

➔ Equivalent path length (EPL)



X-ray absorption by the liquid jet follows Beer-Lambert's law

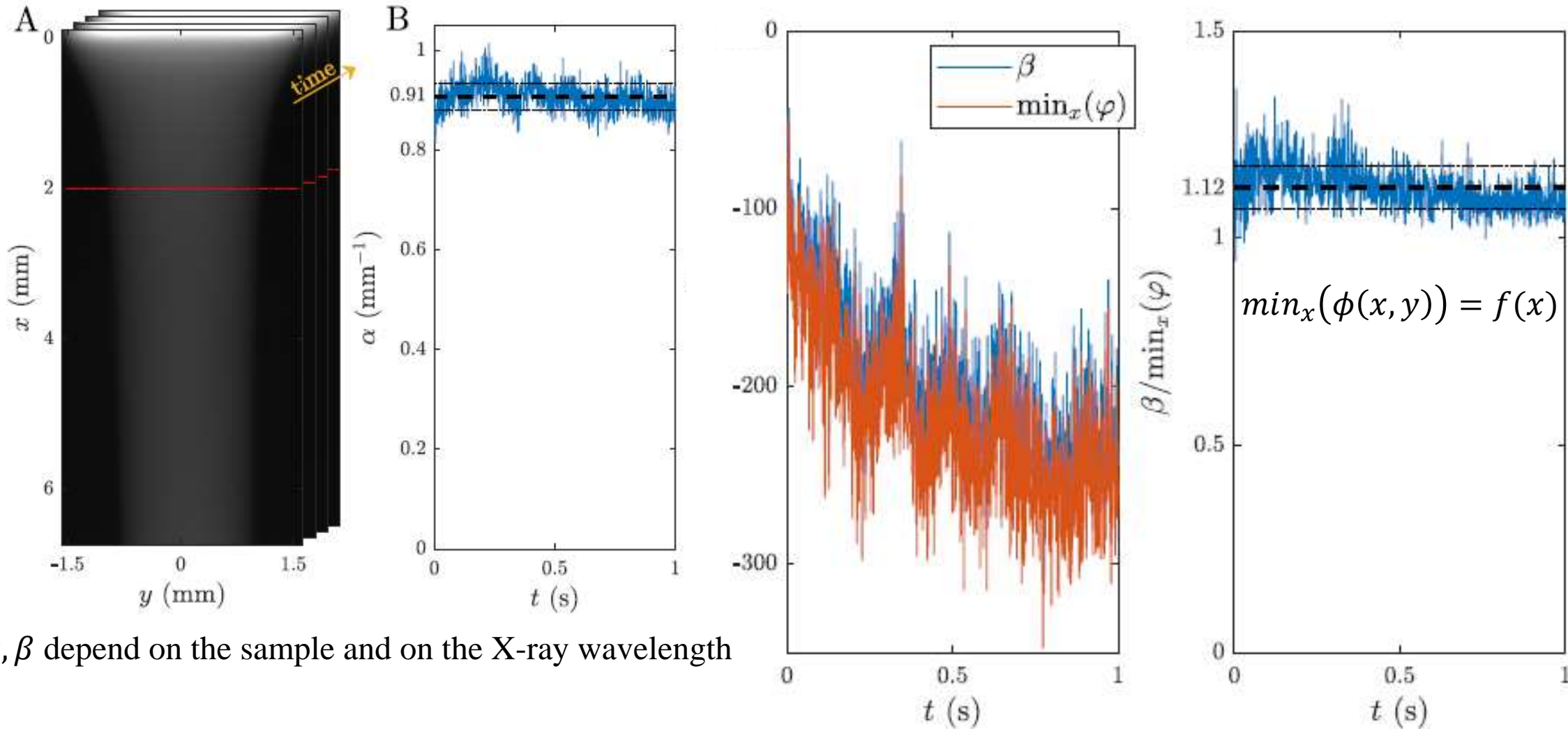
→ Equivalent path length (EPL)



$$\phi = \alpha h(y) + \beta$$

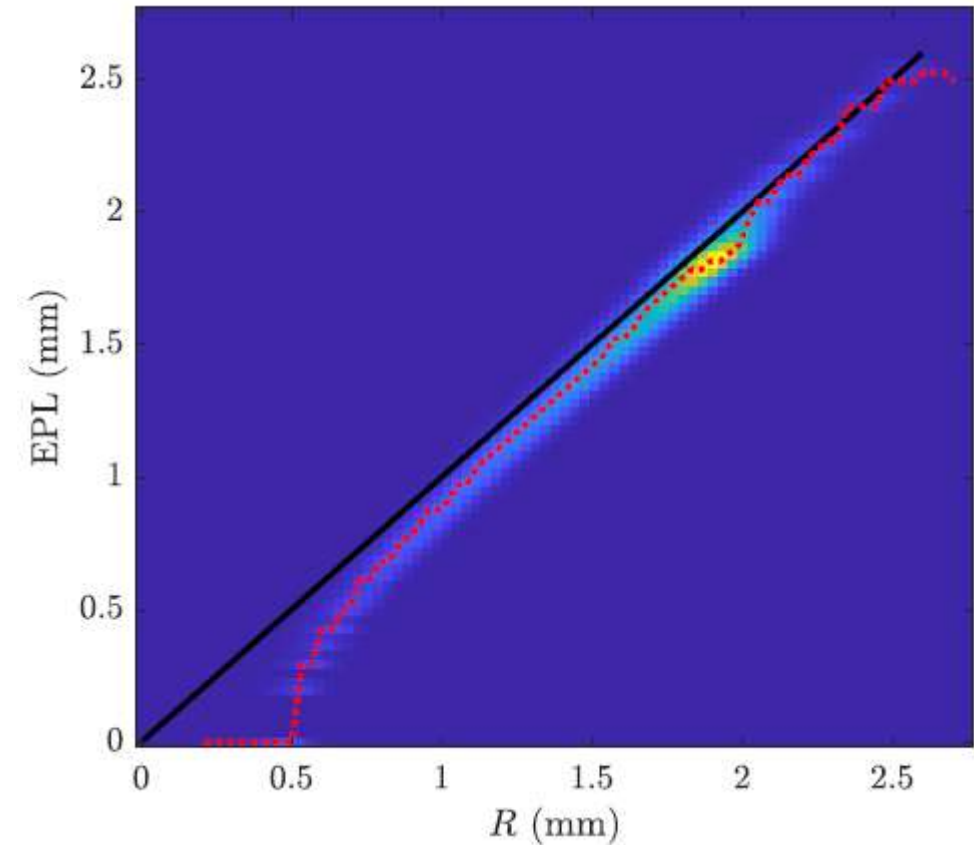
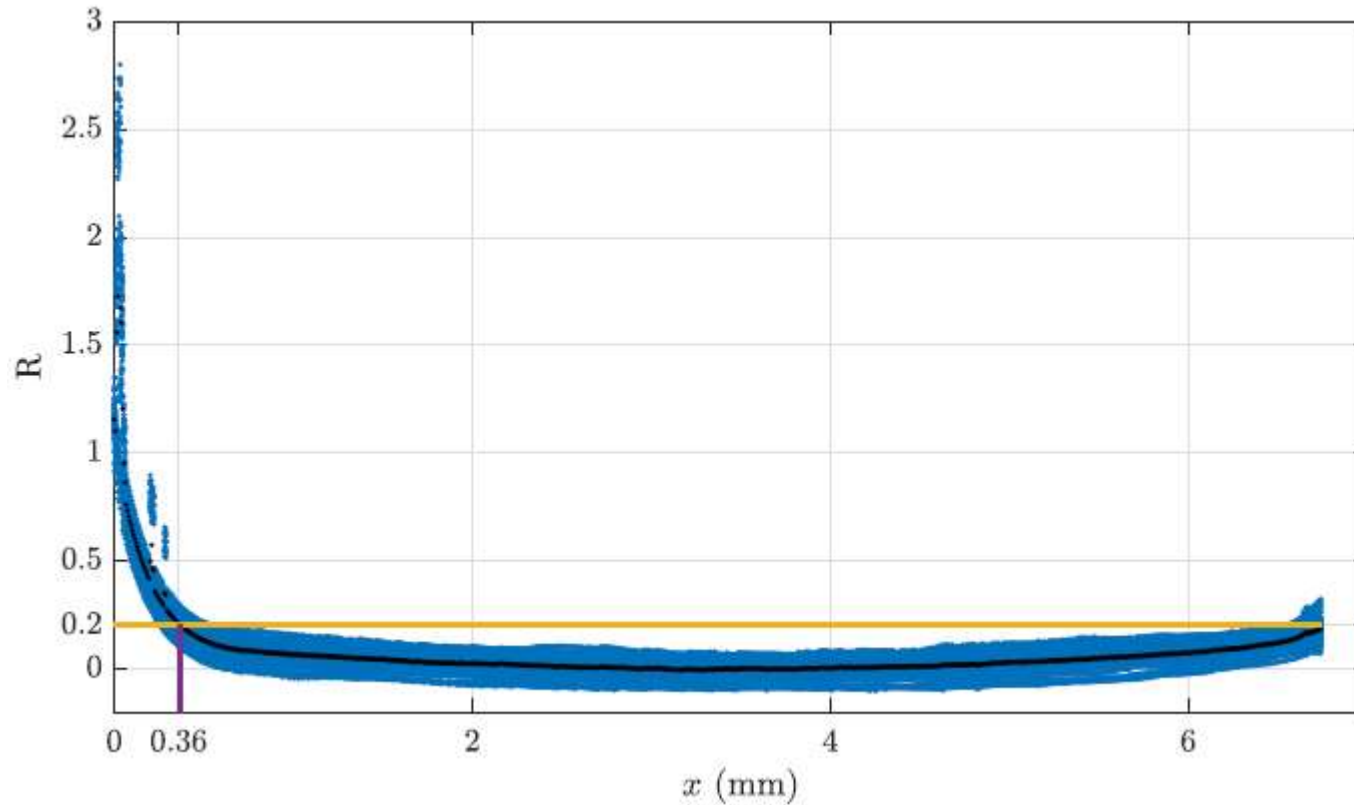
$$h(y) = 2R \sqrt{1 - (y/R)^2}$$

→ Calibrate for the coefficient  $\alpha$  and  $\beta$  (non-monochromatic, spatial and temporal inhomogeneities...)



$\alpha, \beta$  depend on the sample and on the X-ray wavelength

→  $\alpha = 0.91 \text{ mm}^{-1}$  and  $\beta = 1.12 \min_x(\phi)$  for what follows



Longitudinal cut along the liquid jet

2D PDF: EPL vs fitted radii

## Limitations of the uncertainties' evaluation

- Nozzle glare (ANKA Phase is for a single material)
  - Interference patterns due to X-ray scattering by interfaces limit the probing of small radius values
- ➔ For  $x > \frac{D_l}{10}$  and for  $EPL > 1$  mm, approximately 10% accuracy (~ 20% for smaller thicknesses?)



