

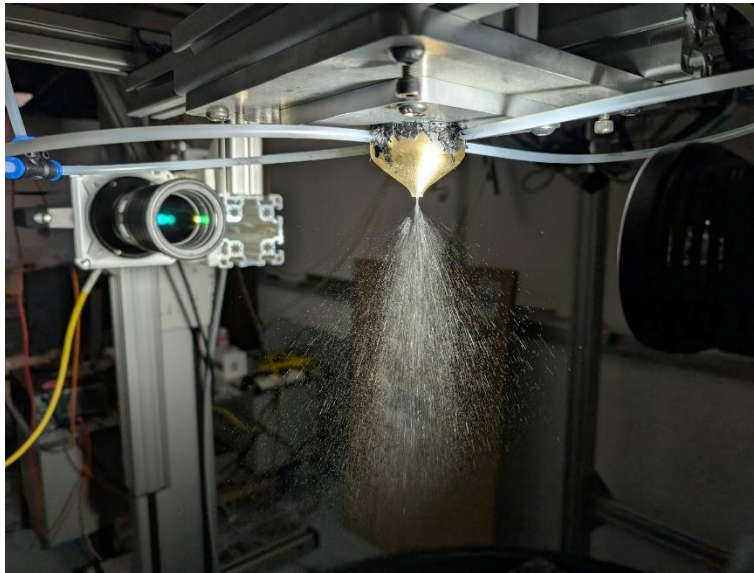
Scale effect in coaxial two-fluid atomization

Corentin Bourjaillat^(1,2), Mathieu Gibert⁽¹⁾, Nathanaël Machicoane⁽²⁾, Jean-Philippe Matas⁽³⁾

(1) Univ. Grenoble Alpes, CNRS, Institut Néel, Grenoble Cedex 9 38042, France

(2) Univ. Grenoble Alpes, CNRS, Grenoble INP, LEGI, 38000 Grenoble, France

(3) Université Claude Bernard Lyon 1, LMFA, Villeurbanne, France



GdR TransInter June 10th 2025

Atomization



Fuel mixing



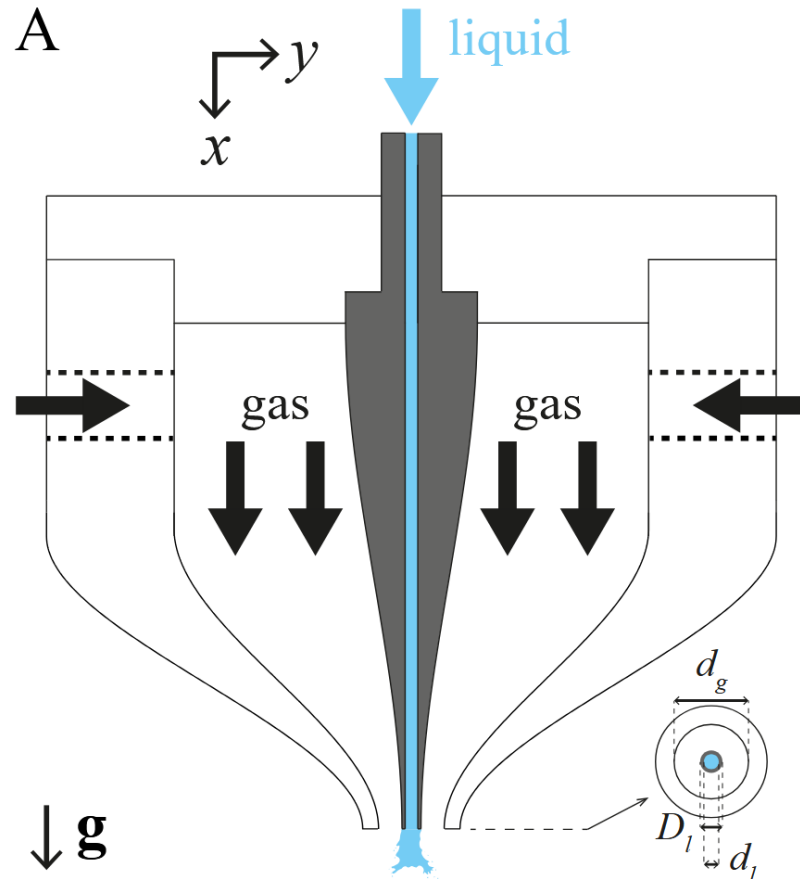
Industrial coating



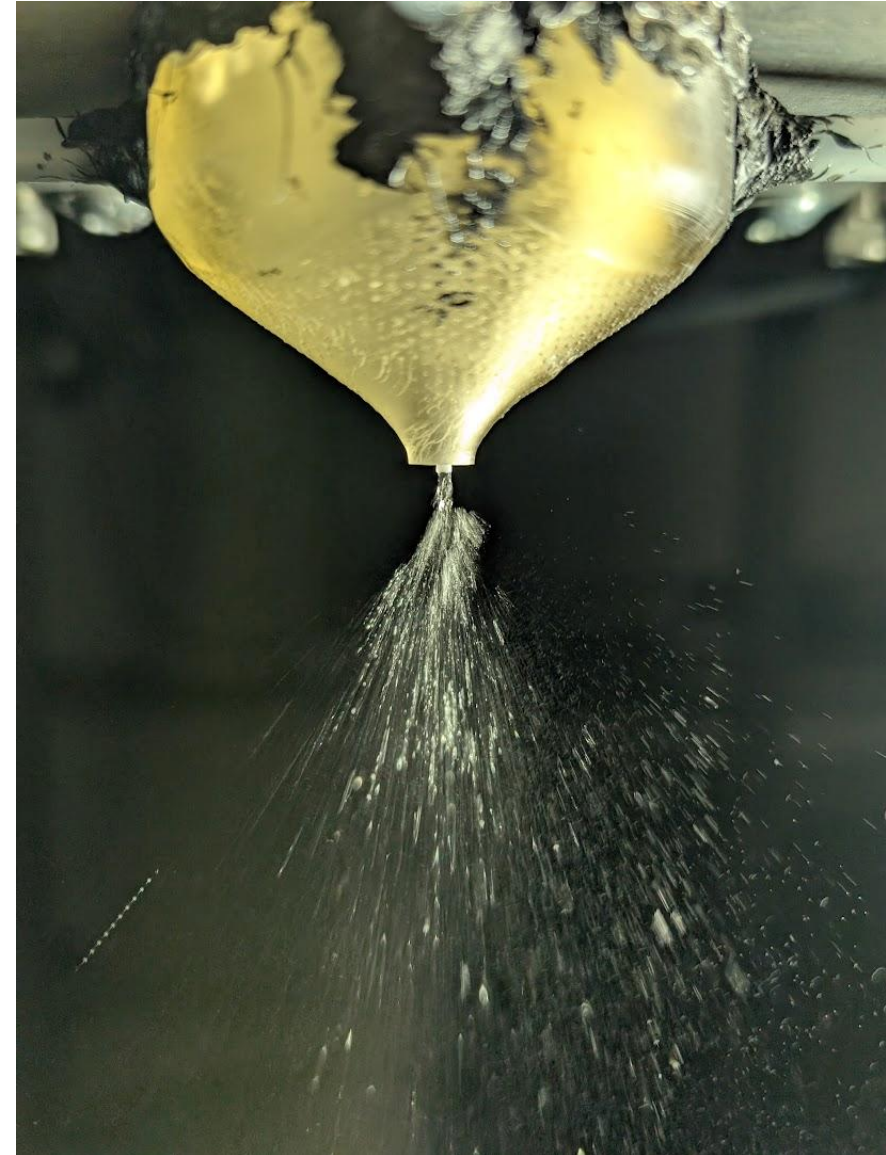
Oceanic spray

<https://www.spray.com/enau/applications/coating>
<https://www.lsxmag.com/tech-stories/fuel-cooling-ignition-tech/taking-the-guesswork-out-with-fuel-injector-clinic/>
<https://cpo.noaa.gov/uncovering-the-links-between-surfactants-sea-spray-and-tropical-cyclone-intensification/>

Atomization

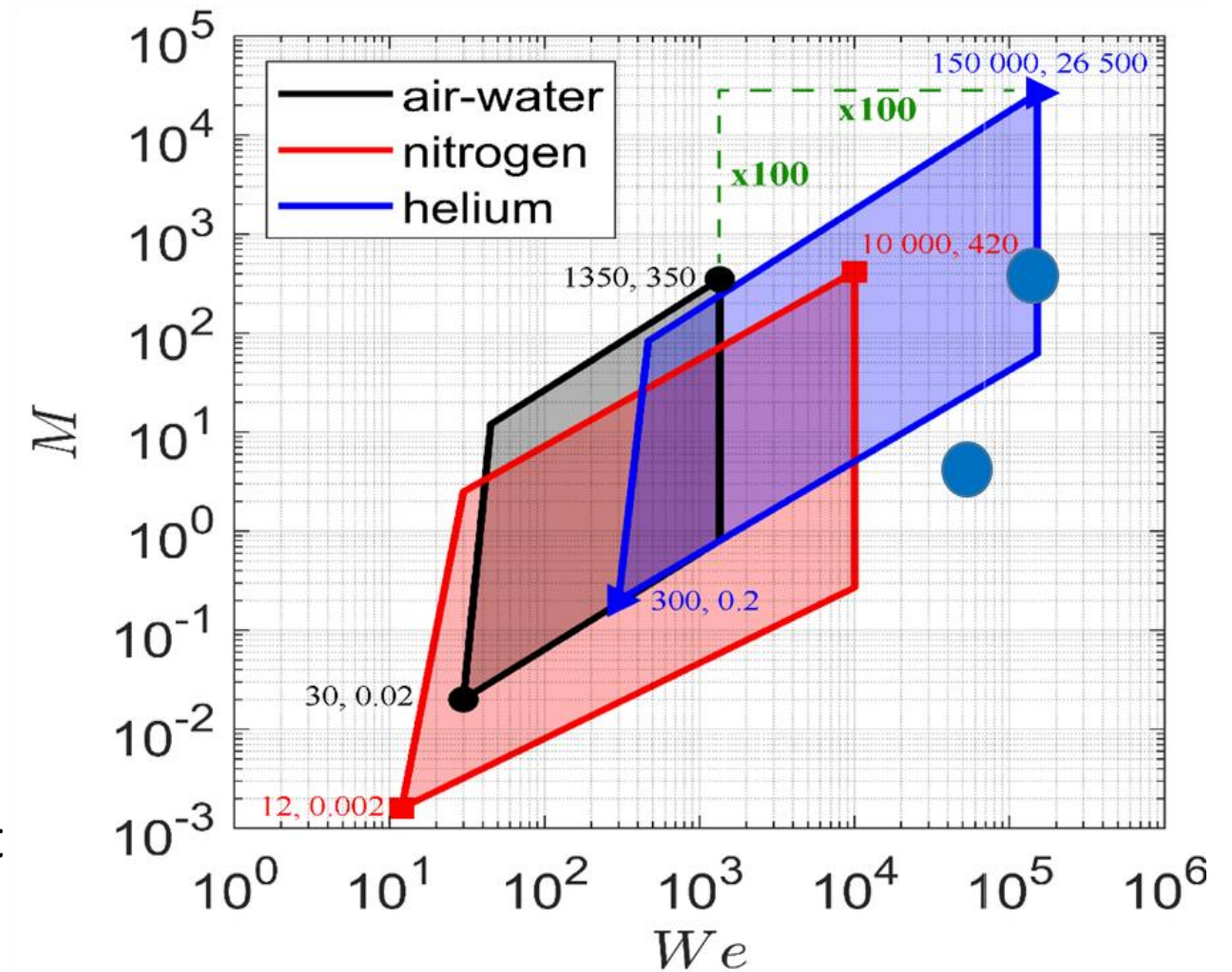


Coaxial two-fluid atomizer



Motivations

- ANR Cryospray
- Scale down needed
- Implementation in LN_2 and LHe cryostat



Will the downscaling of the nozzle impact the atomization mechanisms ?

Motivations

- Collaboration with J-P Matas

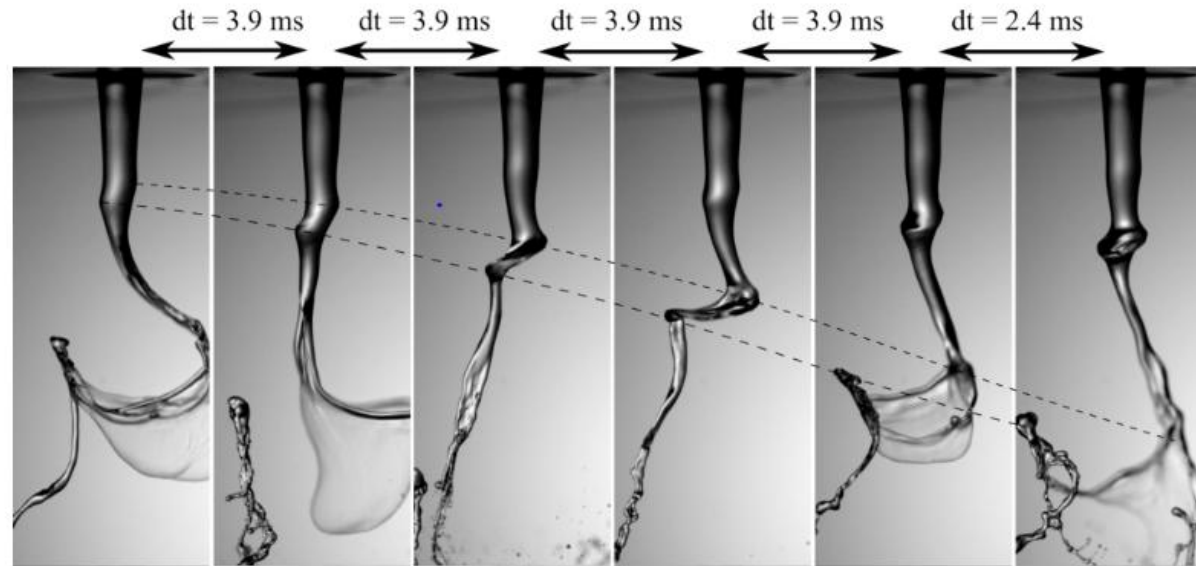
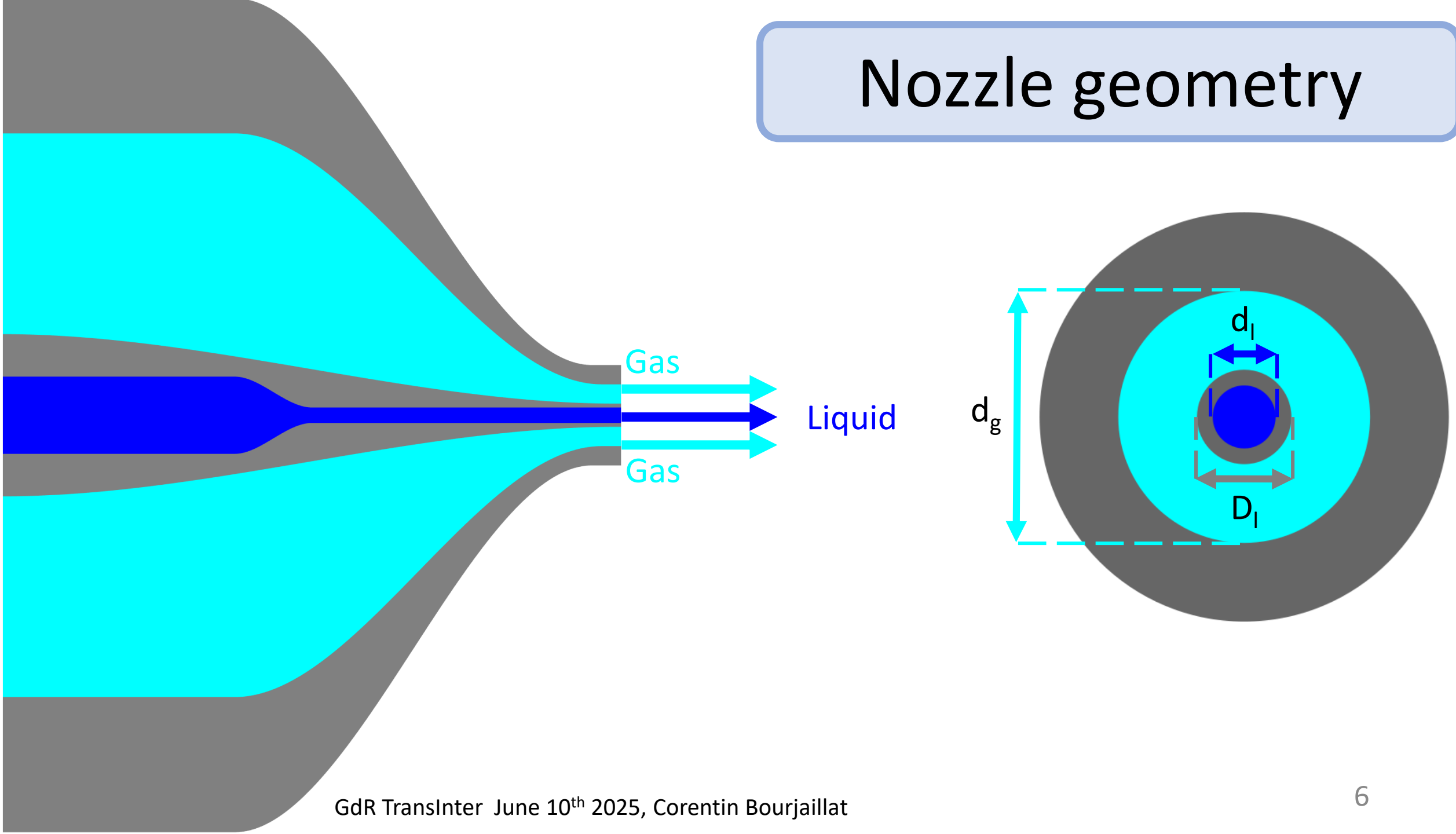


FIG. 11. Time evolution of an oblique shear instability wave, for $H_L = 5$ mm, $H_G = 5$ mm, $U_L = 0.28$ m/s, and $U_G = 22$ m/s.

Which scales govern the instabilities ?

Nozzle geometry



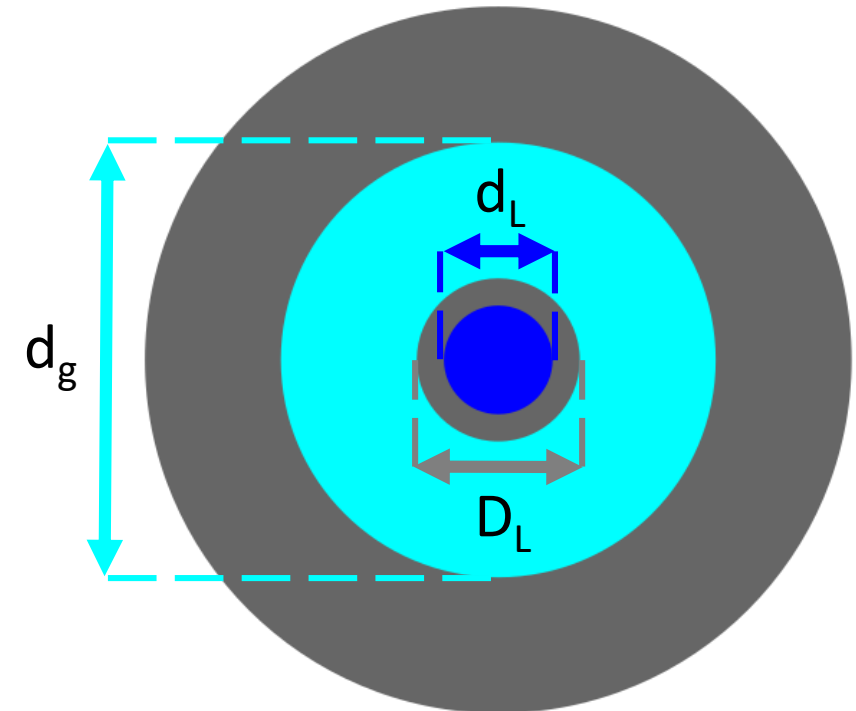
Nozzle geometry

ALUMINUM NOZZLE

Nozzle	d_i [mm]	D_i [mm]	d_g [mm]
N_{1,V_0}	2	3	10
N_{1,V_1}	2	2,5	8
$N_{1/2,V_1}$	1	1,5	4

NEW, 3D PRINTED NOZZLES

$N_{1/2,V_1}$: “ $\frac{1}{2}$ scale nozzle, version 1”



~30 cm

3D Printed by
Tristan Vandenberghe
@LEGI

Nozzles



2.5× scale



1× scale

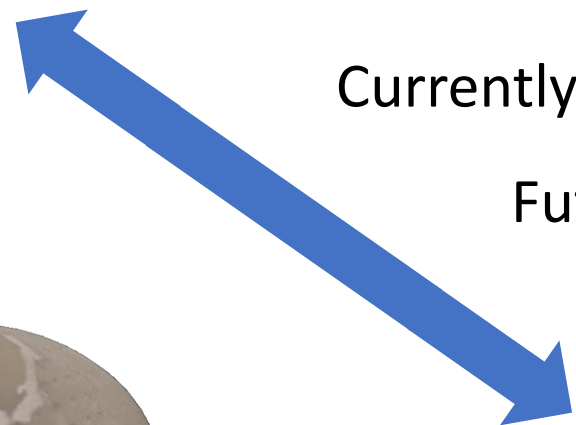


$\frac{1}{2}$ × scale



$\frac{1}{4}$ × scale

~3 cm



Currently : 2× scaling

Future : full decade range ?

Parameters

- Weber number : $We = \frac{\rho u_G^2 d_l}{\sigma} = \frac{\text{Inertia}}{\text{Surface tension}}$
- Dynamic gas-to-liquid pressure ratio : $M = \frac{\rho_G u_G^2}{\rho_L u_L^2}$
- Gas Reynolds number : $Re_G = \frac{4Q_G}{v_G \sqrt{4\pi A_G}} = \frac{u_G \sqrt{d_g^2 - D_l^2}}{v_G}$
- Liquid Reynolds number : $Re_L = \frac{4Q_L}{v_L \sqrt{4\pi A_L}} = \frac{u_G d_l}{v_G}$

Back-lit imaging

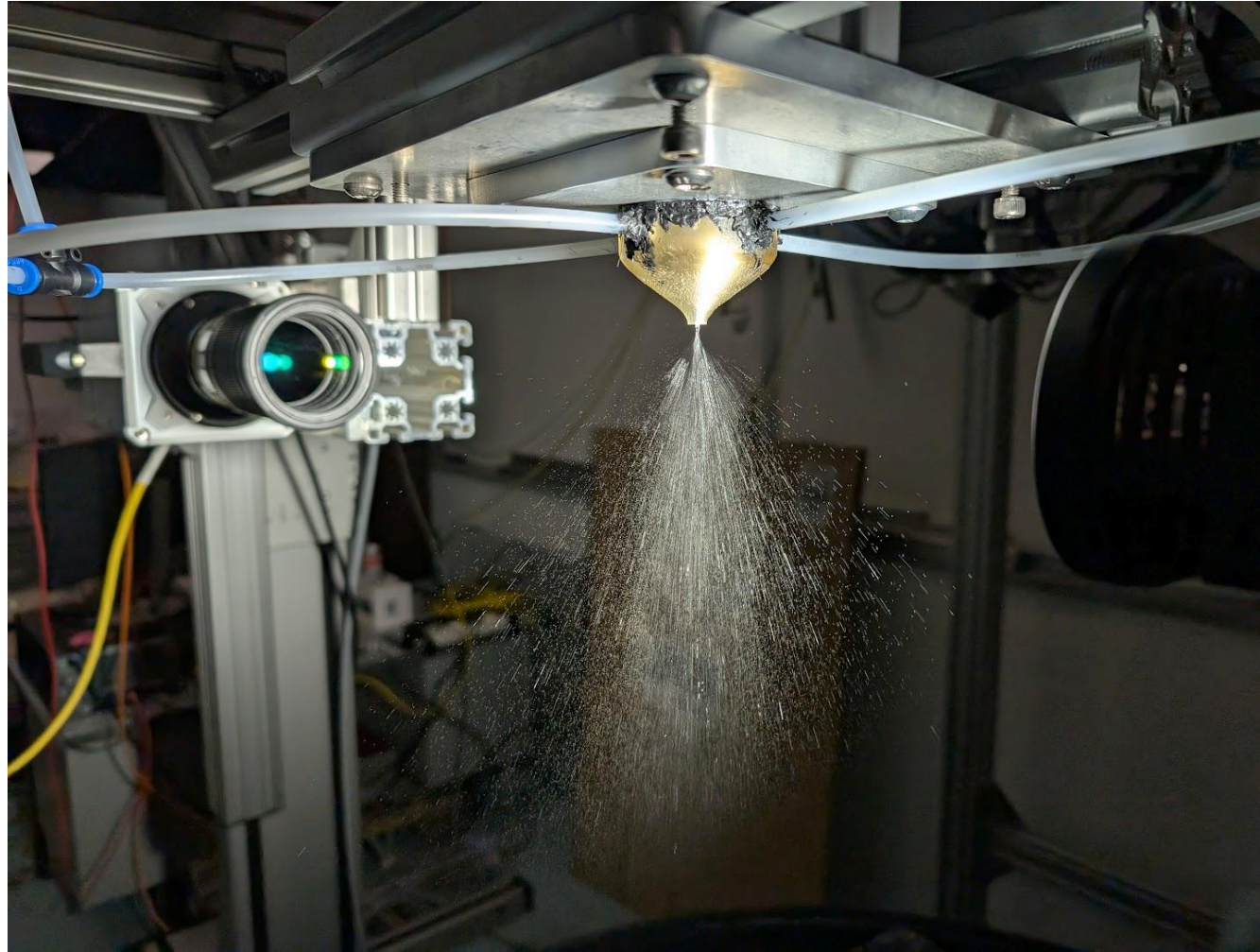


Image processing

- Raw image

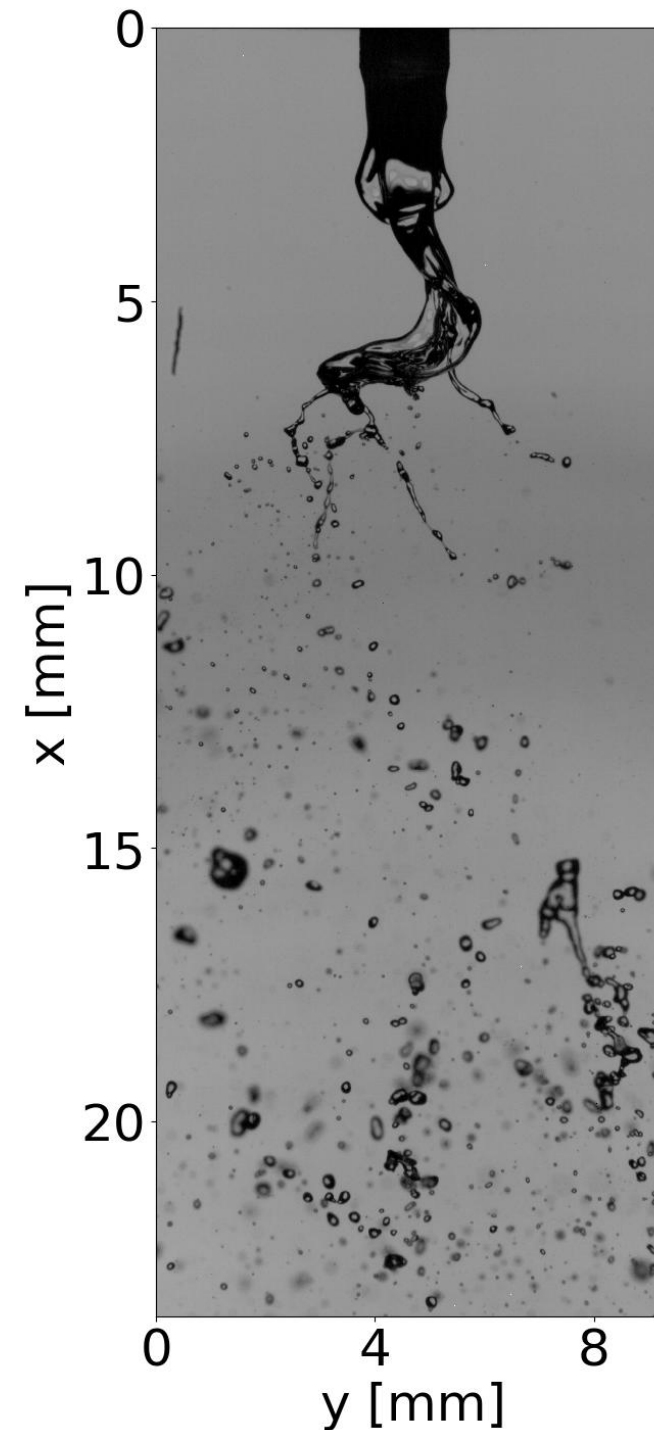


Image processing

- Background removal

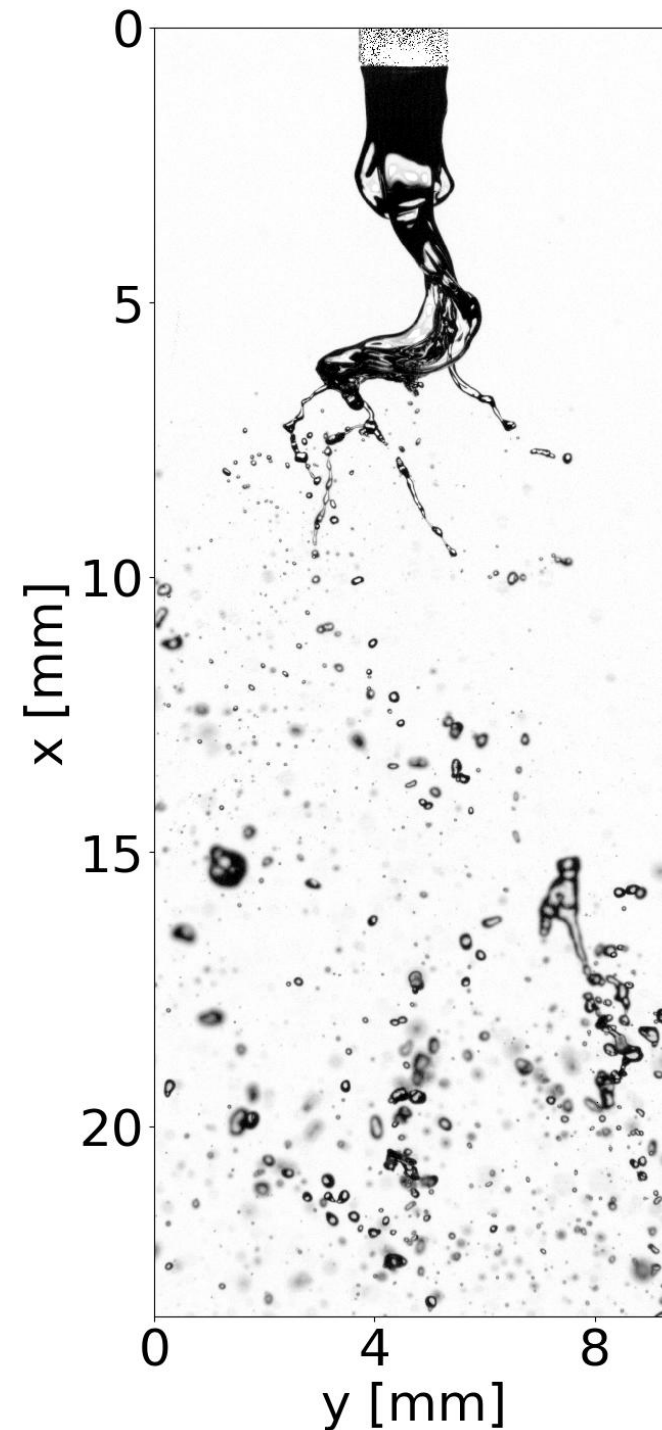


Image processing

- Thresholding

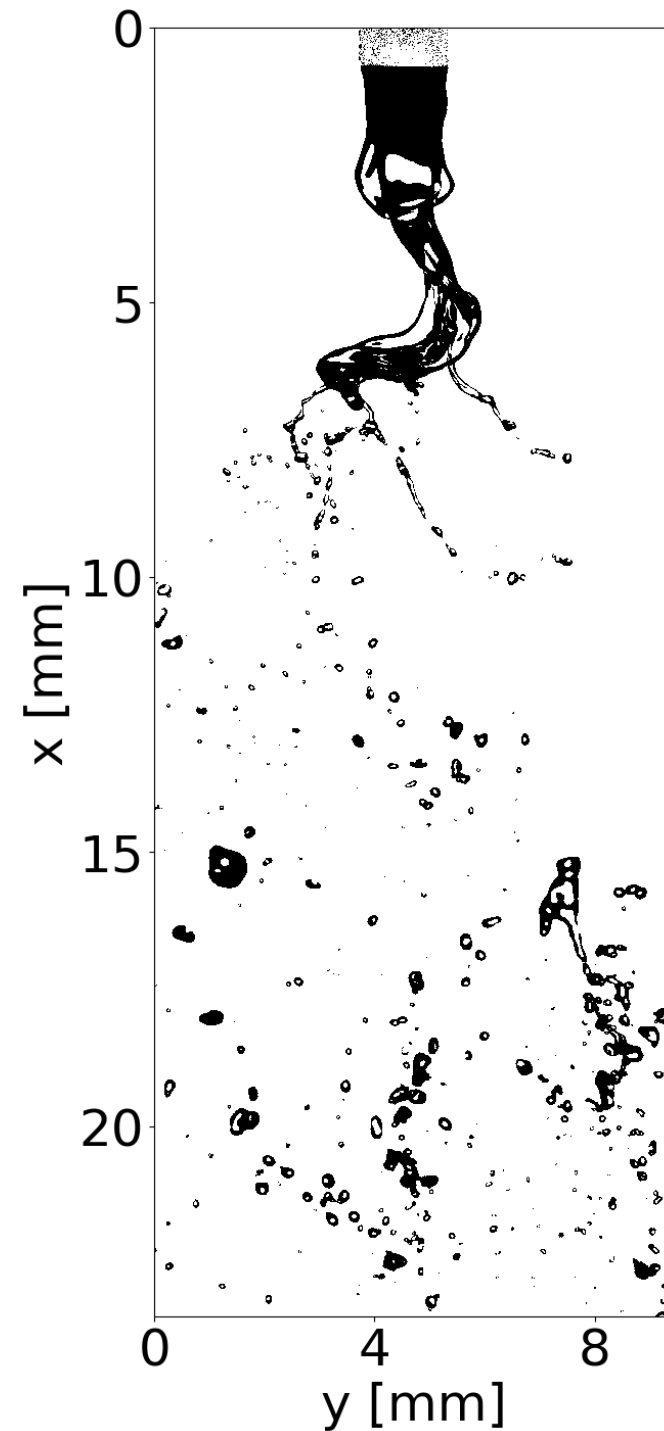


Image processing

- Fill holes

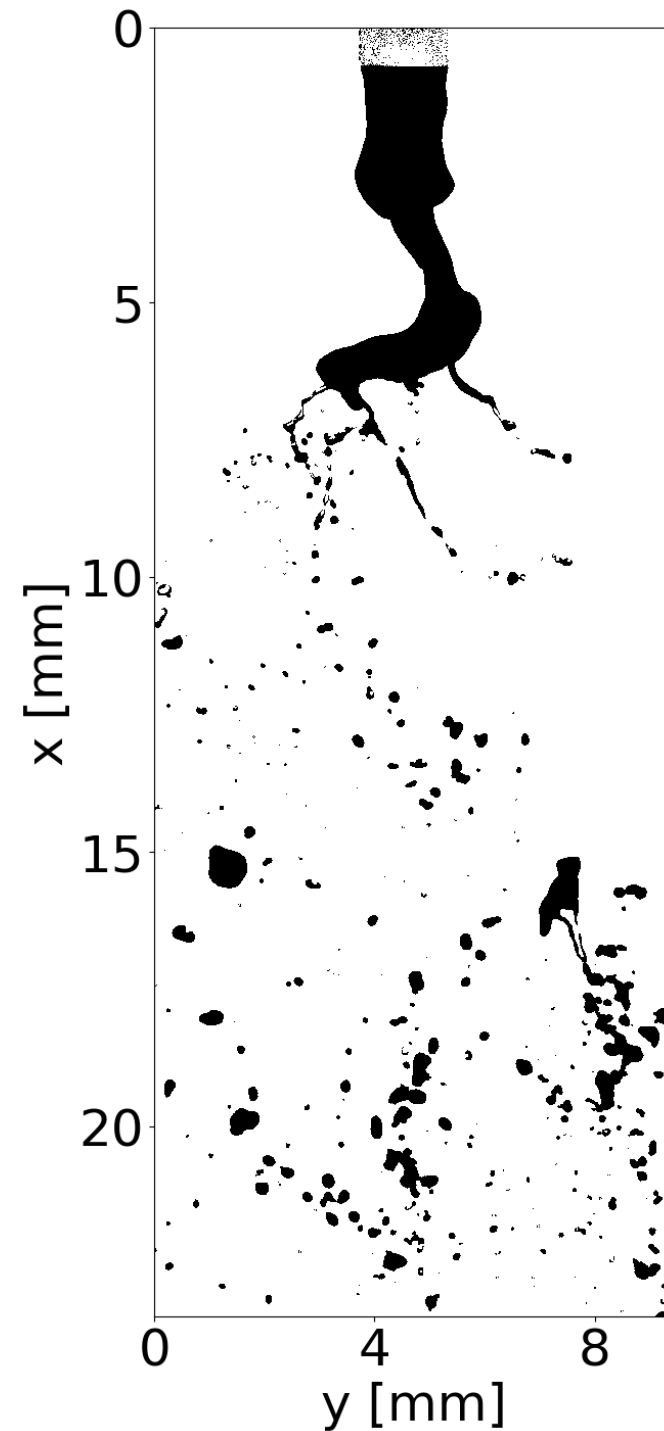


Image processing

- Identify core

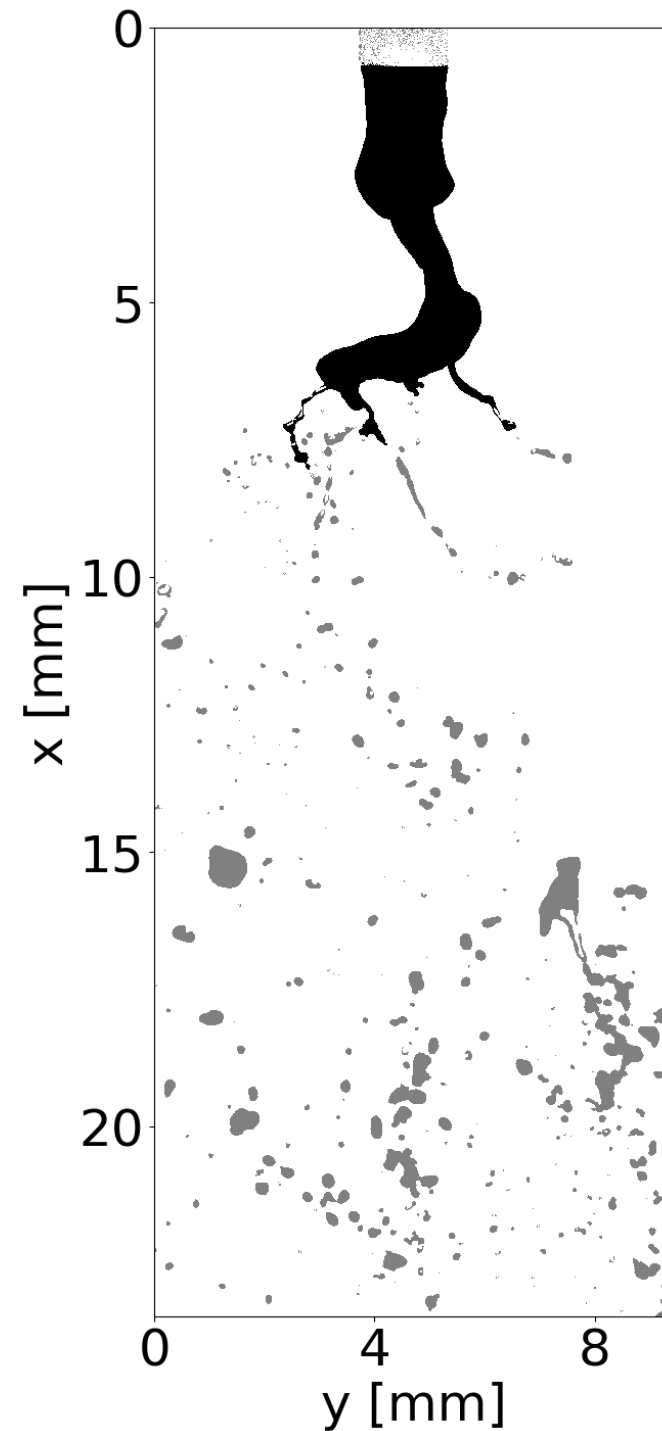


Image processing

- Identify core

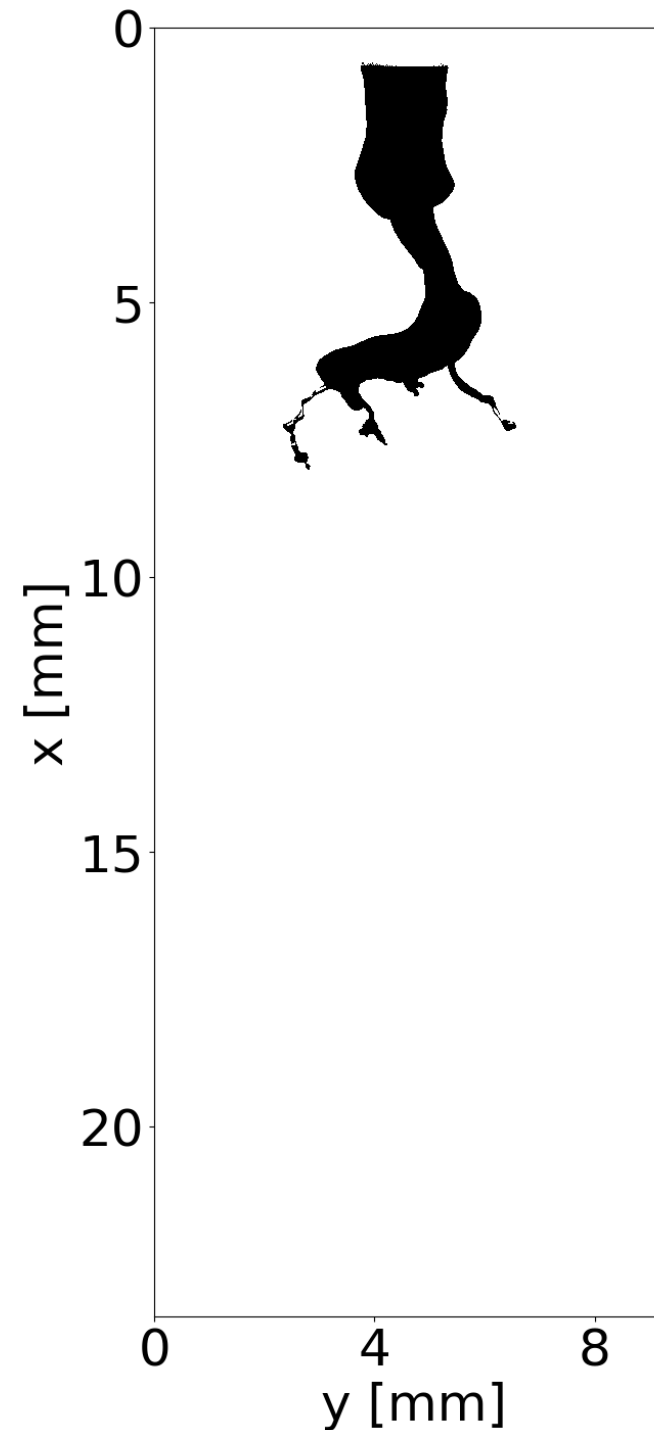
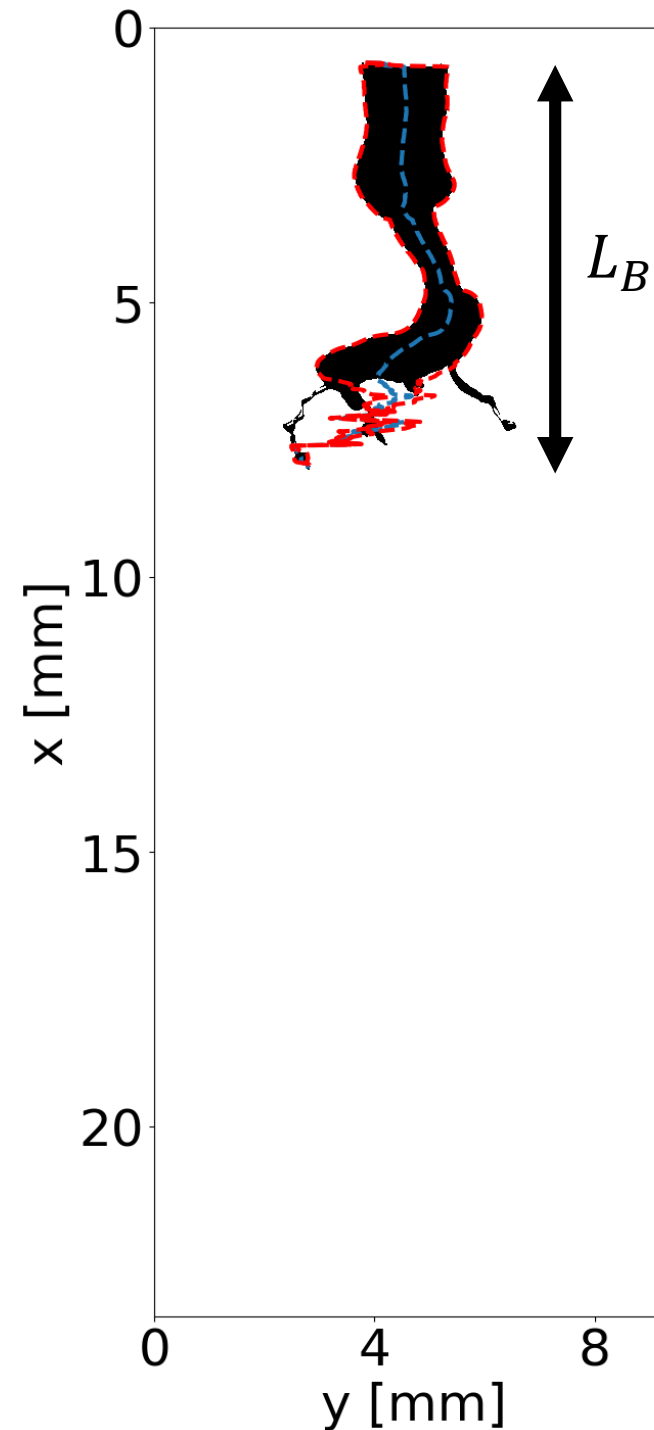


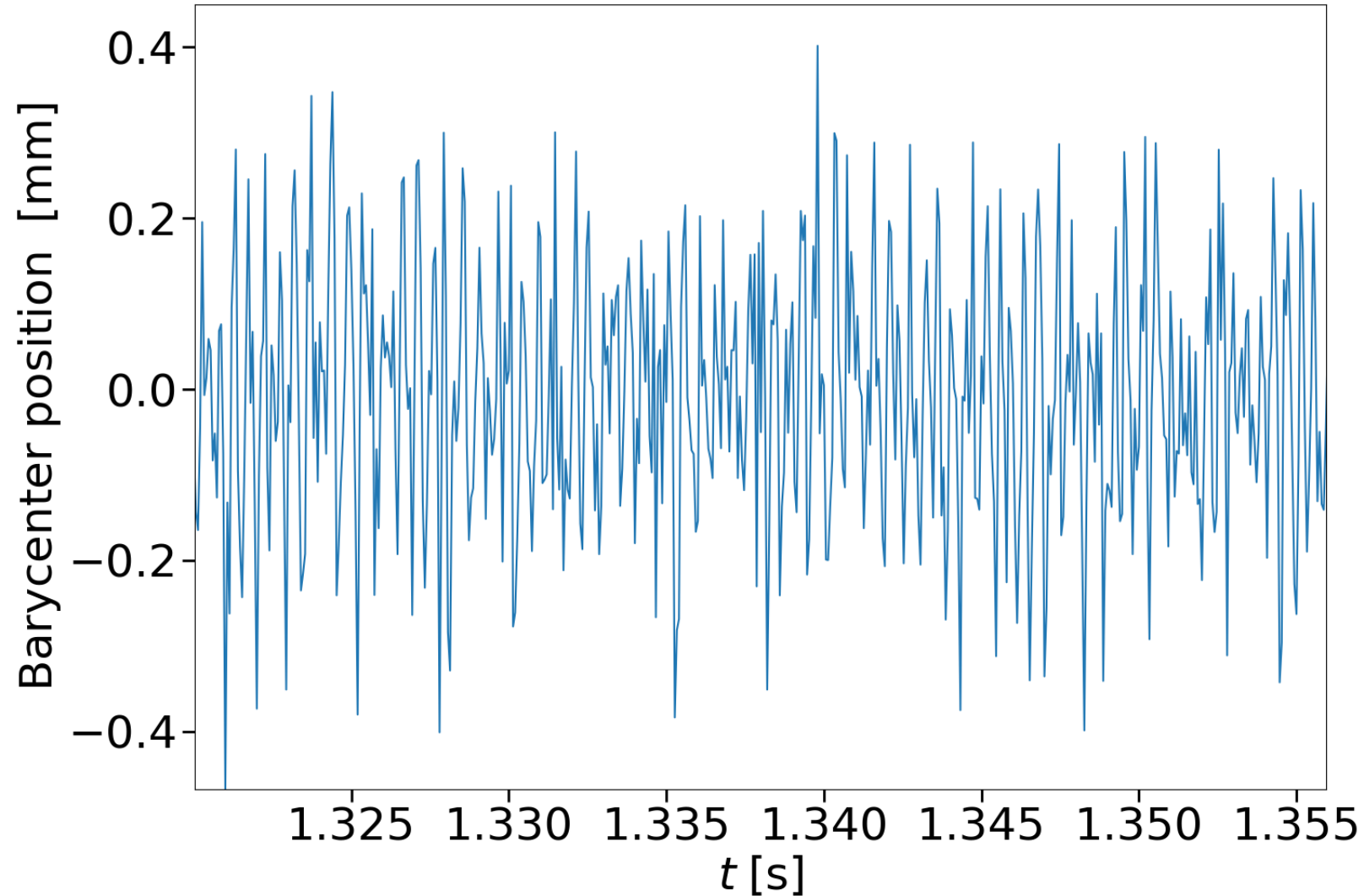
Image processing

Measure :

- Core length : $L_B(t)$
- Barycenter (x, t)
- Width (x, t)



Barycenter dynamics

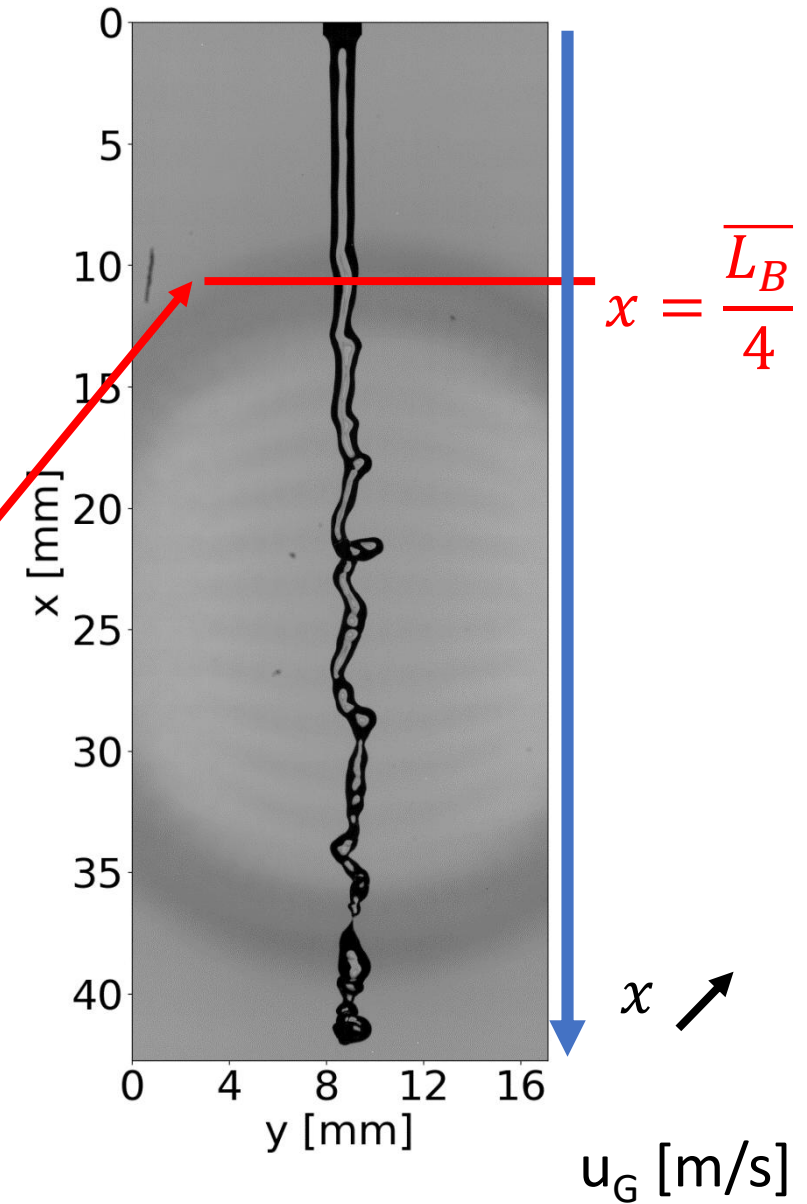
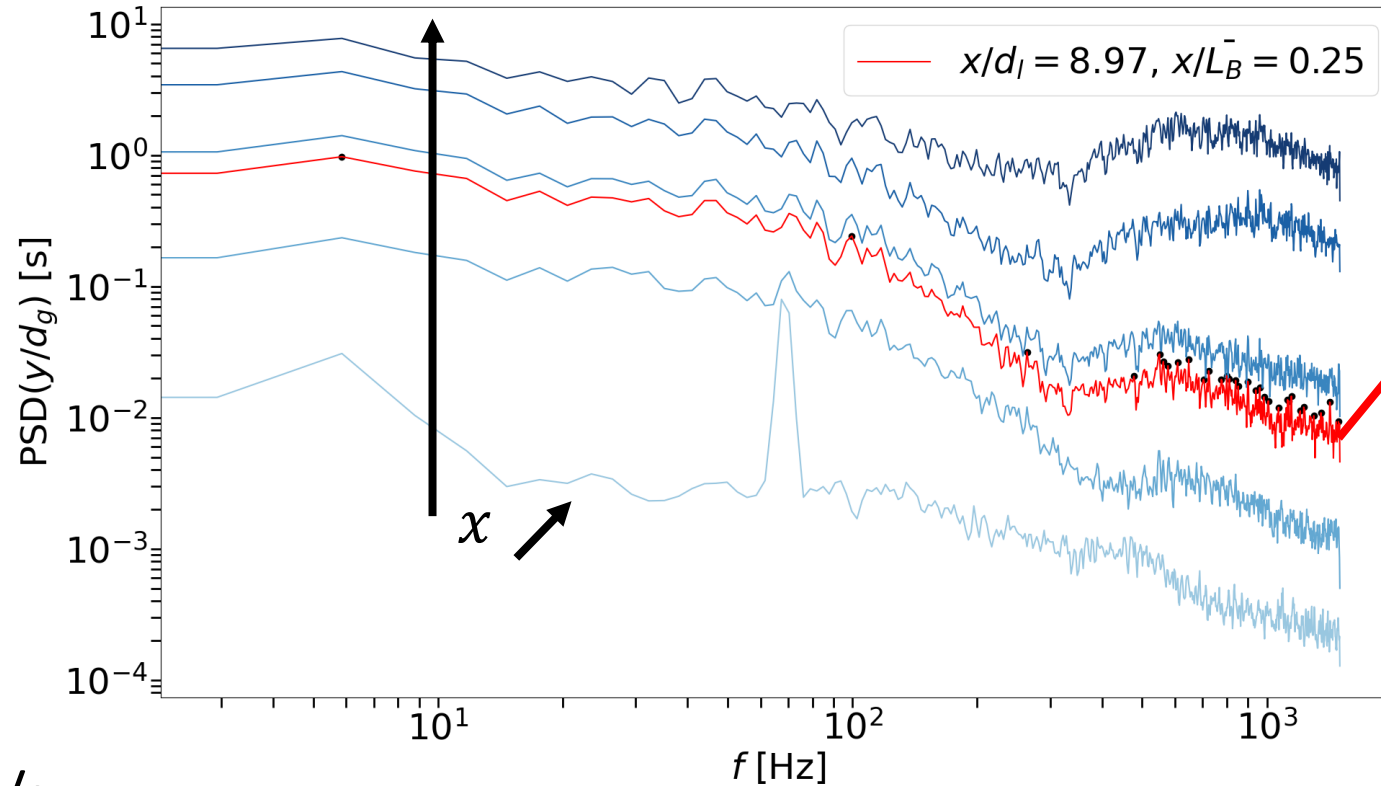


Barycenter time
series at one x
position

Spray Regimes

$$Re_L = 2500$$

Very low u_G : Rayleigh-like breakup, no small drop production



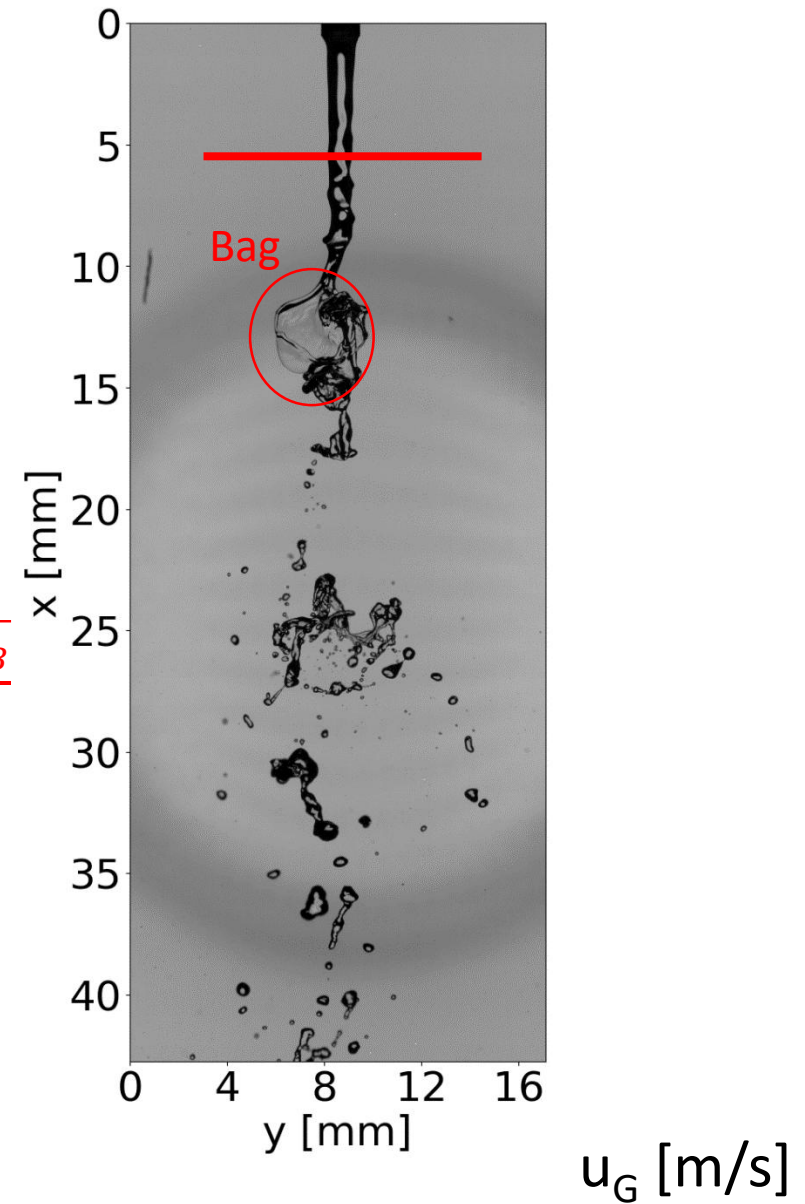
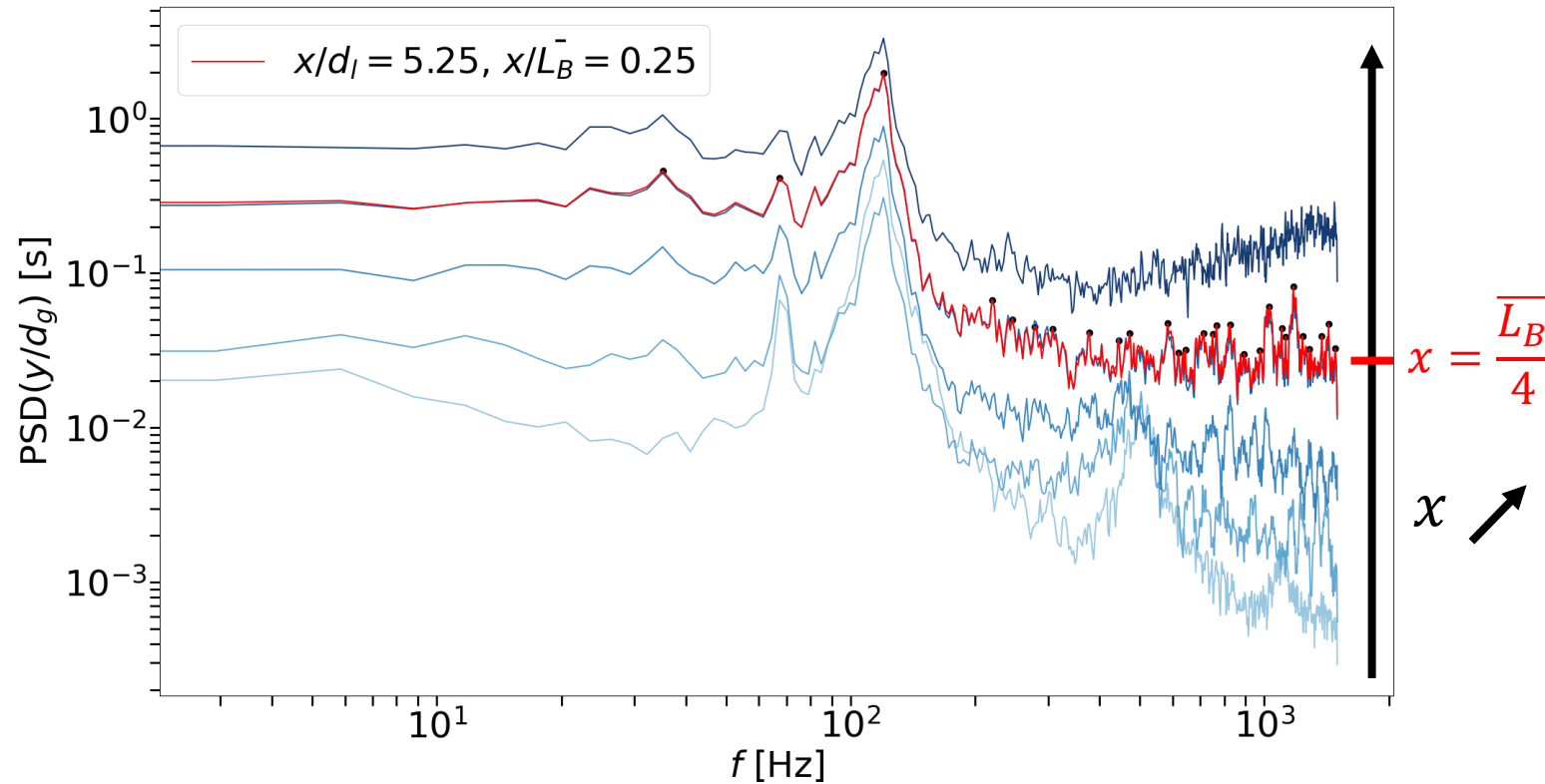
30 m/s

$We = 12$

Spray Regimes

$$Re_L = 2500$$

Low-medium u_G : Bag breakup



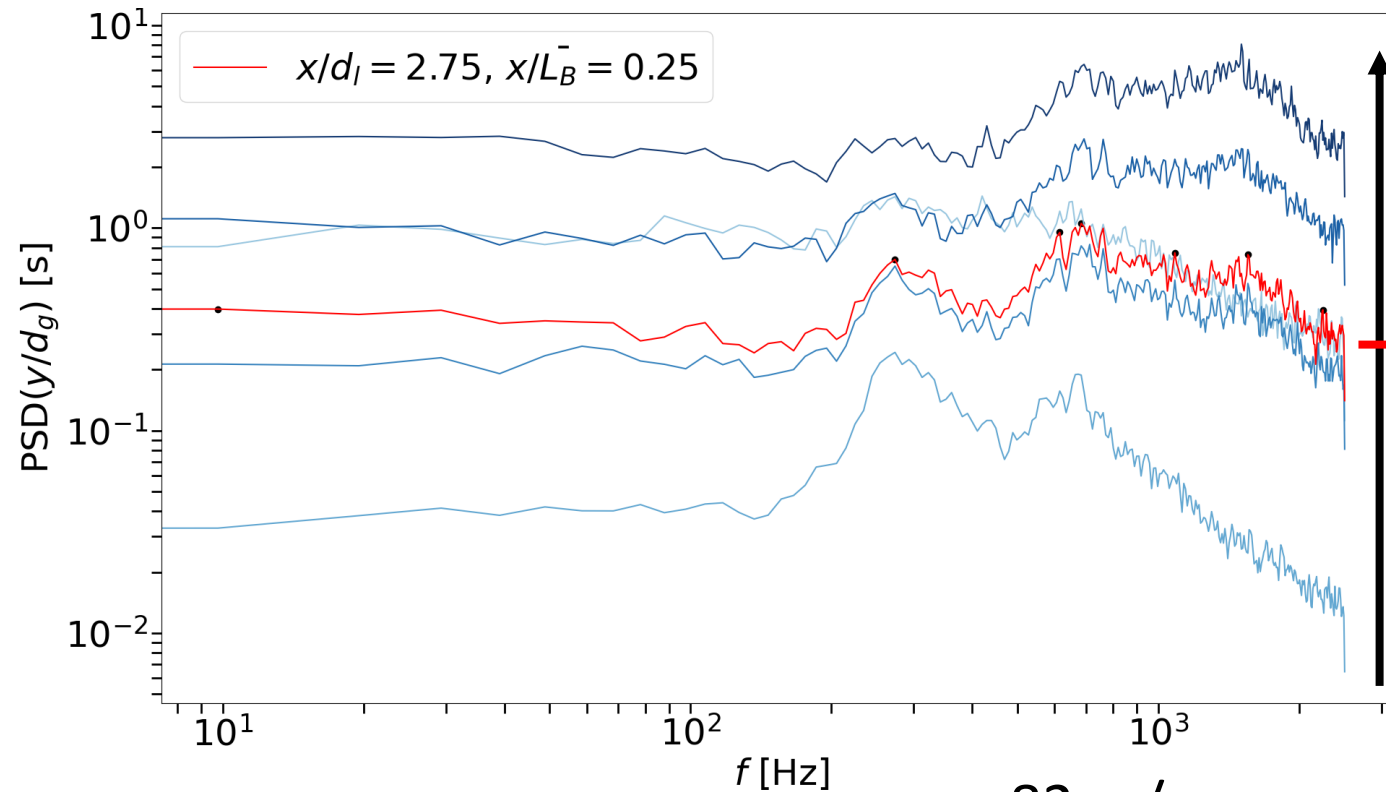
42 m/s

$$We = 23$$

Spray Regimes

$$Re_L = 2500$$

Low-medium u_G : Intermediate regime



82 m/s

$$We = 89$$

Ligament

$$x = \frac{\bar{L}_B}{4}$$

x

x [mm]

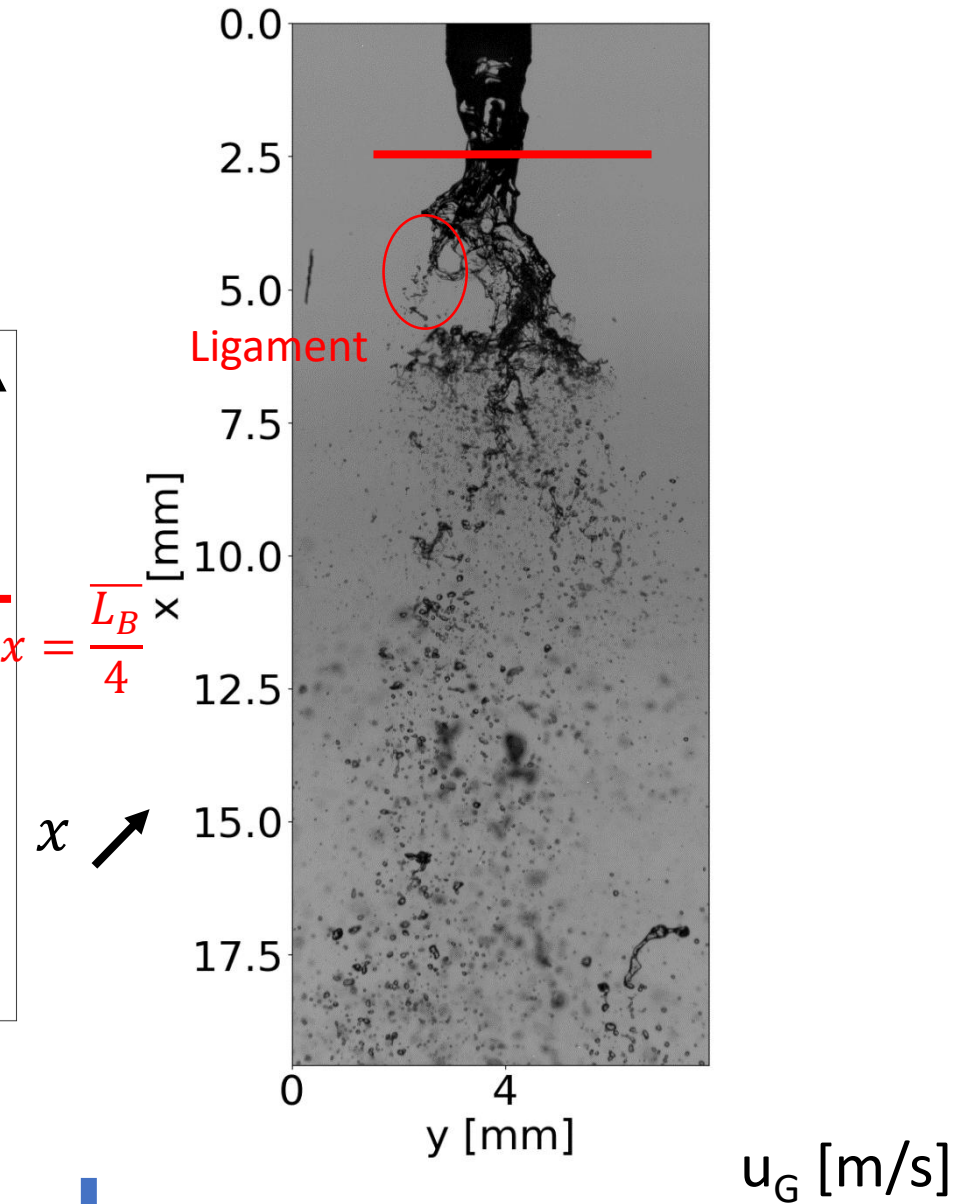
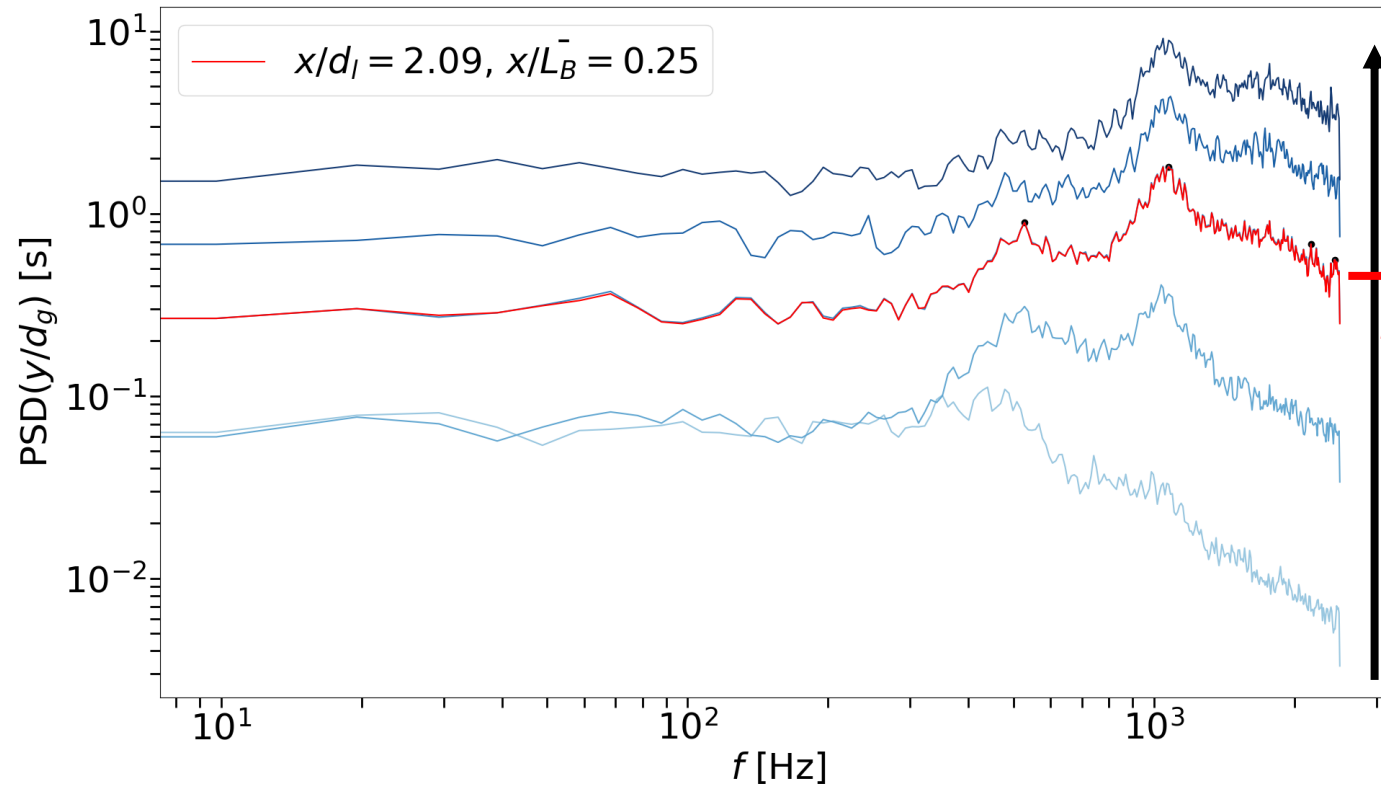
Bag

y [mm]

u_G [m/s]

Spray Regimes

High u_G : Fiber-type atomization

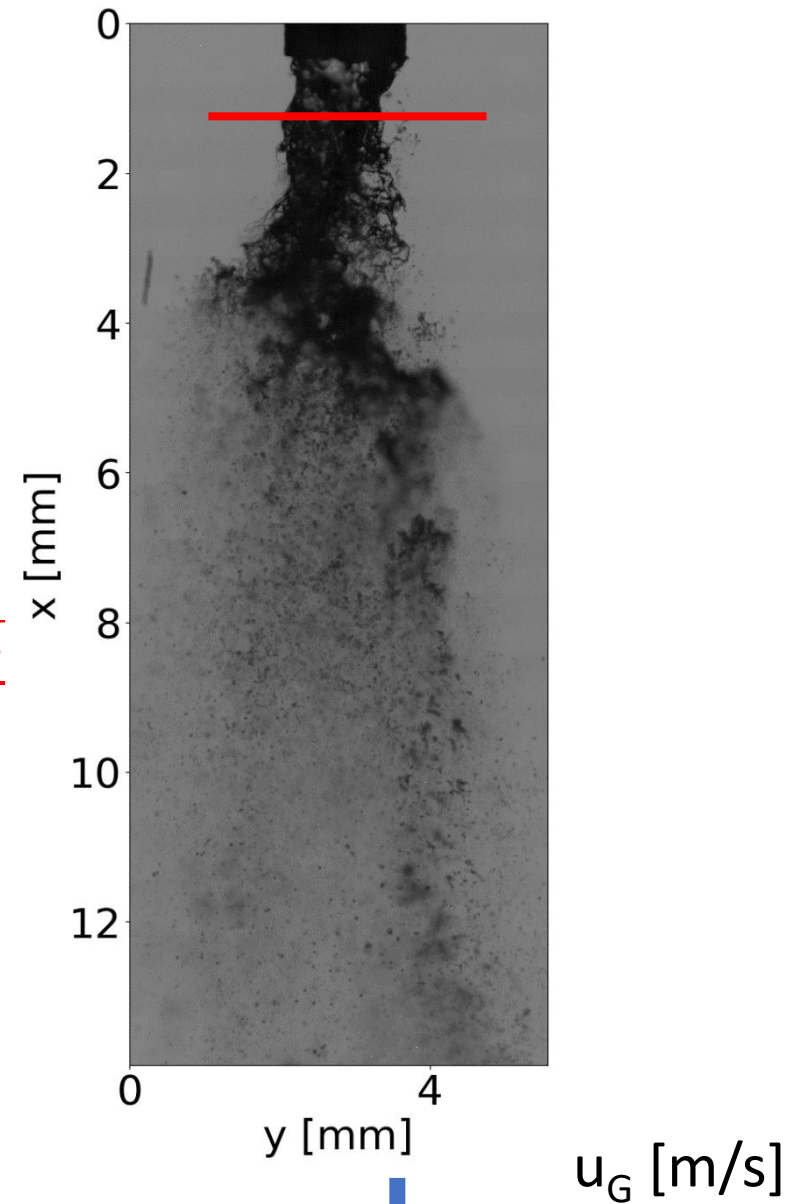
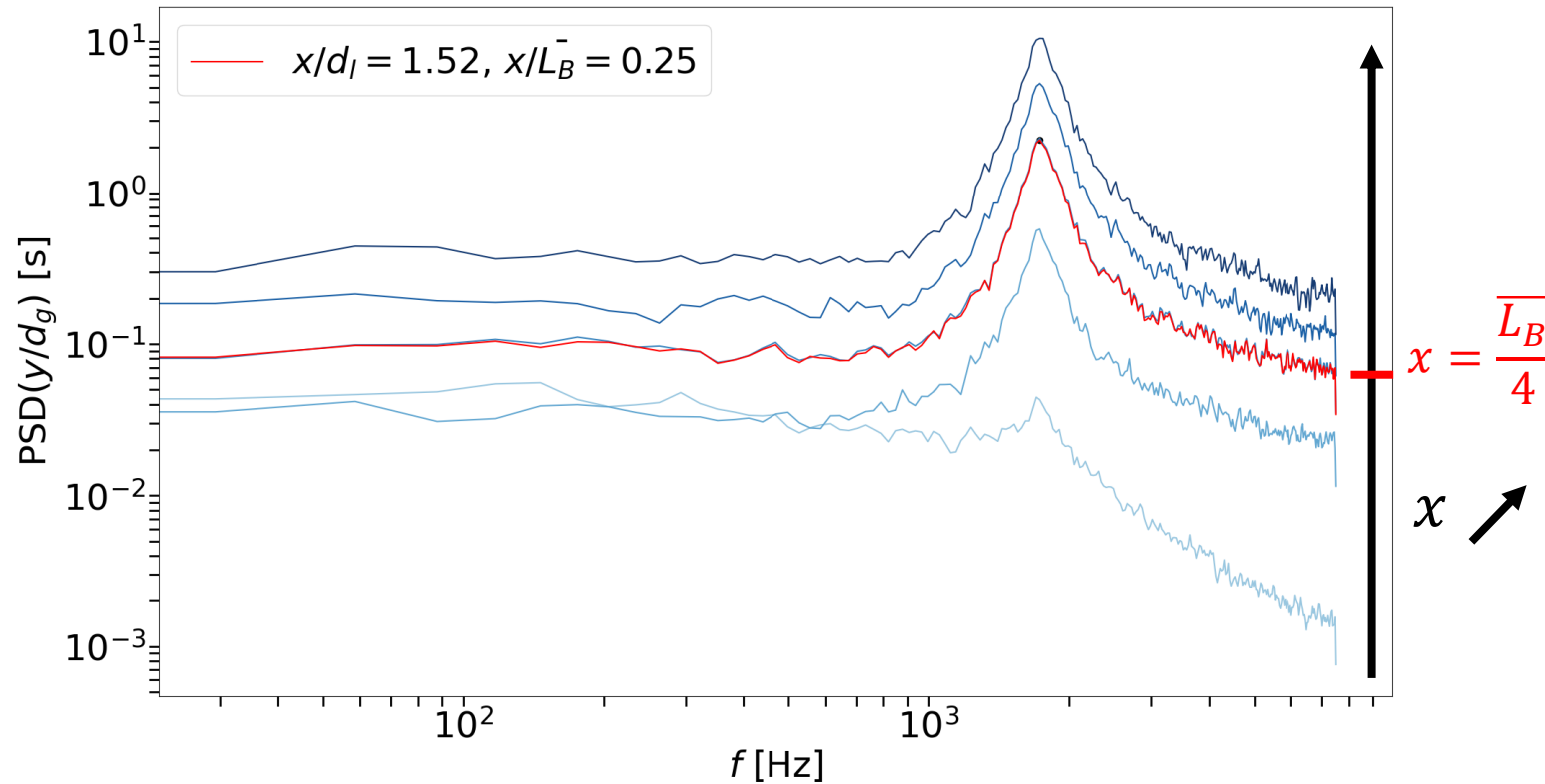


116 m/s, $We = 190$

Spray Regimes

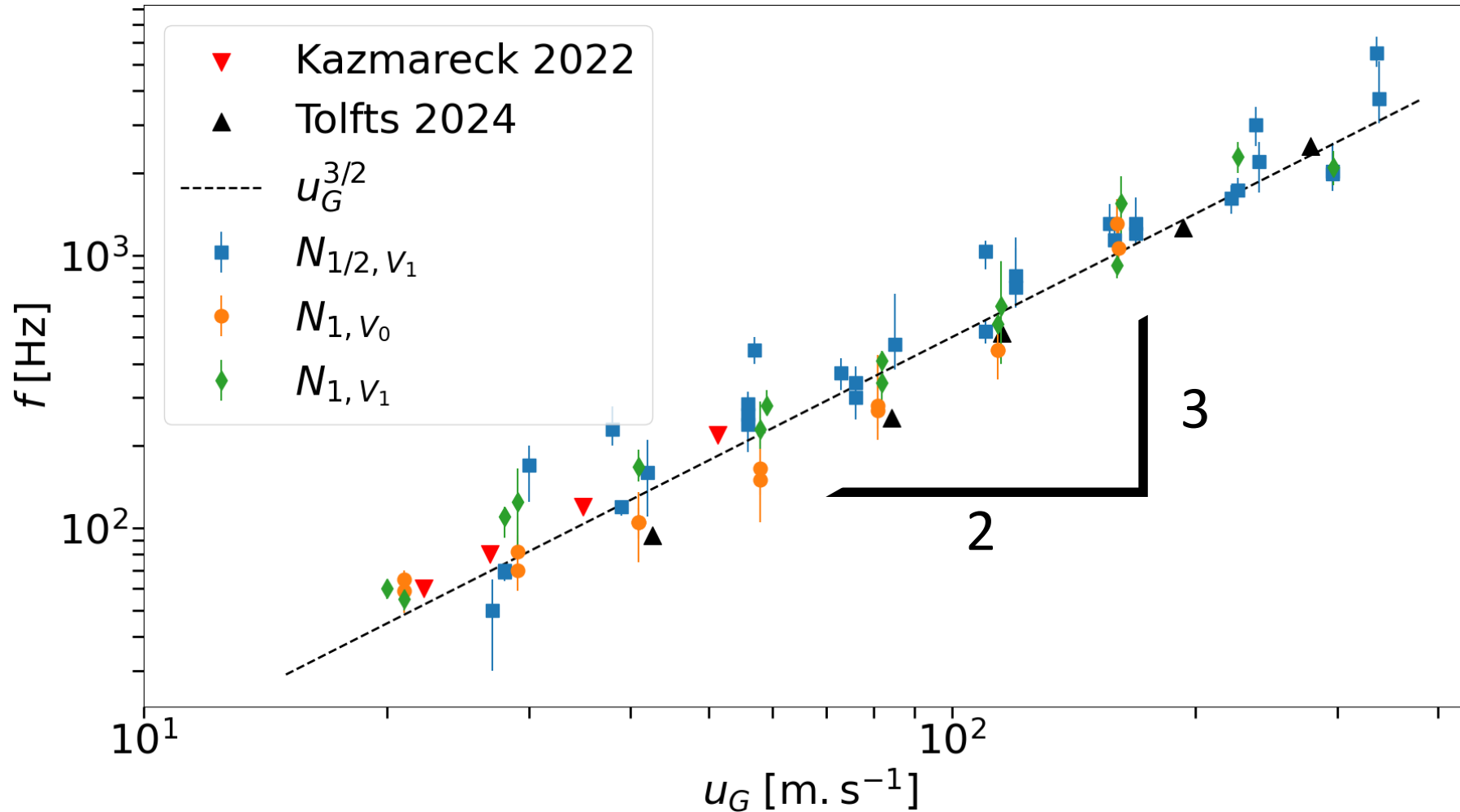
$$Re_L = 2500$$

High u_G : Fiber-type atomization



230 m/s, $We = 1400$

Flapping frequency



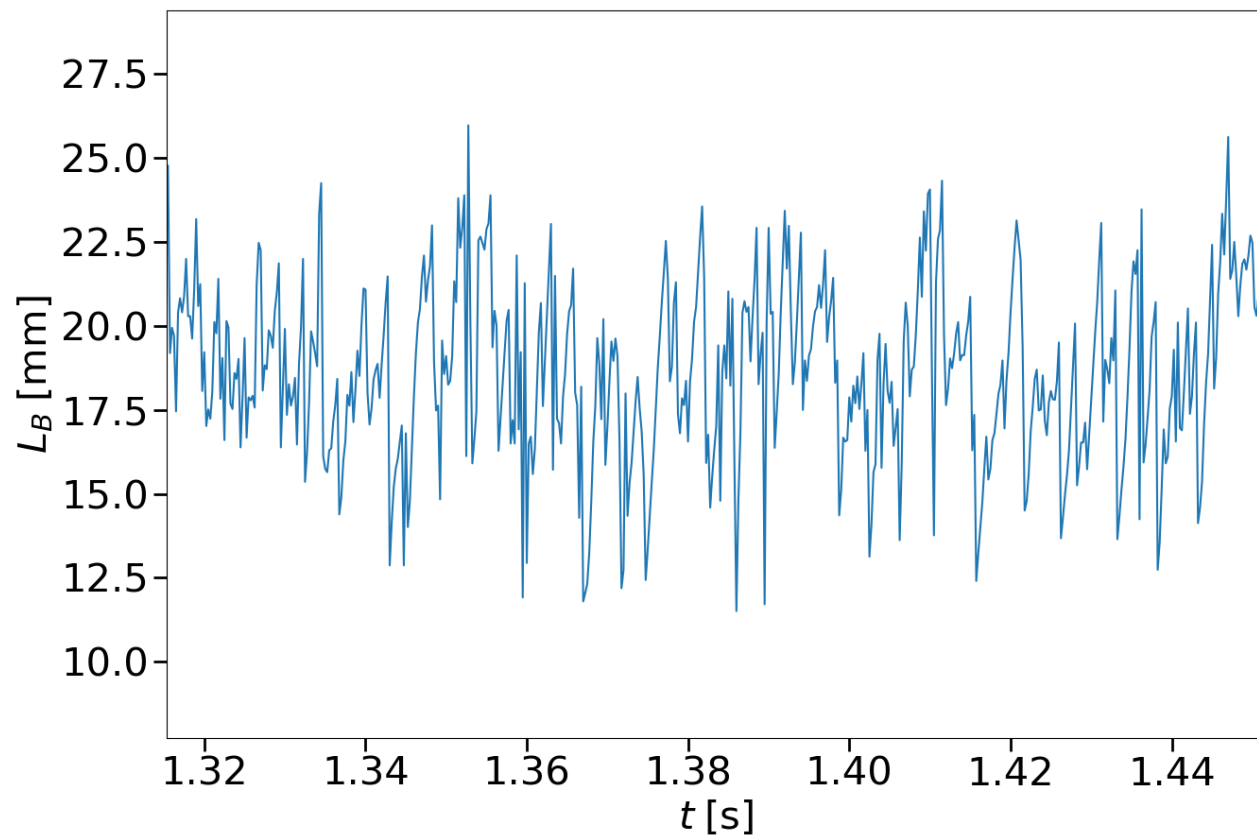
Power law only
partially explained by
models, e.g.
Marmottant &
Villermaux 2004

Marmottant, P., & Villermaux, E. (2004). On spray formation. *Journal of fluid mechanics*, 498, 73-111.

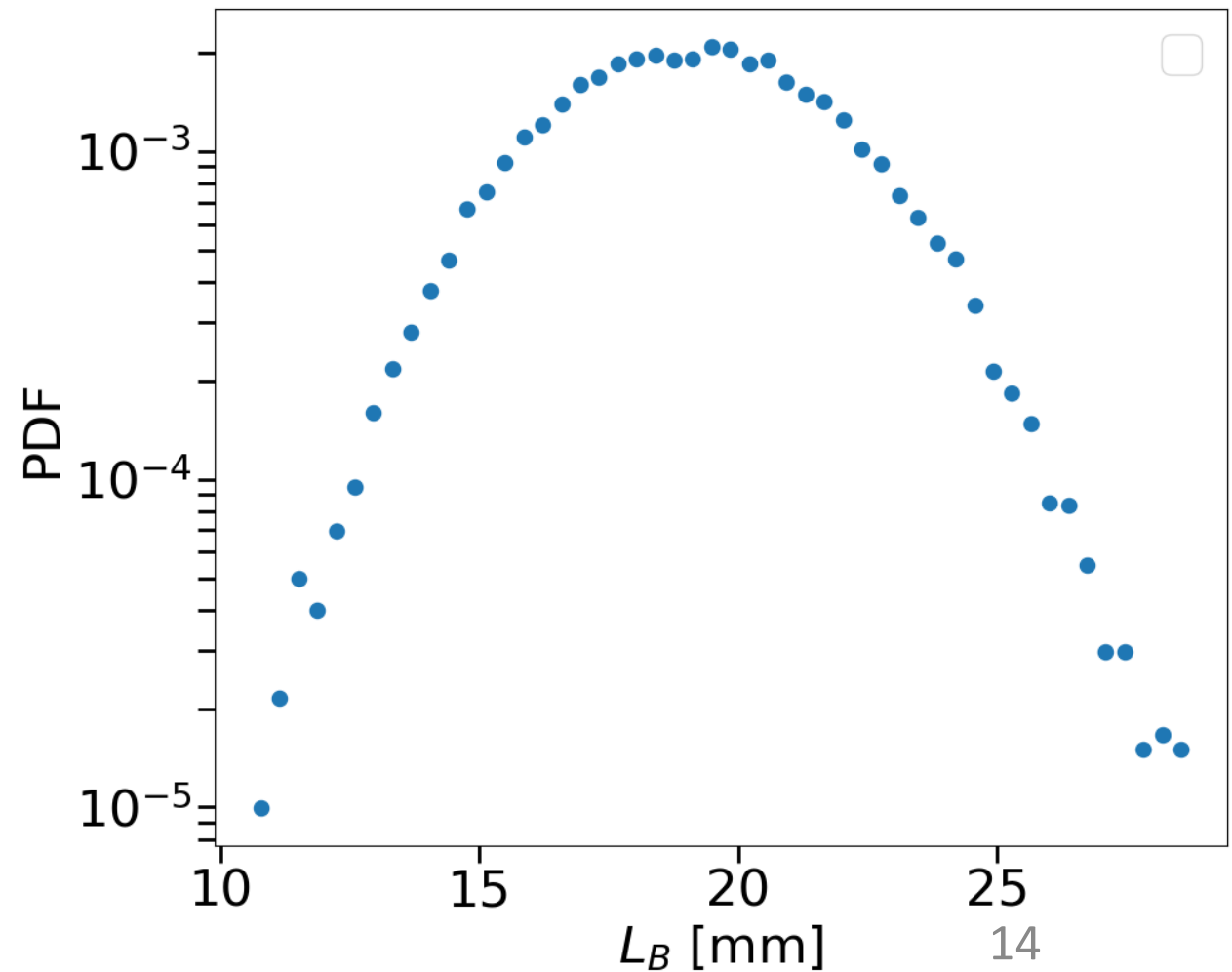
Kaczmarek, M., Osuna-Orozco, R., Huck, P. D., Aliseda, A., & Machicoane, N. (2022). *International Journal of Multiphase Flow*, 152, 104056.

Tolfts, O., Rack, A., & Machicoane, N. (2024). *International Journal of Multiphase Flow*, 181, 105004.

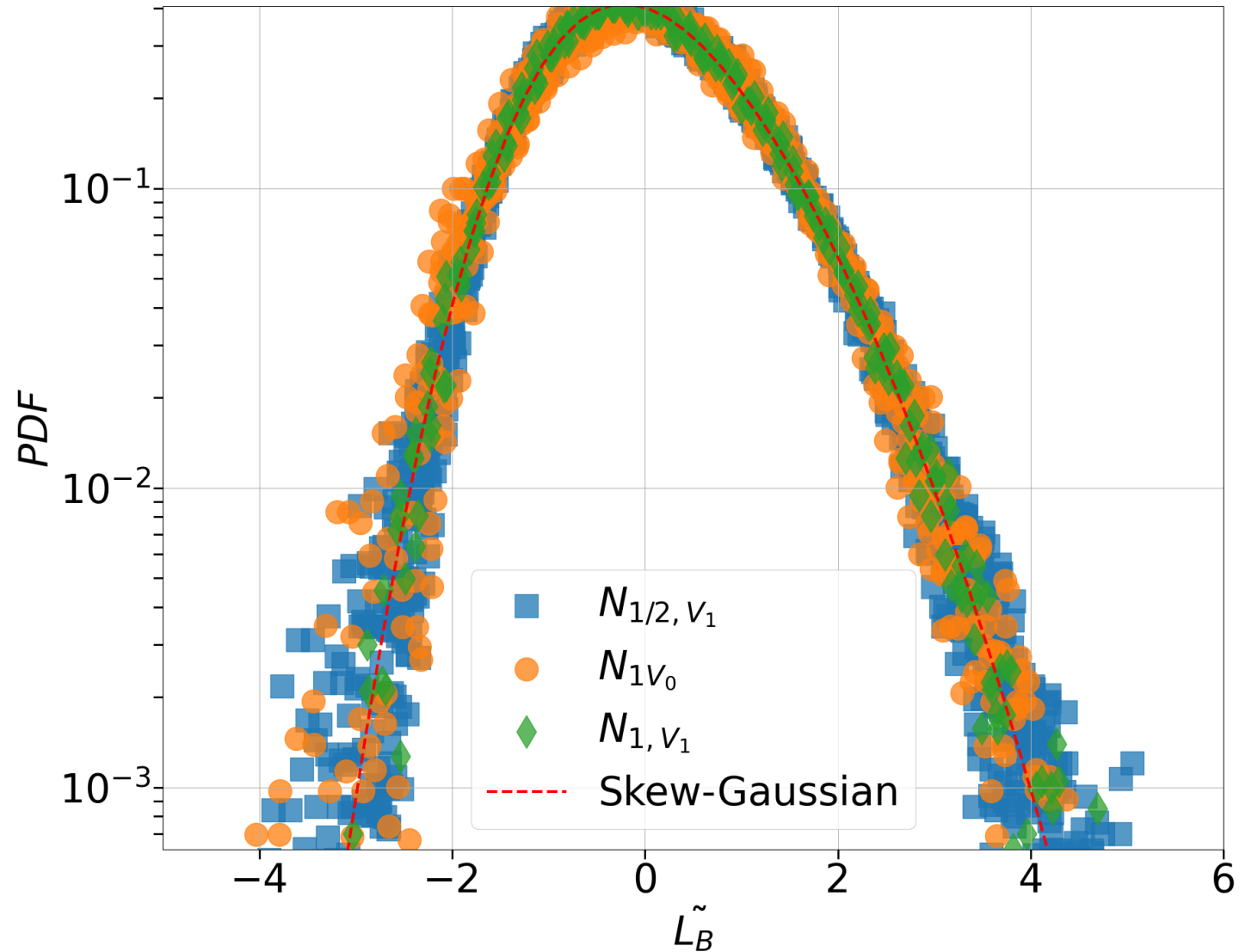
L_B statistics



Nozzle	d_L [mm]
N_{1,V_0}	2
N_{1,V_1}	2
$N_{1/2,V_1}$	1



L_B statistics



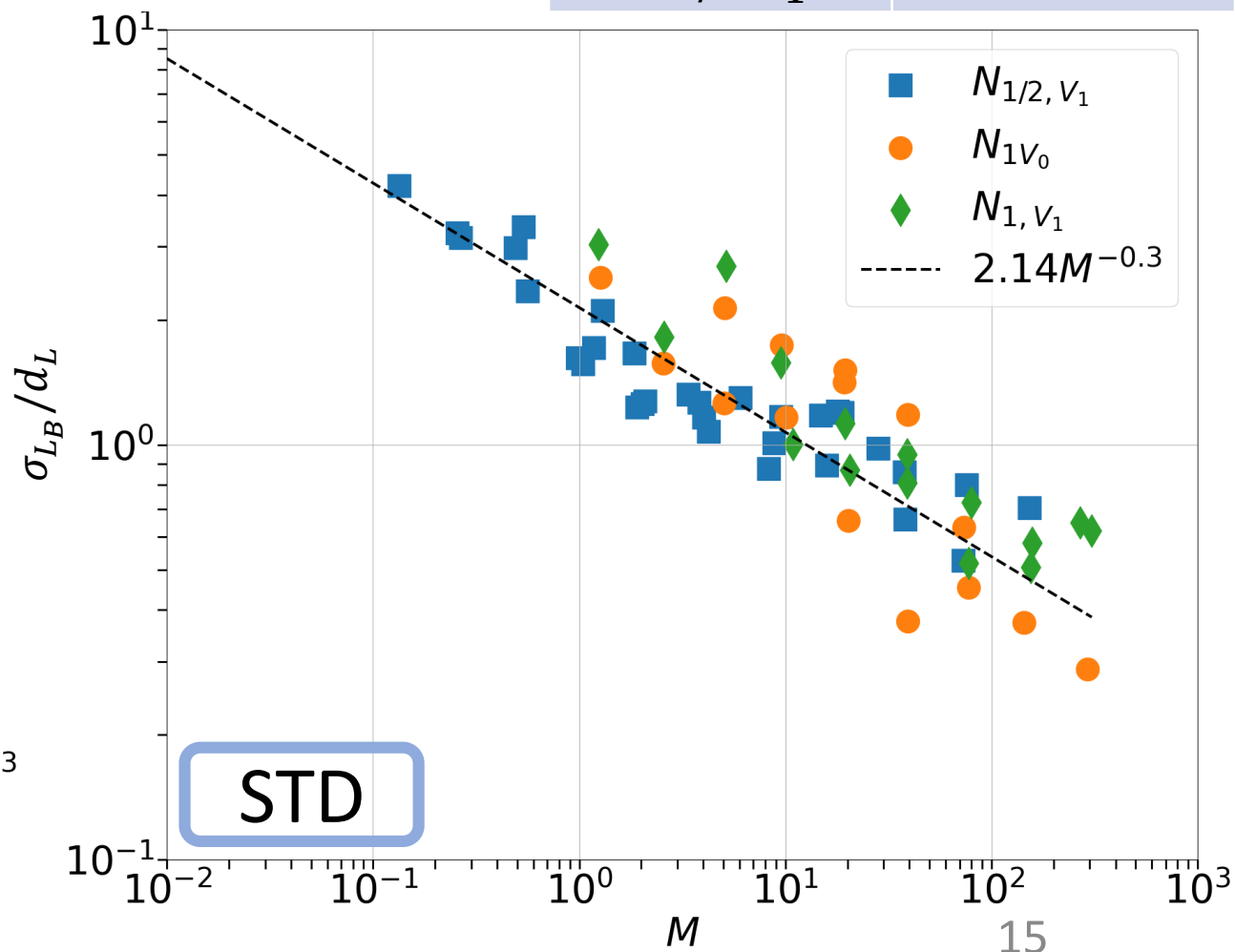
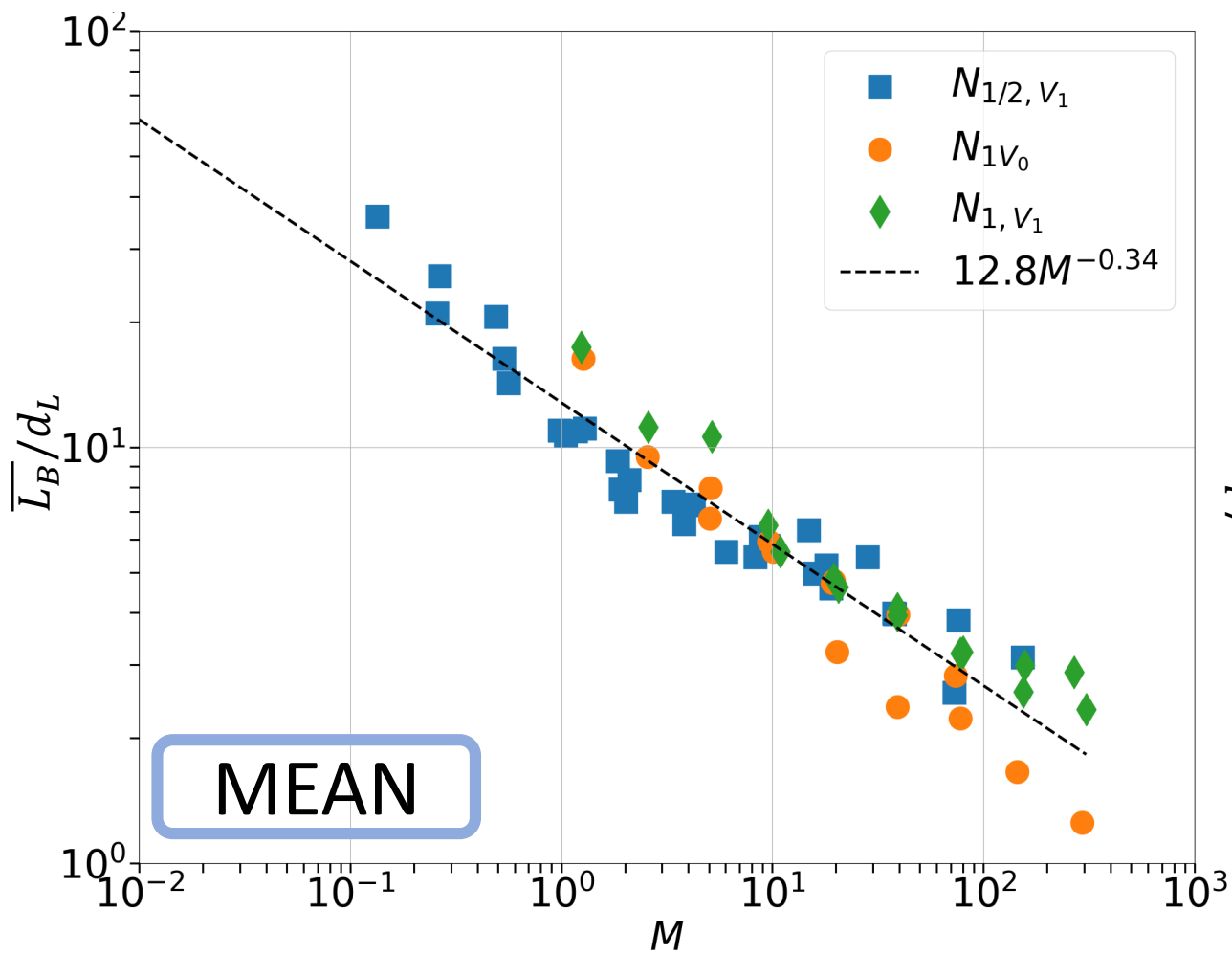
Nozzle	d_L [mm]
N_{1, V_0}	2
N_{1, V_1}	2
$N_{1/2, V_1}$	1

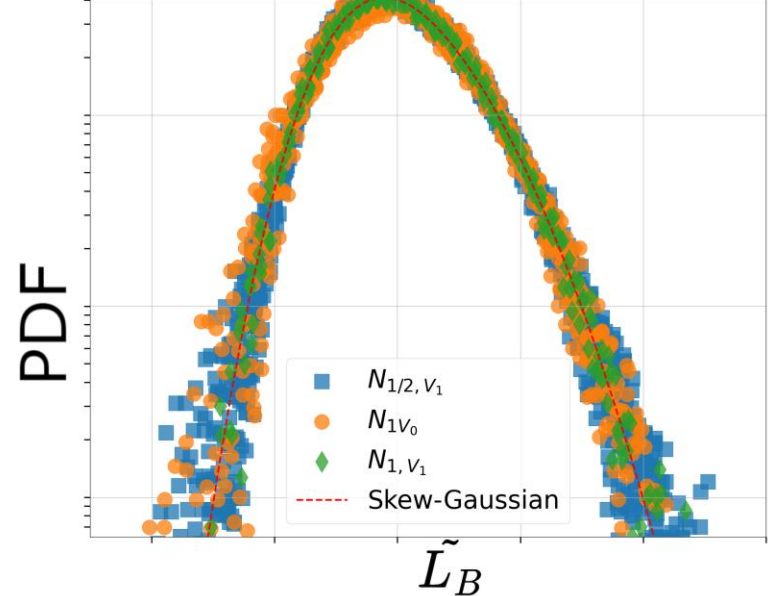
$$\tilde{L}_B = \frac{L_B - \overline{L}_B}{\sigma_{L_B}}$$

L_B statistics

Tolfts, O., Rack, A., & Machicoane, N. (2024). Morphology and dynamics of the liquid jet in high-speed gas-assisted atomization retrieved through synchrotron-based high-speed X-ray imaging. *International Journal of Multiphase Flow*, 181, 105004.

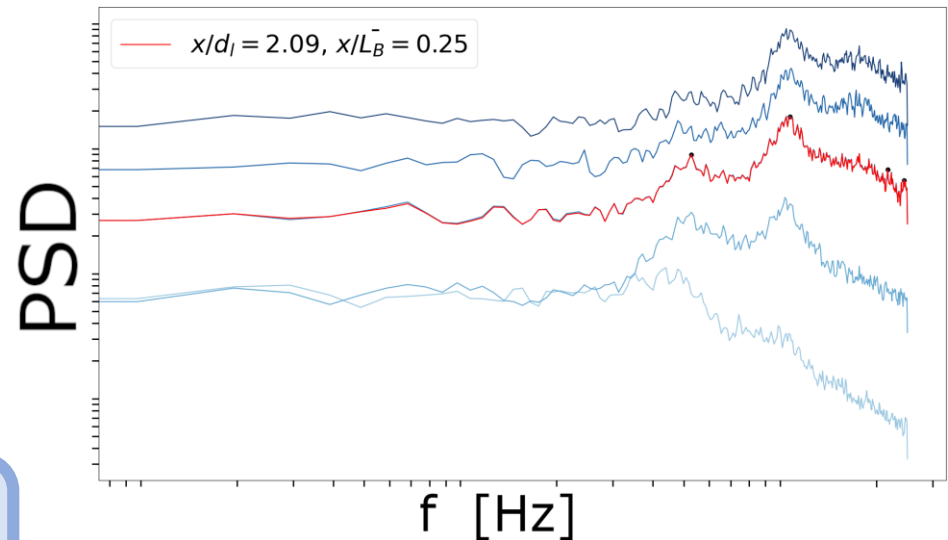
Nozzle	d_L [mm]
N_{1,V_0}	2
N_{1,V_1}	2
$N_{1/2,V_1}$	1





Scale invariant
centered normalized
PDF

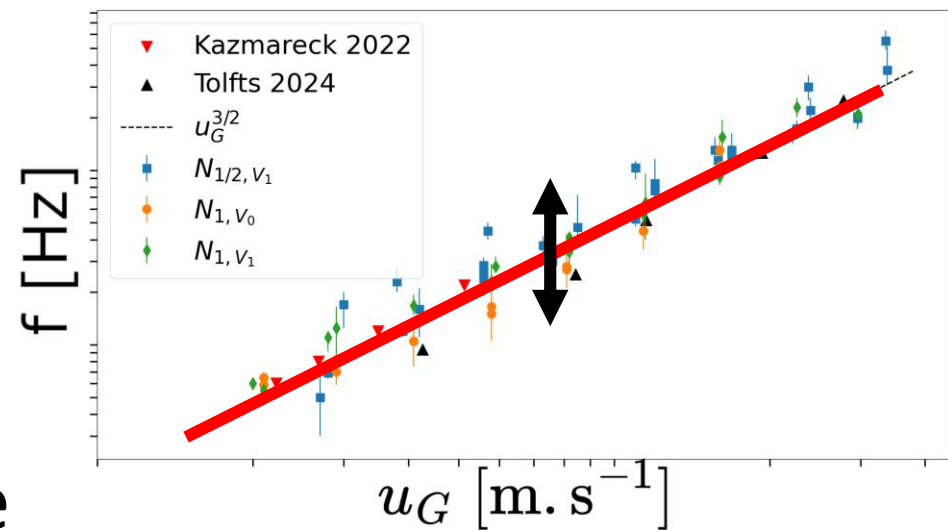
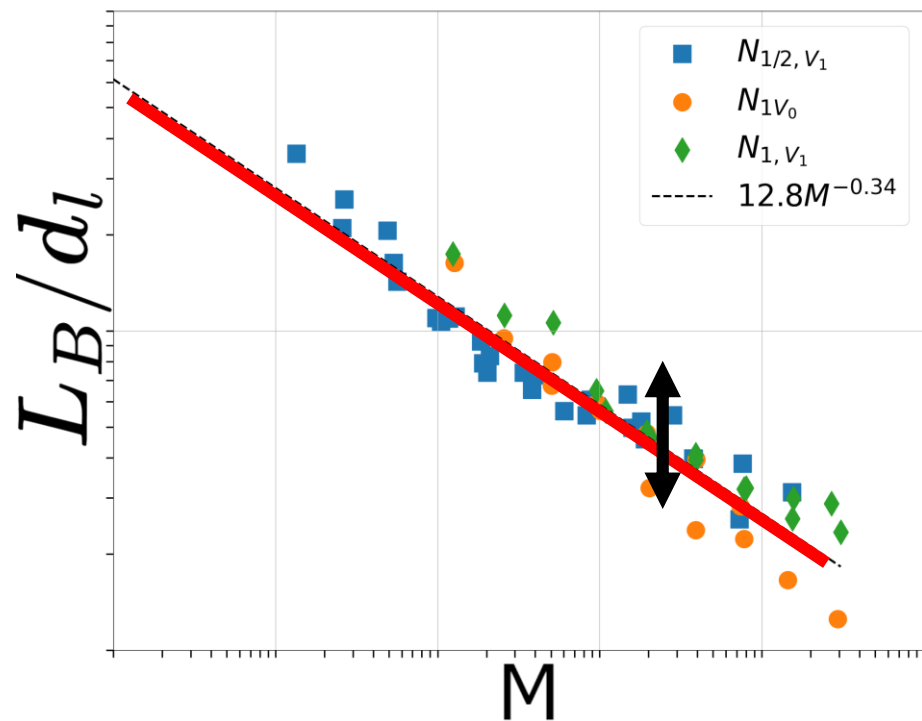
Rich spectra to
understand



Conclusions

Trends preserved
at different scales

Imperfect collapse



Perspectives

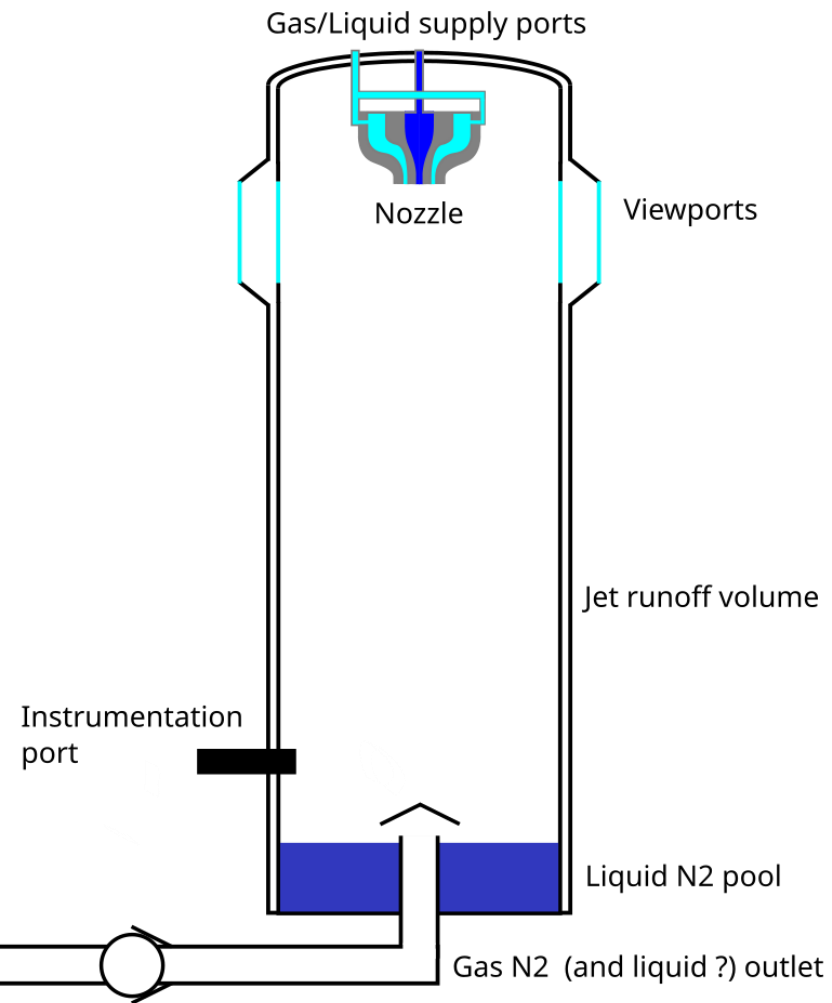
Analysis :

- Measure other quantities e.g. interface positions
- Linear Stability analysis with J-P Matas

Setup development :

- Expand range of scales
- Study other geometric variations, e.g. lip thickness
- Nitrogen cryostat in construction
- Helium setup in development

Perspectives



Design by
Grégory Garde
@Institut Néel

